بسم الله الرحمن الرحيم

Palestine Polytechnic University



College of Engineering & Technology

Mechanical Engineering Department

Graduation Project

Theoretical Design of Geothermal Assisted Heat Pump System for Barakat Al-Qadi Building in Hebron

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Abstract

Geothermal energy is one of the most important ways to conserve energy. The aims of this project is to describe the procedure of theoretical design of Vertical Ground loop Source Heat pump, to obtain a comparison between ordinary heat pump and geothermal heat pump, and to calculate the payback period for the economical feasibility study of the geothermal heat pump compared to chiller system for cooling and heating load.

Local climate conditions and soil properties of Hebron will be used to design the geothermal coil, and coefficient of performance for cooling and heating will be calculated and predicted for the local conditions available.

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CHAPTER ONE

INTRODUCTION

- 1.1 Introduction
- 1.2 Project Outline
- 1.3 The Objectives and Scope
- 1.4 Time Schedule

Chapter One

Introduction:

1.1 Introduction

Conventional energy sources based on oil, coal, and natural gas are harmful to environment, to economical progress, and to human life. These traditional fossil fuel-based energy sources are facing an increasing pressure on a host of environmental fronts, with the most serious challenge confronting the future use of coal being the Kyoto Protocol greenhouse gas reduction targets. Renewable energy sources currently supply around 15% of world's total energy demand in 2008. The supply is dominated by traditional biomass, mostly fuel wood used for cooking and heating, especially in developing countries [1].

The potential of renewable energy resources is enormous as they can in principle meet many times the world's energy demand. Renewable energy sources such as small hydropower, wind, solar, biomass, and geothermal can provide sustainable energy services, based on the use of routinely available, indigenous resources. It is time for transition to renewable-based energy systems, taking into consideration the costs of solar and wind power systems which have dropped substantially in the past 30 years, and continue to decline, unlike the prices of oil and gas which continue to fluctuate, in fact each moving in opposite directions [2].

Geothermal Energy is one of the renewable energy resources which is a clean low cost energy based on the idea of using the ground as a heat source/sink (which is defined as the Medium where heat is absorbed/rejected without changing its temperature) to reduce the cost of heating or cooling or for getting high temperature from the earth below the crust for producing steam and thus generate electricity.

Geothermal energy in both cases is a sustainable renewable energy resource because it reduces the energy consumed, and thus reduces the emissions and the use of the resources, this way it is a sustainable energy resource and sustainable way of using resources keeping in mind meeting our needs without compromising the needs of the future generations. So it has an economical dimension (reducing costs), ecological dimension (maintaining the environment, maintaining the resources, and reduce the emissions), Social dimension (human being health, human prosperity, and human development) with the fact those future generations was taken into consideration by acting this way, and that is the basis of the sustainable economies that are modeled now days in Sweden, Canada, and many countries in the world [3].

1.2 Project Outline

The project is divided up in 5 chapters; the chapters follow each other logically to get the complete idea about the project. Chapter 1; Provides an introduction about the project, Chapter 2; it talks about geothermal energy, Chapter 3; it talks about heat pump, Chapter 4; it talks about geothermal heat pump, Chapter 5; design and calculation.

1.3 The Objectives and Scope

- 1. To design and modeling a vertical loop Ground Source Heat pump.
- To obtain a comparison between ordinary heat pump and geothermal heat pump.
- To find the effect of the heat sink temperature on the performance of the heat pump.
- 4. To use renewable and clean energy in air conditioning.

1.4 Time Schedule

Table 1.1: Project time-schedule for first semester

Week No Task	1	2	33	4	5	6	7	8	9	10	1.1	12	13	14	15	16
Literature survey																
Collect the information about problem																
Geothermal energy																
Heat pump																
Geothermal heat pump				0												
Writing Documentation																
Printing and finishing																

Table 1.2: Project time-schedule for second semester

Week No Task	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
Calculation of heating and cooling loads for building	de la	Tall the same														
Design the GHP system								MINIST	The second							
Planning by AutoCAD and Selection									Mark The State of							
Writing Documentation																

CHAPTER TWO

GEOTHERMAL ENERGY

Content:

- 2.1 What is Geothermal Energy?
- 2.2 Temperature Variation with Depth
- 2.3 Earth's Structure
- 2.4 Sources of Geothermal Heat
- 2.5 Uses of Geothermal Energy

Chapter Two

Geothermal Energy

2.1 What is Geothermal Energy?

Geothermal energy is energy that comes from deep inside of Earth. The word geothermal comes from the Greek words geo (meaning "earth") and thermal (meaning "heat"). Geothermal power is a clean, renewable energy source that may someday provide a significant portion of the world's energy.

At the center of Earth about 4,000 miles (6,400 kilometers) below the surface is a very hot core. Some scientists estimate its temperature at about 7600 Fahrenheit (4200 Celsius). The center of the core is solid. The heat from this part of the core is powerful enough to melt rock into a hot liquid called magma. This molten (melted) rock forms the outer core. The heat from magma rises through Earth's mantle. The mantle is the layer that surrounds the core (see Figure 2.1) [5].

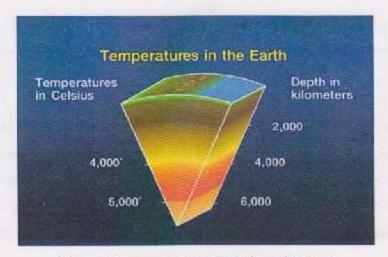


Figure 2.1: Temperature Variation with Dept

2.2 Temperature Variation with Depth

Considering that 46% of sun's energy is absorbed by the earth as shown in (Figure 2.2), because the ground transport heat slowly and has a high heat storage capacity, its temperature change slowly on the order of months or even years, heat absorbed by the earth during the summer effectively gets used in the winter.

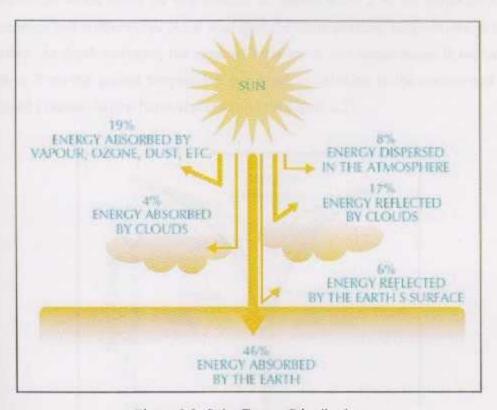


Figure 2.2: Solar Energy Distribution

Along with the Earth's structure and composition, irregular the temperature distribution within the Earth has been one of the fundamental research problems that impact our understanding of the evolution of the Earth. The present-day temperature distribution inside the Earth depends on (i) the original temperature distribution shortly after formation, (ii) the distribution and intensity of heat sources, both of

which are time-dependent, and (iii) the mechanism of internal heat transfer conduction, convection or both.

A thorough investigation into the ground properties of a proposed site is vital to designing an appropriate geothermal installation. The ground temperature is one of the most important factors, since it is the difference between this and the fluid temperature which drives the heat transfer. At depths below 2 m, the minimum and maximum soil temperatures occur later than the corresponding temperatures at the surface. As depth increases, the seasonal variation in soil temperatures is reduced. Above 2 m, the ground temperature is subject to radiation at the surface and is utilized in some shallow horizontal systems (see Figure 2.3).

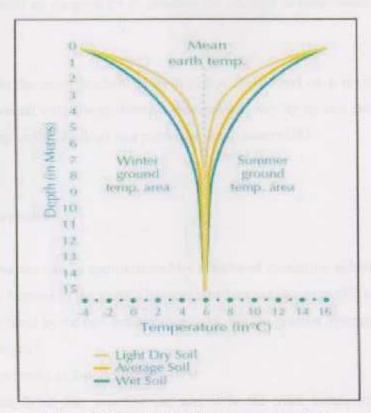


Figure 2.3: Typical Soil Temperature Variation

2.2.1 Temperature gradient

It is possible to estimate temperatures at 100 m depth by applying Fourier's Law of heat conduction: [14]

$$\frac{q}{A} = -\mathbf{k} * \frac{dt}{dz} \tag{2.1}$$

where q = heat flow (W/m²), k = thermal conductivity (W/m.K) and dt/dz = temperature gradient (K/m). Thermal conductivity has been taken as the thermal conductivity of the bedrock geology (i.e. the rock below the soil and superficial deposits layers). The calculated temperature gradient has been added to the estimate of the mean annual air temperature to generate the estimate of temperature at 100 m depth.

The variation in the mean gradient is from (1.5 - 5°C/100m) on a regional basis. Within an individual well, the geothermal gradient can vary by up to a factor of 5 or more, depending on the lithology in a particular depth interval.[6]

2.3 Earth's Structure

The Earth's structure can be approximated by a series of concentric spherical shells. The large-scale features of the Earth's internal structure are shown in (Figure 2.4). The core, constituted by the two innermost regions, has the greatest average density, exceeding 10⁴ kg.m³.

The Earth is composed of four different layers:

 Crust: is the layer that you live on, and it is the most widely studied and understood, the crust is only about 25 miles (32 kilometers) thick under the continents.

- 2. Mantle: is much hotter and has the ability to flow.
- Outer Core: is so hot that the metals in it are all in the liquid state, is composed of the melted metals of nickel and iron.
- Inner Core: has temperatures and pressures so great that the metals are squeezed together, and are forced to vibrate in place like a solid.

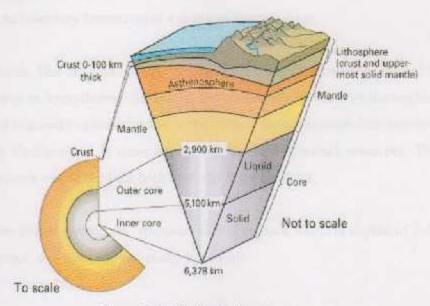


Figure 2.4: The Earth Structure

2.4 Sources of Geothermal Energy

70% comes from the decay of radioactive nuclei with long half lives that are embedded within the Earth. Some energy is from residual heat left over from Earths formation. The rest of the energy comes from meteorite impacts.

There are four types of geothermal resources:

Hydrothermal: when hot water or steam is formed in fractured or porous rock at shallow to moderate depths (100m to 4.5km) as a result of either the intrusion in the earth's crust of molten magma from the earth's interior, or the deep circulation of water through a fault or fracture, they are more suited for space heating than for electricity production [7].

- Geopressured: geothermal resources consist of hot brine saturated with methane, found in large, deep aquifers under high pressure. The water and methane is trapped in sedimentary formations at a depth of about 3-6 km.
- 3. Hot Dry Rock: Hot dry rock (HDR) is a heated geological formation formed in the same way as hydrothermal resources, but containing no water as the aquifers or fractures required to conduct water to the surface are not present. This resource is virtually limitless and is more accessible than hydrothermal resources, This type of resource can be used for both heat and for natural gas.
- 4. Magma: the largest geothermal resource, is molten rock found at depths of 3-10 km and deeper, and therefore not easily accessible.

2.5 Uses of Geothermal Energy

Geothermal energy can be used for electricity production, for commercial, industrial, and residential direct heating purposes, and for efficient home heating and cooling through geothermal heat pumps, the three main uses of geothermal energy are:

- Direct Use and District Heating System: which use hot water from springs or reservoirs near the surface.
- 2. Electricity Generation: in a power plant requires water or steam at very high temperature (300 to 700 °F). Geothermal power plants are generally built where geothermal reservoirs are located within a mile or two of the surfaces.

 Geothermal Heat Pumps: use stable ground or water temperature near the earth's surface to control building temperature above ground.

2.5.1 Direct Use of Geothermal Energy

Hydrothermal resources of low to moderate temperature (20-150 °C) are utilized to provide direct heating for a range of applications.

Geothermal heat is used directly, without involving a power plant or a heat pump, for a variety of applications such as space heating and cooling, food preparation, hot spring bathing and spas (balneology), agriculture, aquaculture, greenhouses, and industrial processes. Uses for heating and bathing are traced back to ancient Roman times.

2.5.2 Geothermal Power Plants

Geothermal power plant use hydrothermal resources which have two common ingredients: water (hydro) and heat (thermal). Its require high temperature (300 to 700 °F), hydrothermal resources that may come from either dry steam wells or hot water wells. We can use these resources by drilling wells into the earth and piping the steam or hot water to the surface. Geothermal wells are one to two miles deep.

There are three basic types of geothermal power plants:

1. Dry Steam Power Plants: Dry steam plants use hydrothermal fluids that are primarily steam. The steam travels directly to a turbine, which drives a generator that produces electricity. The steam eliminates the need to burn fossil fuels to run the turbine (also eliminating the need to transport and store fuels). These plants emit only excess steam and very minor amounts of gases. Steam technology is still effective unday at currently in use at The Geysers in northern California, the world's largest single source of geothermal power. [8]

- 2. Flash Steam Power Plants: Flash steam plants are the most common type of geothermal power generation plants in operation today. Fluid at temperatures greater than 360°F (182°C) is pumped under high pressure into a tank at the surface held at a much lower pressure, causing some of the fluid to rapidly vaporize, or "flash." The vapor then drives a turbine, which drives a generator. If any liquid remains in the tank, it can be flashed again in a second tank to extract even more energy.
- 3. Binary Cycle Power Plants: This system passes moderately hot geothermal water past a liquid, usually an organic fluid, that has a lower boiling point. The resulting steam from the organic liquid drives the turbines. This process does not produce any emissions and the water temperature needed for the water is lower than that needed in the Flash Steam Plants (250-360°F).

2.5.3 Geothermal Heat Pump

People also harness geothermal energy by using heat-pump systems. These systems take advantage of stable temperatures beneath Earth's surface. No matter what season it is, a few feet underground, the temperature is about 50-60°F (10-15°C).

Heat-pump systems include three parts: what is called an Earth connection, the heat pump itself, and a heat distribution system. The Earth connection is a loop of pipes buried in the ground near or beneath a building. A fluid circulates in the loop of pipes. The fluid is water or a mixture of water and antifreeze. The fluid picks up heat from within Earth. The heat pump removes heat from the fluid and sends it to the building. Then, pipes distribute the heat through the building. When it is warm out, beat-pump systems can be used backwards for cooling. The system pulls warm air from the building and sends it underground [8].

CHAPTER THREE

HEAT PUMP

Content:

- 3.1 Introduction
- 3.2 Basic of Heat Pump
- 3.3 Heat Pump Operation
- 3.4 Types of Heat Pumps
- 3.5 Operating Cycle

Chapter Three

Heat Pump

3.1 Introduction

Heat pumps are generally more expensive to purchase and install than other heating systems, but they save money in the long run in some areas because they lower the heating bills. Despite their relatively higher initial costs, the popularity of heat pumps is increasing. About one-third of all single-family homes built in the United States in the last decade are heated by heat pumps.

The most common energy source for heat pumps is atmospheric air (air to- air systems), although water and soil are also used. The major problem with air-source systems is frosting, which occurs in humid climates when the temperature falls below 2 to 5°C. Heat pumps and air conditioners have the same mechanical components. Therefore, it is not economical to have two separate systems to meet the heating and cooling requirements of a building. One system can be used as a heat pump in winter and an air conditioner in summer. This is accomplished by adding a reversing valve to the cycle, [9]

3.2 Basic of Heat Pump

A heat pump is a devise which allows transport of heat from a lower temperature level to a higher one, by using external energy (e.g. to drive a compressor). This seems in a closed-cycle process in which the working fluid is constantly undergoing a change of state (evaporation, compression, condensation and expansion).

A heat pump system consists of heat pumps and piping work; system components include heat exchangers, heat source, heat sink, and controls to provide effective and energy-efficient heating and cooling operations. HCFC-22, HFC-134a, and HFC-407C are the most widely used refrigerants in heat pumps [10].

The thermodynamic principle behind a compression heat pump is the fact that a gas becomes warmer when it is compressed into a smaller volume. This effect is common experience e.g. for cyclists when adjusting air pressure in the tires: The air pump gets warmer in the process.

3.3 Heat Pump Operation

In a heat pump, a medium with low boiling point ("refrigerant") is evaporated by the ground heat, the resulting vapor (gas) is compressed (by using external energy, typically electric power) and thus heated, and then the hot gas can supply its heat to the heating system. Still being in the high pressure part, the vapor now condenses again to a liquid after the useful heat has been transferred. Finally, the fluid enters back into the low-pressure part through an expansion valve, gets very cold and can be evaporated again to continue the cycle (see Figure 3.1).

In General, a fully hermetic compressor (piston or scroll for extremely quiet operation) with built-in, internal overload protection is used in these heat pumps. Stainless steel flat plate heat exchangers or other types like shell and tube or coaxial are used for the evaporator and condenser. Other items in the refrigerant cycle are the expansion valve and possibly a sight glass accumulator and a filter/drier. The refrigeration cycle (Figure 3.1) should be fully insulated against thermal losses and prevent condensation inside the heat pump. For heating/cooling reversible operation.

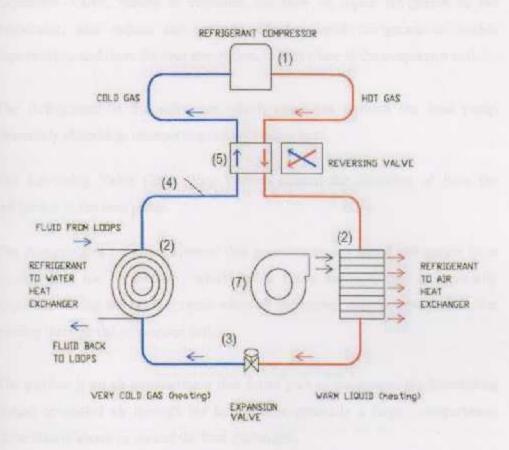


Figure 3.1: Schematic of a vapor compression heat pump

3.3.1 Heat Pump Components

- The Compressor: draws the refrigerant from the evaporator then compresses it.
 Compression adds energy to the refrigerant by raising the pressure and temperature to a desired level.
- 2. Heat Exchanger Coils: The Evaporator and Condenser are coils that absorb or reject heat between two mediums of different temperature; because a heat pump can reverse its function (cooling or heating).

- Expansion Valve: meters or regulates the flow of liquid refrigerant to the evaporator, also reduce the pressure of the liquid refrigerant to enable vaporization, and there for heat absorption, to take place in the evaporator coil.
- The Refrigerant: is the substance which circulates through the heat pump alternately absorbing, transporting, and releasing heat.
- The Reversing Valve (Four Way Valve): control the direction of flow the refrigerant in the heat pump.
- 6. The Accumulator: a storage vessel that prevents excess liquid refrigerant from passing into the compressor, which could cause damage, this is especially important during the heating cycle when all refrigerant may not evaporate after passing through the evaporator coil.
- 7. The plenum is an air compartment that forms part of the system for distributing heated or cooled air through the house. It is generally a large compartment immediately above or around the heat exchanger.

3.4 Types of Heat Pumps

Heat pumps are often classified according to their heat source. The three principal types used in residential and light commercial heating/ cooling systems are: (1) air-source heat pumps, (2) ground-source heat pumps, and (3) water-source heat pumps.

341 Air-Source Heat Pumps

An air-source heat pump (also sometimes called an air-to-air heat pump) relies on the

and transfers it to the rooms and spaces inside the structure. A major technical problem associated with earlier air-source heat pumps was that the temperature of the outdoor air is commonly lowest when heat requirements are highest—that is, during the cold winter months.

Air-source heat pumps operate most efficiently in areas where the winter temperatures usually remain above 0°C. In climates where the winter temperatures frequently drop below freezing, a backup auxiliary heater must be used with an air-source heat pump.

3.4.2 Ground Source Heat Pumps

A ground-source heat pump uses the constant temperature of the earth instead of the outdoor air as the heat-exchange medium (that is, the heat source or heat sink depending on the heating or cooling cycle).

During the summer when cool interior temperatures are required, the fluid circulating through the indoor coil of the heat pump collects the heat from inside the structure and pumps it outdoors into a pipe system located below ground. The heat is then absorbed into the ground through the piping and the fluid is recirculated back to the unit. In the winter, the process is reversed.

The system is based on the principle of heat transfer, whereby heat is transferred from one object (the underground pipe) to another object (the ground) through direct contact (see Figure 3.2). Ground-source heat pumps are more efficient and economical to operate than conventional air-source units in areas with similar heating and cooling loads [11].

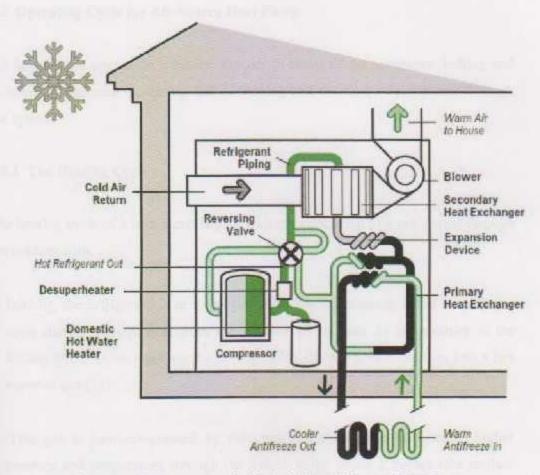


Figure 3.2: Components of a Typical Ground-Source Heat Pump

3.4.3 Water-Source Heat Pumps

Water-source heat pumps use water for both the heat source and the heat sink. The water serves as a direct heat transfer medium in contrast to the heat transfer fluid used in closed-loop systems. The steady cool temperature of the water offsets the seasonal temperature variations by serving as a reservoir of heat in the winter and as a drain of heat in the summer.

3.5 Operating Cycle for Air-Source Heat Pump

All heat pumps operate in a similar manner in terms of the refrigerant boiling and condensing, pressure increasing and decreasing and the flow of refrigerant through the system.

3.5.1 The Heating Cycle

The heating cycle of a heat pump begins with the circulation of a refrigerant through the outdoor coils.

- Initially, the refrigerant is in a low-pressure, low-temperature liquid state, but it soon absorbs enough heat from the outdoor air to raise its temperature to the boiling point. Upon reaching the boiling point, the refrigerant changes into a hot vapor or gas [12].
- This gas is then compressed by the compressor and circulated under higher pressure and temperature through the indoor coils, where it comes into contact with the cooler room air that circulates around the coils. The cooler air causes the gas to cool, condense, and return to the liquid state.
- The condensation of the refrigerant vapor releases heat to the interior of the structure. After the refrigerant has returned to a liquid state, it passes through a special pressure-reducing device (an expansion valve) and then back through the outdoor coils where the heating cycle begins all over again.
- The temperature of the room air that originally cooled the higher-temperature refrigerant vapor is itself increased by the process of heat transfer and recirculated throughout the room to provide the necessary heat.

3.5.2 The Cooling Cycle

- In the cooling cycle, the reversing valve causes the flow of the refrigerant to be reversed. As a result, the compressor pumps the refrigerant in the opposite direction so that the coils that heat the building or space in cold weather cool it in warm weather (See Figure 3.3).
- In other words, the heat is extracted from the interior, cycled through the heat pump, and then expelled outside the building or space during the condensation of the refrigerant (that is, its change from a gaseous to a liquid state).

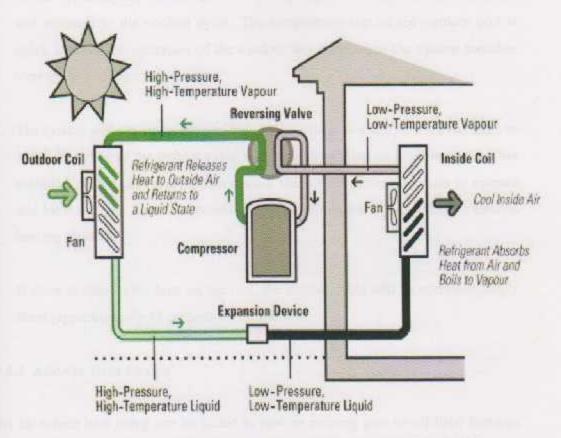


Figure 3.3: Components of an Air-source Heat Pump (Cooling Cycle)

3.5.3 The Defrost Cycle

- Applies only to air-source heat pump.
- Because the outdoor air is relatively cool when the heat pump is on the heating
 cycle, and the outdoor coil is acting as an evaporator, frost forms on the surface
 of the coil under certain conditions of temperature and relative humidity, and it
 must be removed. This is accomplished by putting the heat pump through a
 defrost cycle.
- In the defrost cycle, the action of the heat pump is reversed at certain intervals
 and returned to the cooling cycle. The temperature rise of the outdoor coil is
 quick because the operation of the outdoor fan stops when the system switches
 over to the cooling cycle.
- The system will remain in the cooling cycle until the coil temperature has risen to 14°C. The time of the defrost cycle will vary, depending on how much frost has collected on the coil. During this period, the indoor motor continues to operate and blow cool air. This cold condition can be eliminated by installing an electric heating element.
- If there is little or no frost on the coil, the defrost cycle will be correspondingly short (approximately 45 seconds to 1 minute).

3.5.4 Add-On Heat Pumps

An air-source heat pump can be added to new or existing gas- or oil-fired furnaces (See Figure 3.4). This unit, typically called an add-on, dual-fuel, or hybrid heat pump, normally operates as a conventional heat pump. During extremely cold

weather, the refrigerant circuit is turned off and the furnace provides the required space heating. These add-on heat pumps share the air distribution system with the warm-air furnace. The indoor coil may be either parallel to or in series with the furnace. However, the furnace should never be upstream of the indoor coil if both systems are operated together. Special controls are available that prevent simultaneous operation of the heat pump and furnace in this configuration. This operation raises the refrigerant condensing temperature, which could cause compressor failure.

In applications where the heat pump and furnace operate simultaneously, the following conditions must be met: (1) the furnace and heat pump indoor coil must be arranged in parallel, or (2) the furnace combustion and flue passages must be designed to avoid condensation-induced corrosion during cooling operation. [13]

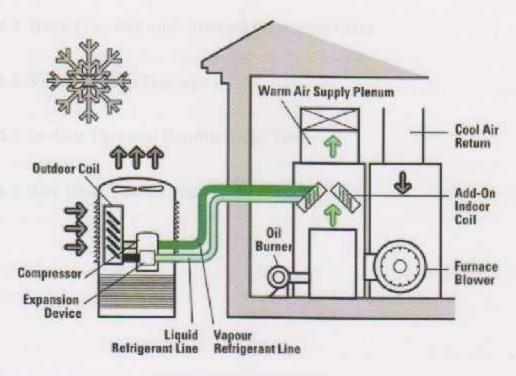


Figure 3.4: Add-On Heat Pump

CHAPTER FOUR

GEOTHERMAL HEAT PUMP SYSTEM

Content:

- 4.1 Overview of Ground-Source Heat Pump Systems
- 4.2 Types of Geothermal Heat Pump System
- 4.3 Heat Transfer and Ground Characteristics
- 4.4 Vertical Loop Concept
- 4.5 In-Situ Thermal Conductivity Test
- 4.6 The Distribution System

Chapter Four

Geothermal Heat Pump System

4.1 Overview of Ground-Source Heat Pump Systems

Ground-source heat pump (GSHP) systems (also referred to as geothermal heat pump systems, earth energy systems, and Geo Exchange systems) have received considerable attention in the recent decades as an alternative energy source for residential and commercial space heating and cooling applications. GSHP applications are one of three categories of geothermal energy resources as defined by ASHRAE (1995). These categories are:

- 1. high-temperature (>150 °C) electric power production.
- 2. intermediate- and low-temperature (<150 °C) direct-use applications.
- GSHP applications (generally <32 °C). The GSHP applications are distinguished from the others by the fact that they operate at relatively low temperatures.

The term "ground-source heat pump" has become an all-inclusive term to describe a heat pump system that uses the earth, ground water, or surface water as a heat source and/or sink. GSHP systems consist of three loops or cycles as shown in (Figure 4.1).

- The first loop is on the load side and is either an air/water loop or a water/water loop, depending on the application.
- 2. The second loop is the refrigerant loop inside a water- source heat pump.
- 3. The third loop in the system is the ground loop in which water or an antifreeze solution exchanges heat with the refrigerant and the earth.

Efficiencies of GSHP systems are much greater than conventional air-source heat pump systems. A higher COP (coefficient of performance) can be achieved by a GSIIP because the source/sink earth temperature is relatively constant compared to air temperatures.

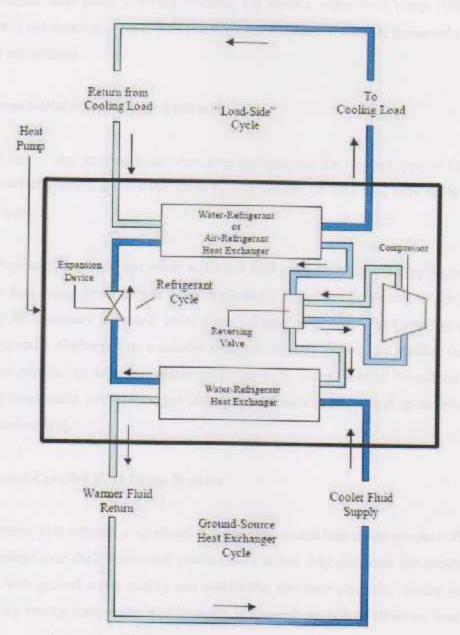


Figure 4.1: Schematic of cycles in a GSHP system in cooling mode

4.2 Types of Geothermal Heat Pump System

According to ASHRAE (1995) groups GSHP systems included into three categories based on the heat source/sink used. A fourth category is added here for the sake of completeness. These categories are: (1) ground-water heat pump (GWHP) systems, (2) ground-coupled heat pump (GCHP) systems, (3) surface water heat pump (SWHP) systems, and (4) standing column well (SCW) systems. Each of these is discussed in the following subsections.

4.2.1 Ground-Water Heat Pump Systems

GWHP systems, also referred to as open-loop systems, are the original type of GSHP system. GWHP systems are not the focus of this project, so they will only be briefly described here.

In GWHP systems, conventional water wells and well pumps are used to supply ground water to a heat pump or directly to some application. Corrosion protection of the heat pump may be necessary if ground water chemical quality is poor. The "used" ground water is typically discharged to a suitable receptor, such as back to an aquifer, to the unsaturated zone a, to a surface-water body, or to a sewer. Design considerations include: ground-water availability, ground-water chemical quality, and ground-water disposal method [15].

4.2.2 Ground-Coupled Heat Pump Systems

GCHP systems, also referred to as closed-loop ground-source heat pump systems. Their main advantage over their water-well prodecessors is that they eliminate the problems associated with ground water quality and availability and they generally require much less pumping energy than water well systems because there is less elevation head to secreome.

In GCHP systems, heat rejection/extraction is accomplished by circulating a heat exchange fluid through a piping system buried in the earth. This fluid is either pure water or an antifreeze solution and is typically circulated through high-density polyethylene (HDPE) pipe installed in vertical boreholes or horizontal trenches as shown in (Figure 4.2, Figure 4.3). These systems are further subdivided into vertical GCHP systems and horizontal GCHP systems.

4.2.2.1 Vertical Ground-Coupled Heat Pump Systems

Vertical borehole GCHP systems are the primary focus of this entire research.

Therefore, they are described in some detail here and their design challenges are explained, laying the foundation for the motivation of this study.

In vertical borehole GCHP systems, ground heat exchanger configurations typically consist of one to tens of boreholes each containing a U-shaped pipe through which the heat exchange fluid is circulated. A number of borehole to borehole plumbing arrangements are possible. Typical U-tubes have a diameter in the range of (19 to 38 mm) and each borehole is typically (30.5 to 122 m) deep with a diameter ranging from (76 to 127 mm). The borehole annulus is generally backfilled with a material that prevents contamination of ground water (see Figure 4.2) [4].

The advantages of the vertical GCHP are that it (1) requires relatively small plots of ground, (2) is in contact with soil that varies very little in temperature and thermal properties, (3) requires the smallest amount of pipe and pumping energy, and (4) can yield the most efficient GCHP system performance. Disadvantages are (1) typically higher cost because of expensive equipment needed to drill the borehole and (2) the limited availability of contractors to perform such work.

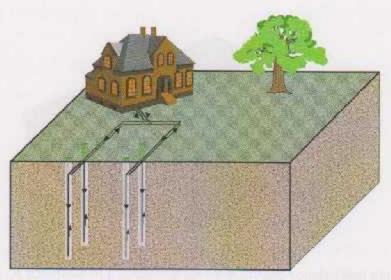


Figure 4.2: A schematic of a vertical borehole ground-coupled heat pump system

4.2.2.2 Horizontal Ground-Coupled Heat Pump Systems

In horizontal GCHP systems, ground heat exchanger configurations typically consist of a series of parallel pipe arrangements laid out in dug trenches or horizontal boreholes about (0.91 to 1.83 m) deep. A number of piping arrangements are possible, "Slinky" configurations (as in Figure 4.3) are popular and simple to install in trenches and shallow excavations. In horizontal boreholes, straight pipe configurations are installed. Typical pipes have a diameter in the range of (19 to 38 mm) and about (121.9 to 182.9 m) of pipe is installed per ton of heating and cooling capacity [13].

The thermal characteristics of horizontal GCHP systems are similar to those of vertical ones. The main difference is that horizontal ground-loop heat exchangers are more affected by weather and air temperature fluctuations because of their proximity to the earth's surface.

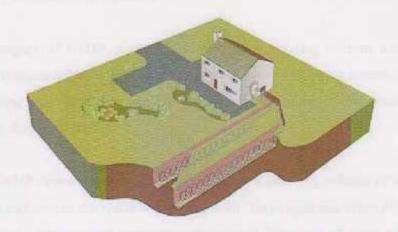


Figure 4.3: A schematic of a horizontal borehole ground-coupled heat pump system

4.2.3 Surface-Water Heat Pump Systems

The third category of GSHP systems is the surface-water heat pump (SWHP) system. A schematic of a SWHP system is shown in (Figure 4.4). The surface-water heat exchanger can be a closed-loop or open-loop type. Typical closed-loop configurations are the Slinky coil type or the loose bundle coil type. In the closed-loop systems, heat rejection/extraction is accomplished by circulating a heat exchange fluid through HDPE pipe positioned at an adequate depth within a lake, pond, reservoir, or other suitable open channel.

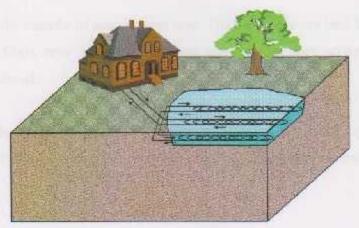


Figure 4.4: A schematic of a surface-water heat pump system.

4.2.4 Standing Column Well Systems

The fourth category of GSHP systems is known as a standing column well (SCW) system. These systems are about as old as the ground-water heat pump systems, but are recently receiving much attention. Since these are not the subject of this research, they are only briefly discussed here.

This type of GSHP draws water to a heat pump from a standing column of water in a deep well bore and returns the water to the same well. These systems, primarily installed in hard rock areas, use uncased boreholes with typical diameters of about (15.24 cm) and depths up to (457.2 m). The uncased borehole allows the heat exchange fluid to be in direct contact with the earth and allows ground water infiltration over the entire length of the borehole.

4.3 Heat Transfer and Ground Characteristics

4.3.1 Heat Transfer

Heat may be transferred or moved from one body to another by one of three methods:

- 1. Radiation: is the transfer of heat by heat rays. The earth receives heat from the sun by radiation. Light rays from the sun turn into heat as they strike opaque or translucent materials.
- 2. Conduction: is the flow of heat between parts of a substance by molecular vibrations. The flow can also be from one substance to another substance in direct contact.

 Convection: is the movement of heat from one place to another by way of fluid or air. [17].

4.3.2 Ground Characteristics

The definition of geothermal energy is subject to variation, in some cases it is considered to be heat below 15-20m in the ground while in others simply all energy stored as heat beneath the earth's surface. Regardless of definition this relatively constant store can be utilized by a heat pump for heating and cooling applications since in winter the ground temperature will be above the average air temperature while in the summer it is likely to be below it (see Figure 4.5).

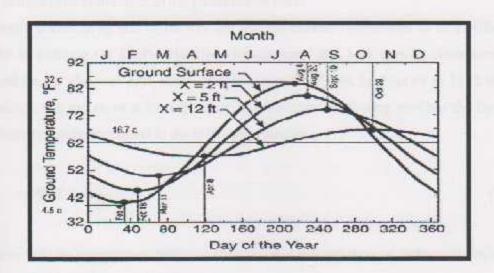


Figure 4.5: Typical Ground Temperature change around the year

The capacity of the GSHP for heating and cooling will depend on not just the size of the system but also the thermal properties of the ground system performance is significantly affected by the material in which the ground heat exchanger (loop) is laid. Factors which will determine performance are:

- Subsurface temperature.
- 2. Thickness and nature of superficial deposits i.e. soil.
- Rock properties i.e. stratigraphy (formation) and lithology (type).
 These will determine strength and conductivity.
- 4. Hydrological issues, depth to groundwater, seasonal variations in Groundwater temperature, flow direction etc. For vertical type geothermal heat pumps "In general groundwater flow improves heat exchange", when significant flow is present, at 4-10°C heat exchange occurs through a dual mechanism of conduction in the aquifer material and convection in the groundwater itself.

Thermal conductivity and diffusivity are two parameters which need to be clarified in order to estimate the likely subsurface temperatures and heat transfer characteristics. Based on the classical heat conduction equation developed by Fourier in 1822 which considers the soil to be a homogeneous and isotropic conducting medium the thermal diffusivity can be expressed in the following equation:

$$\alpha \nabla^2 T = \frac{dT}{dt} \tag{4.1}$$

Where T is the temperature (°K), t is time (s), and α is the thermal diffusivity (m²/s) of the conducting medium and defined by

$$\alpha = \frac{k}{\rho C_p} \tag{4.2}$$

Where k is the thermal conductivity (W/(m. $^{\circ}$ K), ρ is the density (kg/m 3). And C_{p} is the mass specific heat capacity (J/(kg. $^{\circ}$ K). The higher the value of α the faster the propagation of heat within the medium [16].

4.3.2.1 Thermal conductivity (k)

Thermal conductivity is the quantity of rate of heat transmitted per unit area, per unit temperature gradient under steady state conditions. By Multiplying this factor by the thermal gradient will give the heat flow within the ground.

Generally rocks have higher k values than soils. Variability in the latter is explained due to mixing of mineral and organic particles and their associated thermal characteristics. Furthermore in dry soils air is trapped, and since this has a low k value, saturation will raise the conductivity of soils; "Low conductivity soil may require as much as 50% more collector loop than highly conductive soil" [17].

4.3.2.2 Thermal Diffusivity

Thermal diffusivity is the ground thermal conduction in relation to thermal capacity. This links thermal conductivity, specific heat (Cp) and density (ρ). Density is multiplied by specific heat is termed volumetric heat capacity. A high thermal diffusivity value is desirable since this means the material will quickly adjust temperature to that of the surrounding environment since heat is conducted rapidly relative to thermal mass.

4.4 Vertical Loop Concept

4.4.1 Formulas and Concept

One of the fundamental tasks in the design of a reliable GCHP system is properly sizing the ground-coupled heat exchanger length (i.e. depth of boreholes).

The task of sizing the ground-loop heat exchanger was accomplished using rules of thumb (i.e. 250 feet of bore length per ton of heating or cooling capacity) according to ASHREA but this is of course depends on several things of which, the location, the depth and size of the excavation, the time of the year, the soil diffusivity of heat, the heat pump design conditions, the fluid, the pipes type and thermal properties, the flow type and velocity which is relevant to the pump selection of flow and head, the ground water, the percentage of water content in soil, and many other factors.

To design the loop underground several factors were taken into consideration of which:

A. The fluid used was water because it has high heat capacity. From tables of properties of refrigerant R410a which is used in the heat pump, it can be seen that the condenser unit rejects the heat at 75 °C in summer and absorbers heat in the vicinity of the evaporator at 2-4 °C because the outdoor design temperature is 35 °C for cooling in summer and 0 °C for heating in winter. The outdoor temperature should be less than 35° C in summer and more than 0 °C in winter to achieve better performance.

Water is excellent for applications that are above freezing point and below boiling point. But in cold weathers fluids will have to withstand a temperature below freezing point of water, in this case adding antifreeze will be the solution and the performance will drop a little bit but the system will not be damaged because of freezing the water in the heat exchanger. Antifreeze should be added to the water in case of lower temperature which is not our case. Table 4.1 below shows several types of solutions that can be added to water to prevent freezing [18].

Using the formula:

$$Q[kW] = \dot{m} \left[\frac{L}{s} \right] * Cp \left[\frac{kJ}{kg^{\circ}C} \right] * \rho \left[\frac{kg}{L} \right] * \Delta T[^{\circ}C]$$
 (4.3)

Table 4.1: Densities and Specific Heats for Various Solutions

	% by Weight	Mean Temp (°C)	Freezing Point (°C)	Density (kg/m ³)	Specific Heat (kJ/°K*kg)
Pure Water	100	25	0	999.6	4.184
	13.6	25	-9.4	980.2	4.232
Methanol	10.0	30	-6.7	904.2	4.274
Solution	6.3	35	-3.9	989.0	4.296
	2.0	40	-1.1	989.4	4.275
	20.0	25	-9.4	1034.4	3.848
Ethylene	14.6	30	-6.7	1024.4	3.975
Glycol Solution	8.8	35	-3.9	1017.3	4.100
	2.5	40	-1.1	1002.9	4.190
Danasalana	23.5	25	-9.4	1024.5	4.023
Propylene	18.3	30	-6.7	1017.3	4.065
Glycol	12.9	35	-3.9	1012.5	4.107
Solution	5.9	40	-1.1	1005.3	4.149
Sodium	13.3	25	-9.4	1103.6	3,627
Chloride	10.1	30	-6.7	1077.2	3.688
Solution	6.4	35	-3.9	1048.4	3.847
Calcium	14.3	25	-9.4	1134.7	3.332
Chloride Solution	11.3	30	-6.7	1103.6	3.499

B. Pipe Type: Pipes are either steel for vertical design, or High density polyethylene for horizontal design, for leakage problems steel pipes are not used. HDPE pipes are defined by their pressure ratings which can be measured by the Standard Dimension Ratio – SDR [19].

It is common to use the SDR as method of rating pressure piping as seen in the Figure (4.6) where S is the thickness of the pipe and D is the outer diameter of the pipe. Then SDR is:

$$SDR = \frac{D}{S} = \frac{Dlameter}{Thickness}$$
 (4.4)



Figure 4.6: Standard Dimension Ratio descriptions

All properties for the pipe are now known such as thickness, material, so the heat conducted through pipes is now known as in Tables (4.2) [20].

Table 4.2: Minimum Required Flow Rate (L/min) for Non laminar Flow Re>3000

		T = -	1°C			T = 1	0 ° C			
Fluid	Non		meter SI ipe)R 11	No	Nominal Diameter SDR 11 Pipe				
(% by weight)	3/4 in. (20	1 in. (25 mm)	1 1/4 in. (32	1 1/2 in. (37.5 mm)	3/4 in. (20 mm)	1 in. (25 mm)	1 1/4 in. (32	1 1/2 in. (37.5 mm)		
20% Ethanol	14.3	18.2	22.7	26.1	9.8	12.1	15.1	17,4		
20% Ethylene Glycol	9.5	11.7	14.8	17.0	6.8	8.4	10.6	11.7		
20% Methanol	11.0	13.6	17.0	19.7	7.6	9.5	11.7	13.2		
20% Propylene Glycol	12.9	15.9	20.4	23.1	8.7	10.6	13.6	15.5		
20% Calcium Chloride	8.6	11.0	13.6	15.5	5.3	7.6	8.4	9.7		
Water	**	***	**	-	4.2	5.3	6.5	7.6		

C. Soil: Ground temperature is changing according to the geographical location, the time of the year, time after being disturbed, type and the depth in the ground. The type of soil is a determinant factor because different soils have different thermal conductivities and different thermal diffusivity. Moisture content affects the diffusivity and conductivity all this is shown in table (4.3) and table (4.4) [20].

Table 4.3: Thermal Properties of Rocks at 25°C

Rock Type	% Occurrenc e in Earth's Crust*	k - All** Thermal Conductivity (W/m.K)	k - 80%*** Thermal Conductivity (W/m.K)	e p Specific Heat (J/kg.K)	ρ Density (kg/m³)	α(k/ρCp) Thermal Diffusivity m²/day
Dense Rock	-	3.46	***	840	3200	0.111
Average Rock	-	2.42	42	840	2800	0.089
Dense Concrete	-	1.73	-	840	2400	0.073
Heavy soil, Saturated	-	2,42		840	3200	0.078
Solid	-	1.3		880	2290	0.056
Heavy soil, Damp		1.3		960	2100	0.056
Heavy soil, Dry	nie .	0.87	-	840	2000	0.045
Light soil, Damp	-	0.87		1050	1600	0.045
Light soil, Dry		0.35	MIGINE IN	840	1440	0.024

^{*} Percentage of sedimentary rocks is higher near the surface.

^{** &}quot;All" represents the conductivity range of all samples tested.

^{*** &}quot;80%" represents the mid-range for samples of rock.

Table 4.4: Thermal Conductivity and Diffusivity of Sand and Clay Soils

Soil	Dry	500 3	Moist	10%	Moist	15% 1	Moist	20%	Moist
Type	Density (kg/m³)	k (W/m K)	c (m²/day)	k (Wim K)	(m ² /day)	k (W/m K)	cm ² /day	k (W/m K)	(m²/day)
Coarse 100% Sand	1900	2.1-3.3	0.089-	2.4-3.5	0.086-	2.8-3.8	0.085-	•	-
	1600	1.4-2.4	0.072-	2.1-2.6	0.089-	2.3-2.8	0.083-	2.4-2.9	0.078- 0.093
	1300	0.9-1.9	0.056- 0.12	1.0-1.9	0.056-	1.0-2.1	0.047-	1.2-2.1	0.048+ 0.083
Fine Grain	1900	1.0-1.4	0.045-	1.0-1.4	0.037-	1.4-1.9	0.043-	*	
100% Clay	1600	0.9-1.0	0.045-	0.9-1.0	0.037- 0.045	1.0-1.2	0.034-	1.0-1.4	0.038-
	1300	0.5-0.9	0.033- 0.056	0.6-0.9	0.033- 0.047	0.7-	0.032- 0.044	0.7-1.0	0.028- 0.042

^{*} Values indicate ranges predicted by five independent methods. k = Thermal Conductivity, α = Thermal Diffusivity, Coarse Grain= 0.075 to 5mm - Fine Grain less than 0.075mm (0.075mm = #200 U.S. Standard Sieve

A vertical GCHP (see Figure 4.7) generally consist of two small-diameter, high-density polyethylene (HDPE) tubes placed in a vertical borehole that is subsequently filled with a solid medium. The tubes are thermally fused at the bottom of the bore to a close return U-bend. Vertical tubes range from 20 to 40 mm nominal diameter. Bore depths range from 15 to 180 m, depending on local drilling conditions and available equipment. Boreholes are typically 100 to 150 mm in diameter for single and double loop.

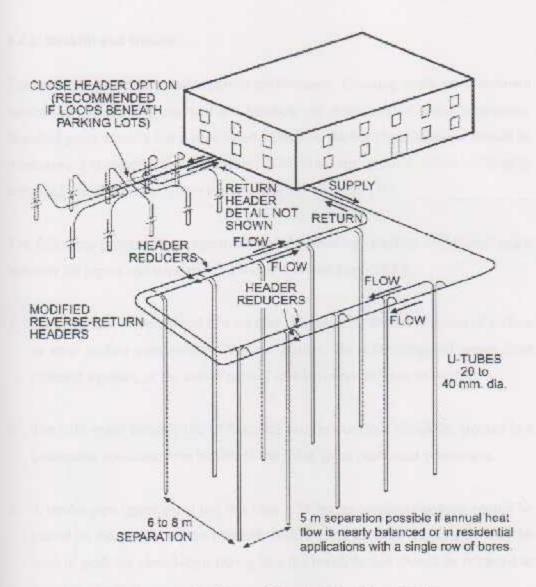


Figure 4.7: Vertical Ground-Coupled Heat Pump Piping

To reduce thermal interference between individual bores, a minimum borehole separation distance of 6 m is recommended when loops are placed in a grid pattern. This distance may be reduced when bores are placed in a single row, the annual ground load is balanced (i.e., energy released in the ground is approximately equal to the energy extracted on an annual basis), or water movement or evaporation and subsequent recharge mitigates the effect of heat build-up in the loop field [13].

4.4.2 Backfill and Grouts

The backfill also plays a major part in performance. Grouting is the most common material for backfill. It can seal the borehole off from surface water penetration. Standard grout actually has a poor conductivity, so the bore hole diameter should be minimized (Approximately 5" diameter) to limit the grout's affect. Thermally enhanced grouts have been developed to address this issue [21].

The following provisions are recommended for grouting (sealing) of the void space between the piping and borehole of a Vertical closed-loop (VCL):

- Grouting is to be completed in a manner that prevents the introduction of surface or near surface contaminants into an aquifer, the interchange of water from different aquifers, or the loss of natural artesian pressure from an aquifer.
- The void space between the VCL piping and the borehole should be grouted in a continuous operation from bottom to top using grout placement procedures.
- 3. A tremie pipe (grout pipe) not less than 1.25 inches nominal diameter should be placed to the bottom of the borchole before grouting. The tremie pipe may be used to push the closed-loop piping into the borehole and should be retracted as grouting proceeds.
- 4. Grout should be pumped through the tremie pipe until the density of the grout flowing from the borehole at the ground surface equals the density of the grout being pumped in.
- Grout manufacturers' product specifications should be followed when mixing and pumping grout.

4.5 In-Situ Thermal Conductivity Tests

Ground testing provide the designer with accurate information on the thermal conductivity. With this information, the loop design can be optimized (in most cases) and the length of piping reduced. If the bidding contractors will test bore data and drilling conditions on the site, this will remove some of the uncertainty and they may a provide a price with less of a hedge in it.

The test are generally connected by drilling a bore hole and adding a loop. Hot water from portable eclectic heater is circulated as shown in Figure 4.8.

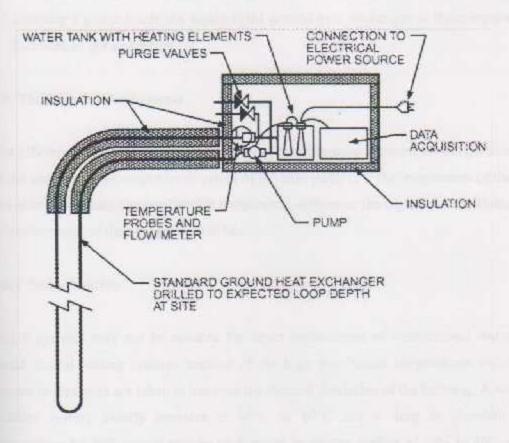


Figure 4.8: Thermal Properties Test Apparatus

We take a specifications to enhance reported accuracy, that are include [22]:

- Test duration should be 36 to 48 hours.
- Heat input rate should be 15 to 25 W for each foot of borehole depth.
- The input electric power to the heater should have a standard deviation of less than ±1.5% of the average value and the peaks less than ±10% of the average.
- After the ground loop is installed with grout, a five-day waiting period should elapse before starting a test in low-thermal conductivity soils [k<1.0 Btu/hr-ft-°F(1.7 W/m.°C)]. In more conductive soils a three-day waiting period is recommended.
- At the end of the waiting period the ground temperature should be measured by inserting a probe inside the liquid-filled ground heat exchanger at three vertical locations to get an average.

4.6 The Distribution Systems

The efficiency of a heat pump is a function of the difference between the temperature of the source and the output temperature of the heat pump (i.e. the temperature of the distribution system). The smaller this temperature difference the higher the coefficient of performance of the heat pump will be.

4.6.1 Space heating

Table 20°C would require an increase in emitter surface of 30% to 40% to to the same heat output.

Table 4.5 shows the supply temperatures required for a range of domestic heating distribution systems.

Table 4.5: Typical delivery temperatures for various heating distribution systems

Distribution system	Delivery temperature °C				
Underfloor heating	30-45				
Low temperature radiators	45-55				
Conventional radiators	60-90				
Air	30-50				

For new housing where high insulation levels result in low heating demand, low temperature air distribution systems, low temperature water-based systems or under floor heating are all possible options. The most efficient type of space heating to use with a GSHP system is underfloor heating.

The thermal capacity of the distribution system is important. If it is too low the heat pump may suffer from artificially long off periods at times of light load. This effect is partly due to the presence of a restart delay (designed to reduce wear on the compressor by preventing rapid on/off cycling) in the heat pump.

4.6.2 Space Cooling

Most water-to-air heat pumps are reversible so a forced air distribution system can madily be adapted to provide cooling as well as heating. A reversible water-to-water pump coupled to an under floor distribution system can also be designed to supply space cooling in summer. Even with water-to-water heat pumps designed for making only, a limited amount of 'passive' summer cooling can be provided by the use of the ground loop for example by by-passing the heat pump, and making fluid from the ground coil through a fan convector.

CHAPTER FIVE

THEORITICAL DESIGN AND CALCULATIONS

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- 5.1 Introduction
- 5.2 Cooling Load
- 5.3 Heating Load
- 5.4 Duct Design
- 5.5 Fan Selection
- 5.6 Summer Air Conditioning and Winter Warm Air Heating System
- 5.7 Earth Connection Closed loop Ground Heat Exchangers (GHX)
- 5.8 System Comparison and Payback Period

Chapter Five

Theoretical Design And Calculations

5.1 Introduction

The designer must perform his normal tasks, such as zone-by-zone load analysis. In addition, he must also specify the geothermal type, total bore length, minimum separation distance, pipe diameter, U-bend diameter, operating parameters and antifreeze properties. This chapter will provide the designer with some details on how to solve these issues.

5.2 Cooling Load

5.2.1 Data of Project

Correction of latitude is 32°

All data and calculation are taken in august.

$$T_{out} = 24 \, ^{\circ}\text{C}$$

$$T_{out} = 34 \, ^{\circ}\text{C}$$

$$T_{out} = T_{out} - \frac{DR}{2}$$
(5.1)

Where T_l is the room design temperature, T_{out} is the outdoor temperature, T_{om} is the measure mean temperature. DR is the daily range temperature. [23]

$$T_{ave,max} - T_{ave,min} = 40 - 31.5 = 8.5 \, ^{\circ}\text{C}$$

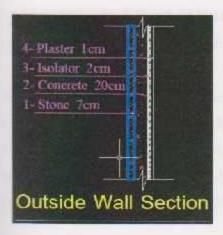
$$T_{ave} = (34 - \frac{8.5}{2}) = 29.75 \, ^{\circ}\text{C}$$

5.2.2 Heat Gain Through Sunlit Walls

Construction of the wall:

(Stone) + (Concrete) + (Insulation) + (Plastering) see Figure & Table (5.1).

Calculation of overall heat transfer coefficient (U) for external wall as follow:



k W/m.°C	Thickness m	Layer
2.2	0.07	Hard Stone (1)
1.75	0.20	Concrete (2)
0.034	0.02	Polystyrene (3)
0.72	0.01	Cement plaster(4)

Table 5.1: Outside wall Component

Figure 5.1: Outside wall section

$$U = \frac{1}{\left(\frac{1}{hfin}\right) + \left(\frac{\Delta x}{ks}\right) + \left(\frac{\Delta x}{kc}\right) + \left(\frac{\Delta x}{ki}\right) + \left(\frac{\Delta x}{kp}\right) + \left(\frac{1}{hfout}\right)}$$
(5.2)

Where ks Thermal conductivity of stone, kc is thermal conductivity of concrete, kp is thermal conductivity of cement plaster, ki is thermal conductivity of polystyrene, hf_{in} is the convection coefficient of inside air, hf_{out} is the convection coefficient of outside air.

So:

$$U = \frac{1}{\left(\frac{1}{8.33}\right) + \left(\frac{0.07}{2.2}\right) + \left(\frac{0.2}{1.75}\right) + \left(\frac{0.02}{0.034}\right) + \left(\frac{0.01}{0.72}\right) + \left(\frac{1}{16.66}\right)}$$

U = 0.96 W/m, °C

$$\dot{Q} = U * A * \Delta T \tag{5.3}$$

Where A is the area of the wall and ΔT is the total equivalent temperature difference, which takes into consideration the increase of wall temperature due to absorption of solar radiation. The values of ΔT are called cooling load temperature differences CLTD. The value of CLTD taken from Table (A-2) needs to be corrected and can be calculated from the following equation:

$$(CLTD)_{corr} = (CLTD + LM)k + (25.5 - T_l) + (T_{am} - 29.4)f$$
 (5.4)

Where LM is latitude correction factor, which can be obtained from Table (A-3) for horizontal and vertical surfaces, the factor k is color adjustment factor such that k = 1 for dark colored roof, k = 0.5 for permanently light colored roofs, k = 0.65 for permanent light color walls, and the factor f is attic fan factor such that f = 1, if there is no attic or roof fan; f = 0.75, if there is an attic or roof fan.

The heat transfer rate through sunlit walls or sunlit roof is calculated form the following equation:

$$Q = U * A * (CLTD)_{corr}$$
 (5.5)

And we can show these calculations for ground floor, first, second, and third floor in Table (5.2), means we have the same combination of internal, and external walls for each floor, for details about building see Figure (A-35), and (A-36).

Table 5.2: Ground, first, second, and third floor (Wall)

Component	Direction	LM	CLTD	(CLTD)corr.	A(m ²)	Q(W)
BDR1	N	-1.1	0	1.135	10.04	11.39
BDRI	W	0.0	1	2.5	9.95	24.87
Bath1	N	-1.1	0	1.135	4.7	6.34

Component	Direction	LM	CLTD	(CLTD)corr.	A(m ²)	$\hat{Q}(W)$
Bath1	E	0.0	12	9.65	7.5	72.37
BDR2	W	0.0	1	2.5	9.95	24.87
BDR3	W	0.0	1	2.5	9.95	24.87
BDR3	S	0.5	9	8.025	11.08	100
Bath2	S	0.5	9	8.025	4.7	37.7
Bath2	E	0.0	12	9.65	6.9	66.58
Lobby	S	0.5	9	8.025	6.51	52.24
Kitchen	w	0.0	1	2.5	7.5	18.75
Kitchen	S	0.5	9	8.025	9.58	76.9
Kitchen	E	0.0	12	9.65	9.88	95.34
Dining	E	0.0	12	9.65	6.3	60.8
Salon	S	0.5	9	8.025	2.4	19.26
Salon	E	0	12	9.65	11.38	109,8
Salon	N	-1.1	0	1.135	8.38	9.51
Bath3	N	-1.1	0	1.135	3.2	3.63
Bath3	W	0.0	1	2.5	7.5	18.75

5.2.3 Heat Gain Through Ceiling (\dot{Q}_{ce}) and Floor (\dot{Q}_f)

$$Q_f = U_{floor} * A * \Delta T \tag{5.6}$$

$$Q_{ce} = U_{ce} * A * (CLTD)_{corr}$$
 (5.7)

$$\Delta T = (T_{out} - T_{in})$$

 $U_{floor} = 2.328 W/m^2$. °C this value taken from Table (A-15)

 $U_{ce} = 1.08 W/m^2$. °C this value taken from Table (A-16)

Tables (5.3) shows these calculations for ground and third floor because there is no ground or ceiling for first, and second floor.

Table 5.3: Ground and Third floor (Floor, Ceiling)

Component	A (m ²)	Q _{Boor} (W)	(CLTD) corr	Q _{cci} (W)
BDR1	BDR1 19.6		16	338.7
Bath I	9.25	75.37	16	159.84
BDR2	17.6	143.4	16	304.13
BDR3	18.4	150	16	317.95
Bath2	3.91	31.86	16	67.56
Lobby	21.45	174.8	16	370.65
Kitchen	19.8	161.3	16	342.14
Dining	11.05	90	16	190.94
Salon	20	163	16	345.6
Bath3	3	24.4	16	51.84

5.2.4 Heat Transmitted Through Glass

5.2.4.1 Construction of the glass

Selection data:

- Double glass
- Regular double
- U_{gt} = 3.2 W/m². °C this value taken from Table (A-4)

The total cooling load due to exposed glass area is the sum of transmission load due to inside-outside glass surface temperature difference (heat conduction) and heat gain due to solar energy (heat convection).

1- The Transmitted cooling load can be calculated from equation:

$$\dot{Q}_{tr} = A(SHG)(SC)(CLF) \tag{5.8}$$

Where A is the area of the glass, (SHG) is the solar heat gain factor and can be taken from Table (A-5), (SC) is the cooling load factor and can be taken from Table (A-6), (CLF) is the cooling load factor and can be taken from Table (A-7) [33].

2- The Convective cooling load can be calculated from equation:

$$Q_{conv} = U * A * (CLTD)_{corr.}$$
(5.9)

Where CLTD is the value of the cooling load temperature difference for the glass and can be taken from Table (A-2).

Table (5.4) shows these calculations for ground, first, second, and third floor are the same as follows:

Table 5.4: Ground, First, Second, and Third floor (Glass)

Comp.	Direction	A(m²)	(CLTD)corr.	SHG	SC	CLF	Qυ	Q conv.	Q total
BORI	N	3	7.75	117	0.51	0.86	153.5	74.4	228.35
BORI	W	2.25	8.85	691	0.51	0.53	420.25	63.72	483.97
Buth 1	N	0.45	7.75	117	0.51	0.86	23.1	11.16	34.36
BOR2	w	2.25	8.85	691	0.51	0.53	420.25	63.72	483.97
HD83	W	2.25	8.85	691	0.51	0.53	420.25	63.72	483.97
BDR3	S	3	9.35	350	0.51	0.68	364.14	89.76	453.9
Birth2	S	0.45	9.35	350	0.51	0.68	364.14	13.46	377.6
Lifey	S	2.25	9,35	350	0.51	0.68	364.14	67.32	431.46
Elizhen	S	3.15	9.35	350	0.51	0.68	364.14	94.25	458.4

Comp.	Direction	A(m²)	(CLTD) _{mer}	SHG	SC	CLF	\dot{Q}_{ir}	$\dot{Q}_{ m conv}$	\dot{Q}_{total}
Kitchen	Е	3.15	8.85	691	0.51	0.22	244.22	89.21	333.43
Salon	Е	3.15	8.85	691	0.51	0.22	244.22	89.21	333.43
Salon	N	3.15	7.75	117	0.51	0.86	161.64	78.12	239.76
Bath3	Ñ	0.45	7.75	117	0.51	0.86	23.1	11.16	34.26

5.2.5 Heat Gain Through Ventilation, Light, and Door

5.2.5.1 For Ventilation (\hat{Q}_{vent})

The amount of the outside air needed for ventilation depends on the type of application, see Table (A-9).

5.2.5.2 For Light (Qught)

$$Q_{light} = P_l * A * (CLF)_{Lt}$$
(5.10)

Where P_l is the lamp rated power in watts, A is the area of room, $(CLF)_{Lt}$ is the light cooling load factor. Table (A-10) gives the light cooling load factor for two types of fixture arguments. [23]

5.2.5.3 For Door (\dot{Q}_{door})

 $Q = UA\Delta T$

 $U = 7 W/m^2$. °C this value taken from Table (A-18)

 $\Delta T = 34 - 24 = 10^{\circ}$ C

Table (5.5) shows these calculations for ground, first, second, and third floor are the same as follows:

Table 5.5: Each Floor (Ventilation, Light, Door)

Component	Q _{vent} (W)	Quant (W)	Q _{door} (W)	
BDR1		405.7	141.7	
Bath1	1620	84	-	
BDR2		385	_	
BDR3		381		
Bath2	1620	73	-	
Lobby			141.7	
Kitchen	then 570 434		_	
Dining	-	229	189	
Salon		414		
Bath3	1540	56	_	

5.2.6 Heat Gain Through Occupants and Equipment

5.2.6.1 For Equipment (\dot{Q}_{squip})

Sensible and latent heat arising from various equipment and appliances that are installed in a conditioned space are given in Table (A-13).

5.2.6.2 For Occupants (Qoccup)

The heat gain through Occupants can be calculated from equation:

$$Q_{sccup} = n * \dot{Q}_s * CLF_{occup} + n * \dot{Q}_L$$
 (5.11)

Where $\hat{Q}_{\mathcal{S}}$ is the sensible heat and can be taken from Table (A-14), n is the number of person, CLF_{accup} is the cooling load factor and can be taken from Table (A-11), $\hat{Q}_{\mathcal{L}}$ is the latent heat. [23]

Table (5.6) shows all these calculations for ground, 1st, 2nd, and 3rd floor.

Table 5.6: Each Floor (Equipment, Occupants)

Component	Q _{equip} (W)	Q _{occup} (W)
BDRI	1245	267.4
Bath1	1465	86
BDR2	995	258
BDR3	650	258
Bath2	1065	86
Lobby	250	687
Kitchen	3190	344
Dining		514
Salon		258
Bath3		86

5.2.7 Heat Gain Through Infiltration (Qinf)

The cooling load due to infiltration is given by the following equation:

$$Q_{inf} = \rho * C_p * \dot{V}_f * (T_{cut} - T_{in})$$
(5.12)

Where \dot{V}_f is the volumetric flow rate of infiltration air, C_p is the specific heat at constant pressure, and ρ is the density of infiltration air. [23]

If the density of air which is 1.25 kg/m³, and its specific heat at constant pressure 1900 J/kg.K are substituted eq. (5.12), then

$$Q_{inf} = \left(\frac{1250}{3600}\right) * \dot{V}_f * (T_{in} - T_{out})$$
 (5.13)

$$T = 34 - 24 = 10$$
°C

= V + Air changes per hour

Where V is the volume of the room, and Air changes per hour is given in Table (A-17).

Table (5.7) shows all these calculations for ground, 1st, 2nd, and 3rd floor.

Table 5.7: Each Floor (Infiltration)

Component	V(m³)	Air Change/hour	\dot{Q}_{inf} (W)	
BDR1	58.8	1.5	306.25	
Bath1	52.8	1	183.3	
BDR2	55.2	1.5	287.5	
BDR3	11.73	2	81.2	
Bath2	64.35	2	446,5	
Lobby	59.35	2	412.5	
Kitchen	33.15	2	230.5	
Dining	60	2	416.7	
Salon	9	3	93.7	
Bath3	12.75	3	133	

5.2.8 Total Cooling Load

5.2.8.1 Total Cooling Load of Ground Floor

 $\hat{Q}_{Total} = \dot{Q}_{wall} + \dot{Q}_{Glass} + \dot{Q}_{floor} + \dot{Q}_{inf} + \dot{Q}_{door} + \dot{Q}_{v} + \dot{Q}_{l} + \dot{Q}_{equ} + \dot{Q}_{oc}$ (5.14) Table (5.8) shows all these calculations for ground floor.

Table 5.8: Ground Floor Total

Component	$\dot{Q}_{sens}(W)$	Q _{laten} (W)	Qtotal(W)	
BDR1	2518.4	272	2790.4	
Bath1	3594.6	32	3626,6	
BDR2	2676.47	64	2738.47	
BDR3	2518.9	64	2582.9	

Component	Q _{sens} (W)	$\hat{Q}_{laten}(W)$	Qtotal(W)	
Bath2	3808	32	3840	
Lobby	2588.6	96	2684.6	
Kitchen	5282	630	5912	
Dining	1378.8	120	1498.8	
Salon	1883.1		1883.1	
Bath3	1774	32	1806	
Sum	28026.3	1342	29368.3	

5.2.8.2 Total Cooling Load of First and Second Floor

 $Q_{Total} = \hat{Q}_{wall} + \hat{Q}_{Glass} + \hat{Q}_{inf} + \hat{Q}_{door} + \hat{Q}_{v} + \hat{Q}_{l} + \hat{Q}_{equ} + \hat{Q}_{oc}$ (5.15) Table (5.9) shows all these calculations for first floor, and the same total for second floor.

Table 5.9: First Floor Total

Component	$\dot{Q}_{sens}(₩)$	Q _{laten} (W)	Qtotat(W)	
BDR1	23.58.66	272	2630.66	
Bath1	3519.1	32	3551.1	
BDR2	2531.1	64	2595.1	
BDR3	2368.9	64	2432.9	
Bath2	3776	32	3808	
Lobby	2418.8	96	2514.8	
Kitchen	nen 5120.7 630		5750.7	
Dining	ng 1288.8 120		1408.8	
Salon	n 1720 —		1720	
Bath3	1749.6	32	1781.6	
Sum	26851.66	1342	28193.66	

5.2.8.3 Total Cooling Load of Third Floor

 $\dot{Q}_{Total} = \dot{Q}_{wall} + \dot{Q}_{Glass} + \dot{Q}_{ciel} + \dot{Q}_{inf} + \dot{Q}_{door} + \dot{Q}_{v} + \dot{Q}_{l} + \dot{Q}_{equ} + \dot{Q}_{oc}$ (5.16)
Table (5.10) shows all these calculations for third floor.

Table 5.10: Third Floor Total

Component	$\dot{Q}_{sens}(\mathrm{W})$	Q _{iasen} (W)	Qtotat(W)	
BDR1	2697.4	272	2969.4	
Bath1	3679	32	3711	
BDR2	2835	64	2899	
BDR3	2686.8	64	2750.8	
Bath2	3853.5	32	3875.5	
Lobby	2789.5	96	2885.5	
Kitchen	5462.8	630	6092.8	
Dining	1479.7	120	1599.7	
Salon	alon 2065.6 —		2065.6	
Bath3	1801.4	32	1833.4	
Sum	29340.72	1342	30682.72	

$$Q_{tot}$$
 Cooling of Building = $Q_{tot1} + +Q_{tot2} + Q_{tot3} + Q_{tot4}$
= $29368.3 + 28193.66 + 28193.66 + 30682.72$
= 116438.34 W

$$Q_{tot}$$
 Design of Building = 116438.34 * 1.1

= 128082.17 W

5.3 Heating load

5.3.1 Heat Loss Through Walls

We can calculate the heat loss through walls by:

$$\dot{Q}_{wall} = UA\Delta T$$
 (5.17)

Where U is the over heat transfer coefficients (0.96W/m².°C) which is calculated in equation (5.2), A is the area of the wall and ΔT is the total temperature difference.

$$\Delta T = (T_{tn} - T_{out})$$

Where T_{in} is the room design temperature (24°C) and T_{out} is the outdoor design temperature (4°C).

$$\Delta T = 24 - 4 = 20^{\circ}$$
C

Table (5.11) shows all these calculations for ground, 1st, 2nd, and 3rd floor.

Table 5.11: Ground, 1st, 2nd, and 3rd floor (Wall)

Component	Direction	Area (m²)	Qwall(W)	
BDR1	W	9.95	199	
BDR2	W	9,95	199	
BDR3	W	9.95	199	
BDR3	S	11.08	236	
Bath2	S	4.7	94	
Bath2	E	6.9	138	
Lobby	S	6.51	130.2	
Kitchen	W	7.5	150	
Kitchen	S	9.58	191.6	
Kitchen	E	9.88	197.6	
Diming	E	1.46	29.2	
Salon	Е	11.38	227.6	
Salon	N	8.38	167.6	
Bath3	N	3.2	64	

Component	Direction	Area (m²)	ģ (W)	
Lobby	N	5.82	116.4	
Bath1	N	4.7	94	
BDR1	N	10.04	200.8	
Salon	S	2.4	48	
Bath	Е	7.5	150	
Bath3	W	7.5	150	

5.3.2 Heat Loss Through Glass

The total heating load due to exposed glass area is:

$$\hat{Q}_{glass} = UA\Delta T \tag{5.18}$$

Where U is the overall heat transfer coefficients (3.2 W/m^2 . °C)

$$\Delta T = 24 - 4 = 20$$
°C

Table (5.12) shows all these calculations for ground, 1^{st} , 2^{nd} , and 3^{rd} floor.

Table 5.12: Ground, 1st, 2nd, and 3rd floor (Glass)

Component	Direction	Area (m ²)	$\dot{Q}(W)$
BDR1	W	2.05	131.2
BDR2	W	2,05	131.2
BDR3	W	2.05	131.2
BDR3	S	2.72	174.08
Bath2	S	0.4	25.6
Lobby	S	2.05	131.2
Kitchen	S	3.02	193,28
Kitchen	Е	3.02	193.28
Salon	Е	3.02	193.28
Salon	N	3.02	193.28
Bath3	N	0.4	25.6
Bath1	N	0.4	25.6
BDR1	N	2.72	174.08

5.3.3 Heat Loss Through Floor and Ceiling

$$\dot{Q}_f = U_f * A * \Delta T_f \tag{5.19}$$

$$\dot{Q}_{ce} = U_{co} * A * \Delta T_{cei}$$
 (5.20)

$$\Delta T_f = (T_{in} - T_{out})$$

$$\Delta T_f = 24 - 10 = 14 \, ^{\circ}\text{C}$$

$$\Delta T_{cei} = (T_{in} - T_{out})$$

= 24 - 10 = 14 °C

 $U_f = 2.328 \, W/m^2$. °C this value taken from Table (A-15)

 $U_{ce} = 1.08 \, W/m^2$, °C this value taken from Table (A-16)

Table (5.13) shows these calculation for ground and third floor because there is no ground or ceiling for first, and second floor.

Table 5.13: Ground and Third floor (Floor, Ceiling)

Component	Area (m ²)	Qneer (W)	Q ceiling (W)
BDR1	19.6	456.3	423.36
Bath1	4.25	98.94	91.8
BDR2	17.6	409.73	380.16
BDR3	3 18.4 428.35		397.44
Bath2	3.91	91.03	84.45
Lobby	21.45	499.35	463.32
Kitchen	19.8	460.94	427.68
Dining	ing 11.05 257.24		238.68
Salon	20	465,6	432
Bath3	3	69.84	64.8

5.3.4 Heat Loss Through Infiltration

The heat load due to infiltration is given by the following equation:

$$\dot{Q}_{inf} = \left(\frac{1250}{3600}\right) * \dot{V}_f * (T_{in} - T_{out})$$
 (5.21)

 $\Delta T = 24 - 4 = 20$ °C

 $\dot{V}_f = V * Air changes per hour$

Table (5.14) shows all these calculations for ground, 1st, 2nd, and 3rd floor.

Table 5.14: Ground, 1st, 2nd, and 3rd floor (Infiltration)

Component	V (m ³)	Air Change/hour	ΔT°C	Qinf (W)
BDR1	58.8	1.5	20	612.5
Bath1	12.75	3	20	265.6
BDR2	52.8	1	20	366.64
BDR3	55.2	1.5	20	574.96
Bath2	11.73	2	20	162.9
Lobby	64.35	2	20	896
Kitchen	59.4	2	20	824.94
Dining	33.15	2	20	460.38
Salon	60	2	20	833.28
Bath3	9	3	20	187.48

5.3.5 Heat Loss Through Door

$$Q_{door} = UA\Delta T (5.22)$$

 $U = 7 W/m^2$. °C this value taken from Table (A-18)

 $\Delta T = 24 - 4 = 20$ °C

Table (5.15) shows these calculations for ground, first, second, and third floor are the same as follows:

Table 5.15: Each Floor (Door)

Component	Direction	A (m ²)	Q _{door} (W)
Lobby	S	2.02	283.5
Dining	E	2.7	378
Lobby	N	2.4	336
BDRI	N	2.02	283.5

5.3.6 Total Heating Load

5.3.6.1 Total Heating Load of Ground Floor

$$\dot{Q}_{Total} = \dot{Q}_{wall} + \dot{Q}_{Glass} + \dot{Q}_{floor} + \dot{Q}_{inf} + \dot{Q}_{door}$$
 (5.23)

Table (5.16) shows all these calculations for ground floor.

Table 5.16: Ground Floor Total

Component	Q _{total} (W)	
BDR1	2057.38	
Bath	634.14	
BDR2	1106.57	
Bath3	1743.6	
Bath2	511.53	
Lobby	2276.25	
Kitchen	2211.64	
Dining	1124,82	
Salon	2128.64	
Bath3	496.92	
Sum	14291.5	

5.3.6.2 Total Heating Load of First Floor

$$\dot{Q}_{Total} = \dot{Q}_{wall} + \dot{Q}_{Glass} + \dot{Q}_{inf} + \dot{Q}_{door}$$
 (5.24)

Table (5.17) shows all these calculations for first floor, and the same total for second floor.

Table 5.17: First Floor Total

Component	$\dot{Q}_{total}(W)$
BDR1	1601.8
Bath	535.2
BDR2	696.84
Bath3	1315.25
Bath2	420.5
Lobby	1776.9
Kitchen	1750.67
Dining	867.58
Salon	1663.04
Bath3	427.08
Sum	11079.1

5.3.6.3 Total Heating Load of Third Floor

$$Q_{rotal} = \dot{Q}_{wall} + \dot{Q}_{Glass} + \dot{Q}_{inf} + \dot{Q}_{door} + \dot{Q}_{cell}$$
 (5.25)

Table (5.18) shows all these calculations for third floor.

Table 5.18: Third Floor Total

Component	\dot{Q}_{total} (W)
BDR1	2024.44
Bath	627
BDR2	1077
Bath3	1712.7

Component	$\dot{Q}_{total}(W)$
Bath2	504.95
Lobby	2240.22
Kitchen	2178.35
Dining	1106.26
Salon	2095.04
Bath3	491.88
Sum	14057.8

$$\dot{Q}_{tot}$$
 heat of Building = \dot{Q}_{tot1} + + \dot{Q}_{tot2} + \dot{Q}_{tot3} + \dot{Q}_{tot4}
= 14291.5 + 11079.1 + 11079.1 + 14057.8
= 50507.5 W

Qtot Design of Building = 50507.5 * 1.1

= 55558.25 W

5.4 Duct Design

54.1 Warm and Cool Air Quantities

the calculated heating load and cooling load for a given space must be met by moducing sufficient amount of warm and cool air into that space, according to the blowing relation. [23]

$$\mathbb{L} = \rho C_p \dot{V} (T_s - T_t) \tag{5.26}$$

is the room sensible heat or cool heat, ρ and C_p are the density and specific the air, respectively, \dot{V} is the volumetric flow rate of the air, T_s and T_t are the sensitive of the supply air and the temperature of the inside room air, respectively.

$$\rho=1.25~kg/m^3$$

$$C_p = 1.01 \, kJ / kg.K$$

$$\dot{Q}_{s\,cooling} = 116.438\,kW$$

$$\dot{Q}_{s heating} = 50.6075 \, kW$$

$$\rightarrow \dot{V}_{cooling} = 9.22 \text{ m}^3/\text{s}$$
 Used to design the duct

$$\rightarrow \dot{V}_{s \, heating} = 1.53 \, m^3/s$$

The highest air flow rate is used for sizing duct system.

5.4.2 Duct Sizing

The relation beteen round duct diameter d, rate of air flow \dot{V} , pressure drop per unit length ($\Delta P/EL$), and velocity v, are presented in Figure (A-33).

These figures are usually used to find the duct diameter required for any flow of air quantities. The duct diameter can also be calculated from the relation:

$$\dot{V} = \frac{\pi}{4}d^2 * v \tag{5.27}$$

Four different methods are used to size ducts:

- 1. The Assumed Velocity Method.
- 2. The Equal Pressure Drop Method.
- 3. Balanced Pressure Drop Method.
- 4. Static Pressure Regain Method.

By using the assumed velocity method to size the duct from fan to diffuser and from return grille to fan, the velocity is assumed in main duct and branches related to Table (A-19) as follows:

 $V_{main\ duct} = 5\ m/s$

 $v_{branch} = (2.5 \text{ to } 3.5) \text{ m/s}$

By using equation (5.26)

 $d_{main duct} = 1.532m$

From Figure (A-37):

 $\Delta P/El = 0.16 Pa/m$

5.4.2.1 Non-Circular Ducts

Most of the used ducts in the air systems are rectangular or non-circular. This is due to the shape of residences and living spaces. If the diameter of circular ducts is calculated from eq. (5.27), then the Table (A-20) gives the equivalent of rectangular ducts for equal pressure drop and equal flow rate.

In Table (5.19), (5.20), and (5.21) show all calculations of the supply duct sizing with non-circular duct for ground, first, and third floor, where the second floor have the same duct size because it have the same load [25].

The line and components for ground floor, 1st, 2nd, and 3nd are the same design because of symmetry (repeated) in building shows in Figure (A-37).

Table 5.19: Supply duct for Ground floor with non-circular size

Line &	V m^3/s	ΔP/EL Pa/m	v (m/sec)	d (m)	High	Width
A-B	2.236	0.263	4.5	0.795	400	1400
B-C	1.957	0.285	4.5	0.744	400	1250
C-D	1.753	0.256	4	0.729	400	1200
D-E	0.661	0.309	3.5	0.473	400	500
E-F	0.491	0.242	3	0.456	400	450
D-G	1.092	0.217	3,5	0.630	400	850

Line & Component	\tilde{V} m^3/s	ΔP/EL Pa/m	v (m/sec)	d (m)	High	Width
G-H	0.879	0.248	3.5	0.565	400	700
H-I	0.411	0.172	2.5	0.457	350	500
H-J	0.411	0.257	3	0.418	350	450
J-K	0.292	0.334	3	0.352	300	350
BDR1	0.221	0.253	2.5	0.335	300	300
Bath 1	0.270	0.223	2.5	0.371	300	400
BDR2	0.170	0.297	2.5	0.294	250	250
BDR3	0.204	0.266	2.5	0.322	300	300
Bath 2	0.279	0.219	2.5	0.377	300	400
Lobby	0.213	0.259	2.5	0.329	300	300
Kitchen	0.411	0.172	2.5	0.457	350	500
Dining	0.119	0.372	2.5	0.246	200	250
Salon	0.149	0.323	2.5	0.276	250	250
Bath 3	0.143	0.331	2.5	0.270	250	250

Table 5.20: Supply duct for First & second floor with non-circular size

Line &	V m^3/s	ΔP/EL Pa/m	v (m/sec)	d (m)	Hìgh	Width
A'-B'	2.229	0.263	4.5	0.794	400	1400
B'-C'	1.929	0.287	4.5	0.739	400	1250
C'-D'	1.7365	0.258	4	0.725	400	1200
D'-E'	0.6945	0.287	3.5	0.502	400	500
E'-F'	0.489	0.243	3	0.455	400	450
D'-G'	1.042	0.224	3.5	0.615	400	800
G'-H'	0.843	0.255	3.5	0.554	400	650
H'-I'	0.455	0.162	2.5	0.481	350	550
H'-J'	0.388	0.28	3	0.406	350	400
J-K'	0.277	0.345	3	0.343	300	350
BDRI	0.208	0.262	2.5	0.325	300	300
Bath 1	0.281	0.281	2.5	0.378	300	400
BDR2	0.2055	0.264	2.5	0.323	300	300

BDR3	0.1926	0.275	2.5	0.313	300	300
Bath 2	0.3	0.209	2.5	0.391	300	400
Lobby	0.199	0.27	2.5	0.318	300	300
Kitchen	0.455	0.162	2.5	0.481	350	550
Dining	0.111	0,388	2.5	0.238	250	200
Salon	0.136	0.342	2.5	0.263	250	250
Bath 3	0.141	0.334	2.5	0.268	250	250

Table 5.21: Supply duct for third floor with non-circular size

Line &	V m^3/s	ΔP/EL Pa/m	v (m/sec)	d (m)	High	Width
A"'-B"	2.5068	0.139	5	0.798	400	1450
B"'-C"	2.1998	0.265	4.5	0.788	400	1400
C"-D"	1.9828	0.283	4.5	0.749	400	1250
D'"-E"	0.8377	0.356	4	0.516	400	550
E"-F"	0.529	0.339	3.5	0.438	400	400
D"'-G"'	1.145	0.294	4	0.603	400	750
G"'-H"	0.917	0.242	3.5	0.577	400	700
H"'-I"	0.482	0.245	3	0.452	400	450
H'''-J'''	0.4351	0.261	3	0,43	400	400
J'''-K'''	0.3085	0.323	3	0.362	350	350
BDR1	0.235	0.243	2.5	0.346	300	300
Bath I	0.2939	0.212	2.5	0.387	350	350
BDR2	0.3088	0.2 05	2.5	0.396	350	350
BDR3	0.217	0.256	2.5	0.332	300	300
Bath 2	0.307	0.206	2.5	0.395	350	350
Lobby	0.228	0.248	2.5	0.34	300	300
Kitchen	0.482	0.156	2.5	0.495	350	600
Dining	0.1266	0.357	2.5	0.254	250	250
Salon	0.1635	0.305	2.5	0.288	250	250
Bath 3	0.145	0.328	2.5	0.271	250	250

5.4.3 Supply Air Ceiling Diffuser

From Table (A-22) we are give the information of supply air ceiling diffuser, Tables (5.22), (5.23), and (5.24) shows the information of supply air ceiling diffuser (see Figure (A-39) & (A-40)). [13]

Table 5.22: Ground floor Diffuser

Component	v m^3/s	ΔP In w.g	Size in*in	Type of Diffuser	CFM
BDR1	0.221	0.1	12*12	4SNOD	500
Bath 1	0.270	0.14	12*12	4SNOD	600
BDR2	0.17	0.067	12*12	4SNOD	400
BDR3	0.204	0.1	12*12	4SNOD	450
Bath 2	0.279	0.14	12*12	4SNOD	600
Lobby	0.213	0.1	12*12	4SNOD	500
Kitchen	0.468	0.1	18*18	4SNOD	1125
Dining	0.119	0.1	9*9	4SNOD	280
Salon	0.149	0.039	12*12	4SNOD	300
Bath 3	0.143	0.039	12*12	4SNOD	300

Table 5.23: First and second floor Diffuser

Component	ν̈́ m³/s	ΔP In w.g	Size in*in	Type Diffuser	CFM
BDRI	0.208	0.1	12*12	4SNOD	500
bath I	0.281	0.067	15*15	4SNOD	624
BDR2	0.205	0.100	12*12	4SNOD	500
BDR3	0.192	0.067	12*12	4SNOD	400
bath2	0.300	0.039	18*18	4SNOD	675
Lobby	0.199	0.1	12*12	4SNOD	500
Kitchen	0.455	0.1	18*18	4SNOD	1125
Dining	0.111	0.1	9*9	4SNOD	280
Salon	0.136	0.039	12*12	4SNOD	300
Bath3	0.141	0.039	12*12	4SNOD	300

Table 5.24: Third floor Diffuser

Component	V m^3/s	ΔP In w.g	Size in*in	Type Diffuser	CFM
BDR1	0.235	0.1	12*12	4SNOD	500
bathl	0.294	0.067	15*15	4SNOD	624
BDR2	0.309	0.039	18*18	4SNOD	675
BDR3	0.217	0.1	12*12	4SNOD	500
bath2	0.307	0.1	15*15	4SNOD	780
Lobby	0.228	0.1	12*12	4SNOD	500
Kitchen	0.482	0.1	18*18	4SNOD	1125
Dining	0.126	0.039	12*12	4SNOD	300
Salon	0.163	0.067	12*12	4SNOD	400
Bath3	0.145	0.039	12*12	4SNOD	300

5.4.4 Design of Return Ducts

The design of return ducts are based on using the above described methods. By using the assumed velocity method. For the return duct system, air flows through the branches into the main duct and back to the fan. [23]

Table (5.25), (5.26), and (5.27) show all calculations of the return duct with noncircular size for 1s, 2nd, and 3rd floor, where the second floor have the same duct size because it have the same load.

The line and components for ground floor, 1st, 2nd, and 3rd are the same design because of symmetry (repeated) in building shows in Figure (A-38).

Table 5.25: Return duct for Ground floor with non-circular size

Line & Component	V m^3/s	ΔP/EL Pa/m	v (m/sec)	d (m)	High	Width
1-2	0.491	0.244	3	0.456	400	450
4-3	0.483	0.246	3	0.452	400	450
3-2	0.653	0.3	3.5	0.487	400	500
2-5	1.144	0.213	3.5	0.645	400	900
5-6	1.357	0.267	4	0.657	400	1000
7-6	0.292	0.686	4	0.304	300	250
6-8	1.649	0.237	4	0.724	400	1200
8-9	1.768	0.305	4.5	0.707	400	1150
9-10	2.236	0.343	5	0.754	400	1300
BDR1	0.221	0.254	2.5	0.335	300	300
Bath I	0.270	0.225	2.5	0.370	300	400
BDR2	0.170	0.3	2.5	0.294	300	300
BDR3	0.204	0.267	2.5	0.322	300	300
Bath 2	0.279	0.22	2.5	0.377	300	400
Lobby	0.213	0.26	2.5	0.329	300	300
Kitchen	0.411	0.173	2.5	0.457	350	500
Dining	0.119	0.374	2.5	0.246	250	200
Salon	0.149	0.325	2.5	0.275	250	250
Bath 3	0.143	0.334	2.5	0.269	250	250

Table 5.26: Return duct for First and second floor with non-circular size

Line & Component	√ m³/s	ΔP/EL Pa/m	v (m/see)	d (m)	High	Width
1'-2'	0.489	0.243	3	0.455	400	450
4'-3'	0.4926	0.242	3	0.457	400	450
3'-2'	0.6981	0.286	3.5	0.504	400	500
2'-5'	1.187	0.207	3.5	0.657	400	950
5'-6'	1.386	0.262	4	0.664	400	1000
7'-6'	0.277	0.705	4	0.267	300	250

Line & Component	[†] m³/s	ΔP/EL Pa/m	v (m/sec)	d (m)	High	Width
6'-8'	1.663	0.234	4	0.727	400	1200
8'-9'	1.774	0.302	4.5	0.708	400	1150
9'-10'	2.23	0.342	5	0.753	400	1300
BDR1	0.208	0.262	2.5	0.325	300	300
Bath 1	0.281	0.218	2.5	0.378	300	400
BDR2	0.205	0.264	2.5	0.323	300	300
BDR3	0.192	0.275	2.5	0.313	300	300
Bath 2	0.300	0.209	2.5	0.391	300	400
Lobby	0.199	0.27	2.5	0.318	300	300
Kitchen	0.455	0,162	2.5	0.481	350	550
Dining	0.111	0.388	2.5	0.237	250	200
Salon	0.136	0.342	2.5	0.263	250	250
Bath 3	0.141	0.334	2.5	0.268	250	250

Table 5.27: Return duct for Third floor with non-circular size

Line & Component	$\frac{\hat{V}}{m^3/s}$	ΔP/EL Pa/m	v (m/sec)	d (m)	High	Width
1'''-2'''	0.530	0.233	3	0.474	400	450
4"-3"	0.524	0.234	3	0.471	400	450
3"'-2"	0.833	0.36	4	0.515	400	550
2""-5"	1.363	0.226	4	0.658	400	950
5'''-6'''	1.599	0.324	4.5	0.672	400	1000
7'''-6'''	0.308	0.476	3.5	0.334	300	350
6"'-8"	1.900	0.292	4	0.733	400	1200
8""-9""	2.027	0.28	4.5	0.757	400	1300
9"-10"	2.507	0.321	5	0.798	400	1450
BDR1	0.235	0,243	2.5	0.346	300	300
Bath 1	0.294	0.212	2.5	0.387	350	350
BDR2	0.309	0.207	2.5	0.396	350	350
BDR3	0.217	0.257	2.5	0.332	300	300
Bath 2	0.307	0.208	2.5	0.395	350	350

Line & Component	\hat{V} m^3/s	ΔP/EL Pa/m	v (m/sec)	d (m)	High	Width
Lobby	0.228	0.25	2.5	0.34	300	300
Kitchen	0.482	0.157	2.5	0.495	350	600
Dining	0.126	0.36	2.5	0.254	250	250
Salon	0.164	0.307	2.5	0.288	250	250
Bath 3	0.145	0.331	2.5	0.271	250	250

5.4.5 Return Air Grille

From Table (A-23) we take the information of return air grille, Table (5.28), (5.29), and (5.30) show the information of Return Air Grille.

Table 5.28: Ground floor (Grille)

Component	ÿ m³/s	ΔP In w.g	Size in*in	Type of Grille	CFM
BDR1	0.221	0.022	12*12	7145H	540
bath1	0.270	0.016	12*16	7145H	620
BDR2	0.170	0.010	12*12	714511	360
BDR3	0.204	0.016	12*12	7145H	450
bath2	0.279	0.016	12*18	7145H	685
Lobby	0.213	0.016	12*12	7145H	450
Kitchen	0.468	0.022	14*20	7145H	1110
Dining	0.119	0.022	12*6	7145H	252
Salon	0.149	0.022	10*10	7145H	360
Bath3	0.143	0.022	10*10	7145H	366

Table 5.29: First and second floor (Grille)

Component	V m³/s	ΔP In w.g	Size in*in	Type of Grille	CFM
BDR1	0.208	0.016	12*12"	7145H	450
bath1	0.281	0.010	12*16"	7145H	496
BDR2	0.205	0.016	12*12"	7145H	450
BDR3	0.192	0.016	12*12"	7145H	450
bath2	0.300	0.016	12*16"	7145H	620
Lobby	0.199	0.016	12*12"	7145H	450
Kitchen	0.455	0.016	16*20"	7145H	1050
Dining	0.111	0.022	12*6"	7145H	252
Salon	0.136	0.016	10*10"	7145H	305
Bath3	0.141	0.016	10*10"	7145H	305

Table 5.30: Third floor (Grille)

Component	\dot{V} m^3/s	ΔP In w.g	Size in*in	Type of Grille	CFM
BDR1	0.235	0.022	12*12"	7145H	540
bath1	0.294	0.016	14*14"	7145H	620
BDR2	0.308	0.022	14*14"	7145H	744
BDR3	0.217	0.016	12*12"	7145H	450
bath2	0.307	0.022	14*14"	7145H	744
Lobby	0.228	0.022	12*12"	7145H	540
Kitchen	0.482	0.016	14*24"	7145H	1050
Dining	0.126	0.016	10*10"	7145H	305
Salon	0.163	0.022	10*10"	7145H	360
Bath3	0.145	0.016	10*10"	7145H	305

5.5 Fan Selection

The fan is an essential and important component of any summer air conditioning and winter warm air heating systems. It is used to circulate the air through ducts and branches.[25]

From Table (A-24) selected model AHU 200 with air CFM = 20000.

The fan pressure rise Δp_{fan} , is expressed as

$$\Delta P_{fan} = \Delta P_{cuet} + \Delta P_{fint} + \Delta P_{diffuser} + \Delta P_{coil} + \Delta P_{filter} + \Delta P_{fon, inlet} + \Delta P_{fan, exit} + \Delta P_{dyn}$$

$$\Delta P_{duct} = \Delta P_{supply} + \Delta P_{return}$$

$$\Delta P_{supply air dust} = \Delta P_{A \rightarrow K} + \Delta P_{fitting}$$

$$\Delta P_{A\to A} = 0.16 * (3.75 + 1.5 + 6) = 1.8 Pa$$

$$\Delta P_{A \to A} = 0.16 * (3.75 + 1.5 + 6) = 1.8 Pa$$

$$\Delta P_{A^{-} \rightarrow A^{-}} = 0.16 * (3.75 + 1.5 + 6) = 1.8 Pa$$

$$^{\Delta P_{A^{-} \rightarrow B^{-}}} = 0.139 * (0.81 + 1.5 + 6) = 1.155 Pa$$

$$\Delta P_{B^{+}\to C} = 0.266*(0.52+1.5+6)=2.125 Pa$$

$$\Delta P_{C^{+} \rightarrow D^{-}} = 0.283 * (3.9 + 1.5 + 6) = 3.22 Pa$$

$$\Delta P_{B^{-}\to G^{-}} = 0.294 * (3.56 + 1.5 + 6) = 3.25 Pa$$

$$\Delta P_{\sigma^- \to H^+} = 0.292 * (2.51 + 1.5 + 6) = 2.42 Pa$$

$$\Delta P_{H^- \to f^-} = 0.261 * (1.72 + 1.5 + 6) = 2.4 Pa$$

$$\Delta P_{f \to K} = 0.323 * (3.52 + 1.5 + 6) = 3.55 Pa$$

$$^{\text{AP}_{\text{K}}}_{\rightarrow \text{Rath3}} = 0.328(1.1 + 1.5 + 6) = 2.82 \, Pa$$

$$\Delta P_{\text{return duct}} = \Delta P10 \rightarrow 4'''$$

$$\Delta P_{10\to 10} = 0.16 * (3.75 + 1.5 + 6) = 1.8 Pa$$

$$4P_{10\to 10} = 0.16 * (3.75 + 1.5 + 6) = 1.8 Pa$$

$$4P_{10^{\circ}-10^{\circ}} = 0.16 * (3.75 + 1.5 + 6) = 1.8 Pa$$

$$\Delta P_{10^{-} \rightarrow 9^{-}} = 0.321 * (3.6 + 1.5 + 6) = 3.56 Pa$$

$$\Delta P_{9^{"}\rightarrow8^{"}} = 0.28 * (3.73 + 1.5 + 6) = 3.14 Pa$$

$$\Delta P_{8''\to6''} = 0.292 * (1.84 + 1.5 + 6) = 2.72 Pa$$

$$\Delta P_{6"\rightarrow 5"} = 0.324 * (3.12 + 1.5 + 6) = 3.44 Pa$$

$$\Delta P_{5^{"}\rightarrow 2^{"}} = 0.226 * (5.76 + 1.5 + 6) = 2.99 Pa$$

$$\Delta P_{2^{-} \rightarrow 3^{-}} = 0.36 * (0.6 + 1.5 + 6) = 2.91 Pa$$

$$\Delta P_{3^{-}\rightarrow 4^{-}} = 0.234 * (4.34 + 1.5 + 6) = 2.77 Pa$$

$$\Delta P_{4^{-} \rightarrow BDR3} = 0.257 * (3.04 + 1.5 + 6) = 2.7 Pa$$

$$\Delta P_{\text{Dynamic}} = \left(\frac{V}{1.29}\right)^2 = \left(\frac{5}{1.29}\right)^2 = 15 \, Pa$$

$$\Delta P_{erill} = 4.5 Pa$$

$$\Delta P_{coil}$$
, ΔP_{Filter} , $\Delta P_{fan inlet}$, $\Delta P_{fan outlet}$, given from Table (A-25).

$$\Delta P_{coll} = 0.328 in of H20 = 81.7 Pa$$

$$\Delta P_{Filter} = 0.68 in of H20 = 169.4 Pa$$

$$\Delta P_{\text{fan inlet}} = 80 Pa$$

$$\Delta P_{lan outlet} = 60 Pa$$

$$Power = \frac{V \cdot \Delta P}{\eta} \tag{5.28}$$

$$Power = \frac{9.22 * 482.67}{0.9 * 1000} = 4.95 \, kW$$

5.6 Summer Air Conditioning and Winter Warm Air Heating System

5.6.1 Traditional Air Conditioning System (Chiller) Selection:

We select Variable Water Volume System (VWV) from Petra company since:

The system offers large savings in energy and initial costs. The system may be used in multi-story buildings, office complexes, hotels, or any other type of project where high-energy savings are required. The system is comprised of air-cooled water chillers (cooling + heating), indoor units with three way valves, a control package, pumps, expansion tanks, storage tanks, water piping and integrated complete system control.

5.6.2 Selection model

Total cooling load = 128.1kW

So we select RWC Model 530 from Petra company Table (A-26).

Cost of this model = 135000 NIS

5.6.2.1 General Data

Cooling capacity = 129.4 kW

Heating capacity = 121.5 kW

Compressor: Hermetically Sealed Scroll

Number of Compressor: 4

Refrigerant: R-22

Water connection size = 3 in

Number of fans = 2

Air flow rate = $14805 \, t/s$

5.6.2.2 Electrical Data

Power supply = 380/420 volt

3Phase, 50Hz

Total Consumption Power = 37kW

5.6.3 Annual power consumption

Annual Power Consumption = (Load [kW]/COP)*No.of month per year * No.of day

per month*No. of hour per day*Price of

electricity (5.29)

$$COP_{cooling} = \frac{129.4}{37} = 3.497$$

$$COP_{heating} = \frac{121.5}{37} = 3.284$$

Annual Power Consumption for Cooling =
$$\left(\frac{128.1}{3.497}\right) * 5 * 30 * 16 * 0.61$$

= 53628.4 NIS
Annual Power Consumption for Heating = $\left(\frac{55.56}{3.284}\right) * 5 * 30 * 16 * 0.61$
= 24768.5 NIS

Total Annual Power Consumption = 78397 NIS

57 Earth Connection - Closed loop Ground Heat Exchangers (GHX)

This section introduces the procedure to estimate the size and the performance of closed-loop ground heat exchangers (GHXs). Since this estimation also requires the calculation of elements that specifically belong to the heat pump system.

1 Vertical Heat Exchanger length Design

find the required vertical heat exchanger length of bore, it takes the following specified for heating:[13]

$$L_{h} = \frac{q_{a}*R_{ga} + (C_{fh}*q_{lh})*(R_{b} + PLF_{m}*R_{gm} + R_{gd}*F_{sc})}{t_{p} + \frac{t_{wi} + t_{wo}}{2} - t_{g}}$$
(5.30)

And takes the following equation for cooling:[13]

$$L_{c} = \frac{q_{a}*R_{ga} + (C_{fc}*q_{lc})*(R_{b} + PLF_{m}*R_{gm} + R_{gd}*F_{sc})}{t_{p} + \frac{t_{wi} + t_{wo}}{2} - t_{g}}$$
(5.31)

Where L_c is the length of bore required for cooling (m), L_h is the bore required for heating (m), q_a net annual average heat transfer to the ground (kW), C_{fb} heat pump correction factor for heating, C_{fc} heat pump correction factor for cooling, q_{fb} building design heating load (kW), q_{fc} building design cooling load (kW), R_b thermal resistivity of bore, R_{gu} effective thermal resistivity of the ground annual pulse (m·K/kW), R_{gm} effective thermal resistivity of the ground monthly pulse (m·K/kW), R_{gf} effective thermal resistivity of the ground daily pulse, PLF_m part-load factor turing design month, F_{sc} short-circuit heat loss factor, t_g undisturbed ground temperature (°C), t_p temperature penalty for interference of adjacent bores (°C), t_{wi} fauld temperature at heat pump inlet (°C), and t_{wo} liquid temperature at heat pump satiet(°C) [13].

To use these equations, the net annual heat transfer to the ground, q_a, needs to be calculated. The net annual heat transfer to the ground is given by the following equation:

$$= \frac{C_{fc}q_{lc}EFLhours\ c + C_{fh}q_{lh}EFLhours\ c}{8760}$$
 (5.32)

Where 8760 is the number of hours per year, EFLhours, is the equivalent full-load hours for cooling, and EFLhours, is the equivalent full-load hours for heating.

The heat pump correction factors, C_{fc} and C_{fb} are taken from Table (Λ -28) and everything is plugged into the above equation for net annual heat transfer.

$$C_{fe} = 1.2$$

 $C_{fh} = 0.8$
 $q_{lc} = 128082.17 \text{ kW} = 437327.09 \text{ Btu}$
 $q_{lh} = 55.558 \text{ kW} = 189698.679 \text{ Btu}$

EFL hours c = 2400 h

EFL hours h = 2400 h

$$q_a = \frac{(1.2*397568.93*2400) + (0.8*189698.67*2400)}{8760}$$
$$= 185356.56 \ Btu/h$$

The program currently uses a length calculation that involves a single value for the ground resistivity. This neglects long-term heat changes in the soil that may arise over the life of the system. By using several values, which are based on three different pulses, a more accurate calculation for the length of bore can be found that takes into account the long-term temperature changes of the soil. These resistivity values are labeled $R_{\rm gs}({\rm annual})_s R_{\rm gm}({\rm monthly})_s$, and $R_{\rm gd}({\rm daily})_s$. To solve for these, calculate τ , or the length of each pulse, for the three different time intervals:

$$\tau_1 = 3650$$
 (10 years); $\tau_2 = 3680$ (1 month); $\tau_1 = 3680.25$ (6 hours) [13].

Then the following equations are used to solve for Fourier number for each of the pulses:

$$F_{01} = \frac{4\alpha(\tau_f - \tau_1)}{d^2}$$
 (5.33)

$$F_{02} = \frac{4(\tau_f - \tau_2)}{d^2} \tag{5.34}$$

$$F_{0f} = \frac{4\alpha\tau_f}{d^2} \tag{5.35}$$

Where α is thermal diffusivity, and d is diameter of pipe. [24] Using the values of F₀ find the G values associated with each of these Fourier values if found form a logarithmic fit of Figure (A-31): [26]

$$G = 0.0769 Ln(F0) + 0.0901 (5.36)$$

Finally, to solve for the thermal resistivity $(R_{ga}, R_{gm}, and R_{gd})$, use the equations:

$$R_{ga} = \frac{G_f - G_1}{k_g} \tag{5.37}$$

$$R_{gen} = \frac{G_1 - G_2}{k_g}$$
 (5.38)

$$R_{gd} = \frac{G_2}{k_g} \tag{5.39}$$

Where k_g the thermal conductivity of earth.

$$a = 0.8 \text{ ft}^2/\text{day}$$

$$-Gf = 1.1575$$

$$-61 = 0.7884$$

$$-62 = 0.4196$$

$$R_{ga} = 0.3 (h ft. °F/Btu)$$

 $R_{gm} = 0.3099 (h ft. °F/Btu)$
 $R_{gd} = 0.3526 (h ft. °F/Btu)$

Next, a specific type of pipe needs to be assumed for use in the heat exchanger. A commonly used pipe for this purpose is 32mm diameter polyethylene tube (SDR11).

Kavanaugh cites the work of Remund and Paul (1997), and their use of a method of solving for thermal resistivity of bore, R_b the equation:

$$R_b = R_{bf} + R_P \tag{5.40}$$

Where R_{bf} is the backfill resistivity, and R_b thermal resistivity of pipe.

$$R_{bf} = 0.7 \text{ h ft.°F/Btu}$$

 $R_p = 0.075 \text{ h ft.°F/Btu}$
 $R_b = 0.7 + 0.075 = 0.775 \text{ h ft °F/Btu}$

Next, the short-circuit heat loss factor F_{sc} , which is the heat lost between adjacent pipes in the same borehole.

$$Fsc = 1.03$$

Now the part load factor can be taken from the equation;

$$PLF_{m} = \left(\frac{load * Hours}{Peakload * 24h}\right) * \left(\frac{DaysOccupiedPerMonth}{DaysPerMonth}\right)$$

$$PLF_{m} = \frac{116.438 * 16}{128.082 * 24} * \frac{27}{31} = 0.528$$
(5.41)

For vertical installation, it is assumed that the ground temperature t_g , is equal to the mean of the winter and summer average temperatures.

Water inlet temperature is suggested to be 20 to 3 degrees higher than t_g in cooling, and 10 to 20 degrees lower than t_g in heating (both in ${}^{\rm a}{\rm F}$). [25]

$$t_{wic} = 29 \, ^{\circ}\text{C} = 84.2 \, ^{\circ}\text{F}$$

$$t_{woc} = 32.22 \, ^{\circ}\text{C} = 90 \, ^{\circ}\text{F}$$

$$t_{wih} = 11 \,^{\circ}\text{C} = 52 \,^{\circ}\text{F}$$

Finally, the temperature penalty due to bores affecting one another t_p , see Table (A-29) can be used to estimate this value. Interpolation can be done with values not exactly matching the chart.

With all of these values determined, equations (5.30), and (5.31) can be used to solve for the bore length required for heating and cooling.

$$L_{h} = \frac{185356.56*0.31+(0.8*189698.667)*(0.775+0.528*0.3099+0.3526*1.03)}{36.68+\frac{52+47.84}{2}-63.2}$$

$$L_h = \frac{255020.94}{23.4} = 10898.33 \, ft = 3322.66 \, m$$

$$L_{c} = \frac{185356.56*0.31+(1.2*437327.09)*(0.775+0.528*0.3099+0.3526*1.03)}{36.68+\frac{84.2+90}{2}-63.2}$$

$$L_c = \frac{740638.1494}{60.58} = 12225,786 \, ft = 3727.01 \, m$$

We depend in design bore length on $L_{\mathcal{C}}$ because $L_{\mathcal{C}}$ is larger than L_{h} .

where of Bores =
$$\frac{Bore\ Length}{deep\ of\ each\ Bore}$$

Number of Bores =
$$\frac{3727.01}{100}$$
 = 37.01 = 37 Bores

Length of Heat exchanger (polyethylene pipe) = $2 * L_c = 7454.02 m$

5.7.2 Circulation Pump Selection

To select the pump must be know the friction loss in pipes and the friction loss in coil of heat pump, so we use the Table (A-30) to calculate the friction in pipes, and use the Table (A-28) to know the value of friction in heat pump coil:

Total Equivalent Length of Pipe = 7454.02 * 1.5 = 11181.3 m

Take the pressure drop in pipe is 6 kPa/100m.

Friction loss in pipes = 11181.3 * $\frac{6}{100}$ = 670.9 kPa

Friction loss in heat pump coil = 23.2 ft. of water = 69.35 kPa

And the total friction loss = 670.9 + 69.35 = 740.25 kPa

Also the required flow rate in heat pump coil to achieve the required amount of heat s = 90 gpm see Table (A-27).

based on the water flow rate and the friction loss in pipes we selected the type of TPE Series 1000 from Grundfoss Company see Figure (A-32).

573 Water Volume in the Heat Exchanger

water amount in ground heat exchanger can be calculated from the following

$$T_{\text{mater}} = \frac{\pi * d^2}{4} * L \tag{5.42}$$

Where A is the cross section area of pipe (m²), L is the length of pipe (m), d is the diameter of pipe.

We should take that require flow rate in SDR11 is 11 1/min per Ton Refrigeration from Ground Loop Design Software. [24]

We have a different diameter start from geothermal heat pump to borehole in different length see Figure (A-43) then the calculation as follow:

$$d_1 = 32 \ mm$$
 , $d_2 = 37.5 \ mm$, $d_3 = 50 \ mm$, $d_4 = 75 \ mm$
 $L_1 = 7525 \ m$. $L_2 = 140 \ m$, $L_3 = 196 \ m$, $L_4 = 3.4 \ m$

$$V_1 = \frac{\pi * (0.032)^2}{4} * 7525 = 6.05 m^3$$

$$V_2 = \frac{\pi * (0.0375)^2}{4} * 140 = 0.154 m^3$$

$$V_3 = \frac{\pi * (0.05)^2}{4} * 196 = 0.385 \, m^3$$
$$V_4 = \frac{\pi * (0.075)^2}{4} * 3.4 = 0.015 \, m^3$$

Total water volume in heat exchanger = 6.05 + 0.154 + 0.385 + 0.015= $6.604 \, m^3$

5.7.4 Geothermal Heat pump Selection

We select heating and cooling heat pump model WRA-420 from Daikin-McQuay see Table (A-27) and (A-28).

5.7.4.1 Selection Model

Total Cooling Load = 128.1 kW = 437008 BTU

Total Hearing Load = $55.56 \, kW = 189698.7 \, BTU$

5.7.4.2 General Data

Cooling capacity = 443177BTU/h = 129.9 kW

Heating capacity = 491495btu/h = 144.05 kW

Number of Compressor scroll type = 2

Refrigerant: R-410a

Water Connection = 3 in pipe

Water Flow Rate = 90 gpm

5.7.4.3 Electrical Data

Power Supply = 380V, 3PH, 50Hz

Total consumption for cooling= 19,838 kW

Total consumption for heating= 30.141 kW

5.7.5 Cost of Geothermal Heat Pump Equipment

Cost of Heat Pump = 32400 \$ = 118260 NIS

Cost of Pipe = 7455 * 3.65 = 27211 NIS

Cost of Drilling = 37 * 1000 * 3.65

= 135050 NIS

Cost of Centrifugal Pump = 2000 \$ = 7300 NIS

SO the Initial cost for Geothermal heat pump = 118260 + 27211 + 135050 + 7300 = 287821 NIS

5.7.6 Annual power Consumption for Heat Pump

$$COP_{cooling} = \frac{129.9}{19.838} = 6.5$$
 $COP_{heating} = \frac{144.05}{30.141} = 4.78$

Annual Power Consumption for Cooling =
$$\left(\frac{128.1}{6.5}\right) * 5 * 30 * 16 * 0.61$$

= 28852.1 NIS/year

Annual Power Consumption For Heating =
$$\left(\frac{55.56}{4.78}\right) * 5 * 30 * 16 * 0.16$$

= 17016.7 NIS/year

5.8 System Comparison and Payback Period

Initial cost difference between two system

- = (initial cost of GHP) (initial cost of Traditional system)
- = 287821 135000 = 152821 NIS

Annual Power Consumption difference between two system

- = Annual Power C. of Traditional S. Annual Power C. of GHP
- = 78397 45868.8 = 32528.2 NIS/year

The number of years necessary to offset the cost difference used simple Payback method:

Payback Period =
$$\frac{\text{Initial cost difference}}{\text{Annual Power Consumption difference}}$$

$$= \frac{152821}{32528.2} = 4.7 \text{ years}$$

Conclusion

The initial cost of Geothermal heat pump system is very high but it can return the initial cost after several years, depend that on load of building, type of ground properties, and other reasons, in this project the payback period is not exceed the typical period of geothermal heat pump system (3-6 years), so we recommend apply it in an individual buildings because it sufficient.

Recommendation

- 1. We recommend applied this project in Residential and commercial building in Palestine, despite his high cost, because the Palestinian suffering from a lack in electrical energy, and this reduces the power consumption.
- We recommend this technology to teach at Palestine polytechnic university, given the importance of this technology.
- We recommend government to motivate the owners of companies and enterprises use GHP in the process of air conditioning and refrigeration, this is because it reduces the power consumption.

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Appendix A

Table A-1 Ground Temperatures

Table A-2 cooling load temperature differences for calculating cooling load from sunlit roofs

Table A-3 Latitude correction factor (I.M) for latitude and month applied to walls and roof, north latitudes

Table A-4 Overall heat transfer coefficient for windows, W/m2.°C

Table A-5 solar heat gain factor (SHG) W/m2, for a latitude angle of 32°

Table A-6 Shading coefficient (SC), for single, double and insulting glass without interior shading

Table A-7 Cooling load factors for glass without interior shading, north latitudes

Table A-8 cooling load temperature differences for glass convection

Table A-9 outdoor air requirement for ventilation

Table A-10 Cooling load factors for lighting

Table A-11 sensible heat Cooling load factors for people

Table A-12 Cooling load factors for occupants

Table A-13 Cooling load factors for equipment

Table A-14 Heat gain from occupants in watt person

Table A-15 Overall heat transfer coefficients Uw , for basement walls below grade (W/m².°C)

Table A-16 overall heat transfer coefficients for typical ceiling constructions, W/m^2 , °C, for $R_0 = 0.03 \text{ m}^2$, C/W

Table A-17 Air change per hours in residences and commercial application

Table A-18 Overall heat transfer coefficients for wood and steel doors, W/m2.°C

Table A-19 Recommended and maximum air velocities for warm and cool air

Table A-20 Circular equivalents of rectangular ducts for equal friction and apacity

Table A-21 Equivalent length Le, of various fittings

Table A-22 Model 4SNOD four-way throw square diffusers

Table A-23 Fixed blade Return Air Grille Models 7145H

Table A-24 Air Handling Unit

Table A-25 "PAH" Static pressure drop

Table A-26 Chiller RWC Model 530 from Petra company

Table A-27 Heat pump performance data cooling part load WRA-420

Table A-28 Heat pump performance data heating part load WRA-420

Table A-29 long-Term change in ground filed Temperature

Table A-30 High density polyethylene pressure drops."1 1/4 in "

Figure A-31 F0 vs. G for a cylindrical heat source

Figure A-32 Performance curves for TPE Series 1000 Grundfoss pump

Figure A-33 Pressure drop (ΔP/EL), for air in galvanized steel ducts, based on round duct diameter

Figure A-34 Elevation

Figure A-35 Ground floor plane

Figure A-36 First floor plane repeated

Figure A-37 First floor duct line repeated

Figure A-38 First floor return duct line repeated

Figure A-39 Ground floor duct and air supply

Figure A-40 Third floor duct and air supply repeated

Figure A-41 Ground floor return duct

Figure A-42 Third floor return duct

Figure A-43 Ground floor plane and GHP lines

Figure A-44 GHP lines section

Table A-1 Ground Temperatures

	FI City	State/Country	GWT (F	Gity	State/Country	GWT (F)	City	Conti
57	Frankfurt	Cermany	66	Charleston	South Caroline	85		State
81	Hamburg	Germany	84	Columbia	South Carolina	70	Birmingram	Alabama
40	Municip	Serruane	92	Groonville	South Carolina		Motile	Alabama
51	Stuttoart	Semmy	51	Sioux Falls	The state of the s	67	Montgomery	Alabama
57	Alhens	Greece		The second second second second second	South Dakote	40	Anchorage	Alaska
53:	Budapest	Hungary	61	Knoxyille	Tennesine	0	Feirbenks	Alásica
20	The state of the s	The state of the s	63	Memphis	Tennossop	73	Phoenia	Arizona
52	Jakana	Indonesia	60	Nashvile	Tennessee	.54	Little Rock	Arkarsas
	Damlin	traland	71	Austin	Texas	68	Freedoc	
53	verus nigm	Palestine	68	Dallas	Tesas	54		Californio
50	Gonova	taly	71	Houston	Texas	and the same of th	Los Angeles	California
57	Milen	itely	72	San Antonic		67	Sacremento	California
12	Naples	Ifaily	58		lexas:	84	San Diego	California
=	Palermo	Haly		Salt Lake City	Utah	90	San Francisco	California
is.	Rome		46	Burington	Vermont	52	Denver	Colorace
16		tay	5.1	Nertalk	Virginia	- 51	Hartions	Connectious
	Torne	italy	60	Richmond	Virginia	.57	Dover	
18	Trieste	Italy	59	Hoenoke	Virginia	70	Daytone Beach	Delaware
22	Venice	Italy	57	Westlington	DC	71		Floride
2	Negoya	Japan	83	Seattle	THE RESIDENCE OF THE PERSON NAMED IN COLUMN 1		Jacksonville	Florida
3	Osska	Jepan			Washington	78	Mismi	Florida
	Sappore	The state of the s	49	Spokane	Washington	69	Tellehasson	Florida
ě.		Japan	58	Charleston	West Virginia	75	Tampa	Florida
_	Toxyo	Japan	46	La Crosse	Wisconsin	62	Atlanta	Georgia
£	Inst'en	Korea	47	Wiwankee	Wisconsin	67	Sevennah	
9	Pusan	Koraa	46	Cheyenne	Wyamina	79		Georgia
	Secul	Korea	42	Caltary			Honolulu	Hawaii
	Kowels City	Kuwatt	40		Alberta	47	Boise	Idaho
1	Tripoli	Libyari Arab Jamahinya		Edmonton	Alberta	51	Chicago	Illinois
	George Town		53	Vancouver	British Columbia	58	Springfield	lilinds
_	The state of the s	Malaysis	40	Winnipeg	Manitoba	#3	Fort Wayne	indiano
2_	Kuain Lumpur	Malaysia	42	Monston	New Entraswick	55	Indianapais	Indiana
1	Acapulee	Mexico	43	Seint John's	Newfoundard	53	Des Moines	111000000000000000000000000000000000000
	Mexico Dity	Mexico	45	Halifax	Nova Scolia	59		lowa
1	Veracruz	Mexico	45	Ottawa			Wichita	Manaes
	Casabianca	Morpeps			Ontens	57	Cincinatti	Onlo
	Amsterdam		48	Taroma	Ontario	50:	Lexington	Kentucky
	The second second second second	Netherlands	42	Charlottetown	Prince Edward Island	60	Louisville	Kentucky
_	Auckland	New Zealand	46	Montreal	Duegeo	70	New Oringes	The state of the s
	Christchurch	New Zoslama	39	Regina	Saskatchewan	66	Shrevoport	Louisiana
	Wellington	New Zealand	64	Buonos Aires	Argentina	46		Lowsiene
	Osio	Norway	64	Adelaide	Australia		Ceribou	Mane
	Asuncion	Pereguay	72			48	Portland	Maine
	Lima	Peru		Brisbane	Australia	57	Baltimore	Meryland
	Mania		67	Canberra	Australia	50	Boston	Massachusetts
		Philippines	59	Mniboume	Australia	50	Wordnester	Maxisachusells
_	Krakow	Poland	97	Perth	Australia	50	Detroit	Michigan
	Warsew	Poland	- 57	Sydney	Australie	49	Flint	
	Parto	Fortugal	51	Saxburg	Austrio	46	The second secon	Michigen
	San Juan	Puerto Rico	50	Vienna	Austria		Grand Repids	Michigan
	Done	Ostar	80		The state of the s	41	Duluth	Minnesota
	Bucherest	Romania		Manama	Bahrain	47	Moneapolic	Minnesata
	Riveon		52	Bosonis	Delgium	67	Jackson	Mississippi
	The second secon	Saudi Arathia	50	Lu Paz	Belivia	58	Korisas City	Missouri
	Singapore	Singapore	62	Вејет	Brazil	50	St. Louis	Missouri
	Barcelona	Spain	80	Drasila	Brazil	49	Brings	
	Macrid	Spain	78	Regre	Brezi	47		Montage
	4 - 4 - 1			10000000			Helena	Montana
	Savila	Spain	70	Sara Pinetes	Chest	2.5		ACCORDING TO A SECURITY OF THE PARTY OF THE
		Spain Spain	70	Sau Phuin	Brazi	53	Omana	14cbrasks
	Valencia	Spain	55	Sofia	Gulgaria	53 80	Cmana Las Veges	ACCORDING TO A SECURITY OF THE PARTY OF THE
	Valencia Stockholm	Spain Sweden	55 51	Sofia Santiago	Bulgara Chile	89 50		Nobraska Nevada
	Valencia Stockholm Cenaya	Spain Sweden Switzerland	55 81 58	Sofia Santiago Belling	Gulgaria	80	Las Veges Reno	Nevada Nevada
	Valencia Stockholm Ceneva Damascus	Spain Sweden Switzerland Syria	55 51	Sofia Santiago	Bulgara Chile	80 50 50	Reno Concord	Nevada Nevada Nevada New Hampshire
	Valencia Stockholm Ceneva Damascus Taipe	Spain Sweden Switzerland	55 81 58	Sofia Santiago Beljing Guangznou	Bulgana Chile China China	89 50 30 55	Reno Concord Trenton	Nevada Nevada New Hamponire New Jersey
	Valencia Stockholm Ceneva Damascus	Spain Sweden Switzerland Syria	55 81 58 77 53	Sofis Santiago Belling Guangznou Harbin	Bulgaria Chile China China China China	80 50 50 55 55	Reno Concord Trenton Abuquerque	New Jersey New Moxico
	Valencia Stockholm Ceneva Damascus Taipe	Spain Sweden Switzerland Syria Talwan Thalland	55 81 58 77 53 77	Sofia Sentiago Belling Guenganou Harbin Hong Kong	Gulgana Chile China China China China	80 50 30 56 59 50	Renn Concord Trenton Albuquerque Albany	Nevada Nevada New Harroshire New Jersey New Moxico New York
	Valencia Stockholm Cenava Damascus Taipe Bangkok Tunks	Spain Sweden Switzerland Syria Tahvan Thalland Turisia	55 58 58 77 53 77 62	Sofia Santiago Belling Guangznou Harbin Hong Kong Shenghal	Gulgana Chile China China China China China China	80 50 50 56 58 50 50	Las Veges Renn Concord Trenton Albuduerque Albany Bulliste	Nevada Nevada New Hampshire New Hampshire New Modec New York New York
	Valencia Stockholm Cenava Damascus Taipe Bangkok Tunis Ankara	Spain Sweden Switzerland Svita Talvan Thalland Turisia Turicy	55 81 58 77 53 77 62 56	Sofis Sentiago Belling Guangzhou Harbin Hong Kong Sharghal Stenyong	Gulgana Chile China China China China China China China	89 50 30 55 59 50 50 50	Las Vegos Reno Concord Trenton Albuduerque Albany Bulliste New York City	Nevada Nevada New Harroshire New Harroshire New Moxico New York New York New York
	Valencia Stockholm Canava Damascus Taine Gangkok Tunis Ankara Istanbul	Spain Sweden Switzerland Syria Tahvan Thalland Turksia Turksy	55 81 58 77 53 77 62 56 58	Sofia Santiago Belling Guengznou Harbin Hong Kong Shenghai Shenghai Shenyang Bogola	Gulgana Chile Grans China	80 50 30 65 59 50 50 50 50	Las Veges Renn Concord Trenton Albuduerque Albany Bulliste	Nevada Nevada New Hampshire New Hampshire New Modec New York New York
	Valencia Stockholm Canava Damascus Taipe Bangkok Tunis Ankora Istanbul Izmir	Spain Sweden Switzerland Switzerland Syria Tahvan Thalland Turkey Turkey Turkey	55 51 58 77 53 77 62 56 58 77	Sofia Santiago Belling Guengznou Harbin Hong Kong Shenghai Shenghai Shenyang Bogola Havana	Gulgana Chile China China China China China China China	89 50 30 55 59 50 50 50	Las Vegos Reno Concord Trenton Albuduerque Albany Bulliste New York City	Nevada Nevada Nevada New Harroshire New Harroshire New Modeo New York New York New York New York New York New York North Ceroline
	Valencia Stockholm Cenava Damascus Taipe Bangkok Tunis Ankora Istanbul Izmir Abu Dhabi	Spain Sweden Switzerland Syria Tahvan Thalland Turksia Turkey	55 58 58 77 53 77 62 56 58 77 66	Sofia Santiago Belling Guengznou Harbin Hong Kong Shenghai Shenghai Shenyang Bogola	Gulgana Chile Grans China	80 50 30 65 59 50 50 50 50	Las Veges Reno Cencord Trenton Albuduerque Albeny Bullate New York City Asteville Chariotte	Nevada Nevada Nevada Nevada New Harroshire New Jersey New Moxico New York New York New York New York North Derolins North Derolins
	Valencia Stockholm Ceneva Damescus Taipe Bangkok Tunis Ankona Istenbul Izmir Abu Dhabi Dubal	Spain Sweden Switzerland Syria Syria Tahvan Thalland Turnsia Tuncy Turkey Turkey Turkey United Arab Emirates United Arab Emirates	55 81 56 77 53 77 62 56 56 58 77 62	Sofia Santiago Belling Guengznou Harbin Hong Kong Shenghai Shenghai Shenyang Bogola Havana	Gulgana Chine China	80 50 30 55 59 50 50 50 50 50 50 50 50 50 50 50 50 50	Las Vegos Reno Concord Concord Albertario Albertario Buillate Vew York City Asheville Chariotis Greensboro	Nevada Nevada Nevada New Harrophire New Harrophire New York New York New York New York New York New York North Deroline North Serolins
	Valencia Stockholm Cenava Damascus Taipe Bangkok Tunis Ankora Istanbul Izmir Abu Dhabi	Spain Sweden Switzerland Syria Tahvan Thalland Turksia Turkey	55 51 58 77 53 77 62 56 58 77 66 47	Sofia Sentiago Belling Guengznou Harbin Hong Kong Shenyang Bogola Havana Pregue Copenhagen	Gulgana Chile China	86 50 36 55 58 59 50 50 50 50 62 60 62	Las Vegos Reno Concend Trenton Abucuerque Albany Buffato New York City Asheville Charlotte Greenstorp Raleigh	Nevada Nevada Nevada New Hampshire Now Jersey New York New York New York New York North Cerolina North Cerolina North Carolina
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	Valencia Stockholm Geneva Damascus Taipe Bangkok Tunis Ankora Istenbul Izmir Abu Dhabi Dubal Aberdeen Bettest Bermegham Edinburgh Liverpool	Spain Sweden Switzerland Syria Talvan Thalland Turnsia Turney Turkey Turkey Turkey Turkey Entrol United Arab Emirates United Kingdom	55 81 58 77 53 77 62 56 58 77 66 47 89 78 73 47 81	Sofia Sentiago Belling Guengzhou Harbin Hong Kong Shenghai Shenghai Shenyong Bogola Havana Prague Copantiagen Quito Aswan Cairo	Gulgana China Chin	80 50 30 55 59 50 50 50 50 62 60 62 44 42 51	Las Vegos Reno Concord Tenton Albuduarque Albany Bullate Vew York City Asheville Chariotte Greenstorp Raleigh Rismanck Fargo Citeveland Columbus	Nebrasks Nevada Nevada Nevada New Hampenire New Hampenire New York North Darolins North Carolins North Carolins North Dakota North Dakota Offic Ohio
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	Valencia Stockholm Garays Damascus Taipe Bangkok Turis Ankora Istanbul Izmir Abu Dhabi Dubal Aberdeen Bettast Burmagham Edinburgh Liverpool London Montavideo	Spain Sweden Switzerland Syria Syria Tahvan Thailland Turnsia Turney Turkey United Arab Emirates United Kingdom	55 51 58 77 53 77 62 56 57 58 77 64 77 80 78 73 47 61 57 69	Sofia Santiago Beiling Guanghou Harbin Hong Kong Sharghai Havania Pregue Copenhagen Duito Aswan Cairo Helsinia Bordenux Lyon Marseille	Gulgaria China Chi	89 50 50 55 58 50 50 50 50 50 60 60 62 44 42 51 55 55 55 60 60 62 60 60 62 64	Las Vegos Reno Concord Trenton Albuduerque Albany Bullate New York City Ashaville Chariotte Greensboro Raleigh Raimmarck Fargo Cleveland Columbus Deyton Deyton Edytora City Portane	Nevada Nevada Nevada Nevada Nevada New Hampshire New Hampshire New York New York New York New York North Cerolina North Cerolina North Cerolina North Carolina North Dakota Ohio Chio Chio Chio Chio Okiahome Oregon
	Valencia Stockholm Geneva Damescus Taipe Bangkok Tunis Ankora Istanbul Istanbul Abu Dhabi Dubal Aberdeen Betfast Rumingham Edinburgh Unetpool London	Spain Sweden Switzerland Syria Syria Talvan Thalland Turnsia Turney Turkey Turkey Turkey United Arab Emirates United Kingdom	55 81 58 77 52 77 62 55 56 77 66 47 80 78 78 77 81 61 57	Sofia Sentiago Belling Guengrhou Harbin Hong Kong Sherghal	Gulgana Chile China Chin	89 50 30 58 59 50 59 50 52 59 60 62 44 42 51 55 55 55 56 62 62 62 63 64 65 65 65 65 65 65 65 65 65 65 65 65 65	Las Vegos Reno Concord Trenton Abuquerque Albany Bullato New York City Asheville Charlotte Greenstoro Raleigh Rimmark Fargo Cileveland Columbus Deyton klahoma City	Nevada Nevada Nevada Nevada New Harroshire New Harroshire New York New York New York New York North Cerolins North Cerolins North Cerolins North Carolina North Dakota Offic Ohio Ohio Ohio Okiohome

Table A-2 cooling load temperature differences for calculating cooling load from sunlit roofs

	Reef Description of	0_				-		23		111			Set	ar T	Time:	4 5										
Va	Commuties	W/relat	1	2	1	14	5	5	7	- 8	41	_		_	-	_	15	115	17	18	10	20	20	12	25	3
2	Security September 2	N. F. T. S.	SIEE			-	-11.77		1000	sec a		-		-				Life and In		Acres (A)	Auto Carlo	-		1000		
9	WATER STATE OF THE PERSON NAMED IN	Contract of the last of the la	SCHOOL SECTION								_	_	****	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	appears.	REPAR	routes		-	44,555	MATERIAL			-		ø
1	THE RESERVE AND ADDRESS OF THE PARTY OF THE	1.209	0	-1	+4	-2	-3	-2	- 4	17	19	23	34	40	7/43	44	45	35	33	25	17	10	7	5	3	
	23.4 mm (or 50.8)	(2,700)							6						E											
	mun) insulation	The State of	10																							
	25 mm wood	0.963	3	2	0	-1	-2	-2	+1	2	- 3	13	22	27	35	22	41	43	22	35	29	21	15	11	-	
	with 25.4 mm		1																					135	O.E.	
	INDUNATION	100 miles	15												=							10				
	-101.6 mm L.W.	1.702	5	3	- 1	n.	-3	-	-2	1	- 1	18	15	25	31	36	30	20	40	37	12	25	19	14	10	
	connecte:												3					122	300	1			1	4	65.	
	50.8 mm H.W.	1.170	1	3	3	2		-1	0	2	76	13	17	71	78	33	36	27	37	34-	30	25	22	16	82	
	concerne 25.4	(0.693)		170	-	00.7			12.	100	-	-00	1000	200	ATTE	100	ED.	20	200	200			77.7		100	
	man (pr 50.8																									
	rems) insulations													0.5												
	25.4 m/s, wood *	-0.619	1-2	0	-2	-9	-	mal	-1	-0	3	9	75	22	-	48	95	26	**	44	**	mh	14	100		
	HILL 30.5	10000	17	V. Par		515	100	100	337	-37	10.5		್	076	T.		200	77.	370	-		-	27	100		
	torralneless		Ł	12	4											-										
	152.4 mm T. W	0.877	15	14	14	5.	Oe.	1	140	0		-			++	19.1	-	**		200	**		-	44	200	ŀ,
	powerele		E'			-	8.0	-	-	u	-	2		13	+0	29	23	23	22	30	23	36	28	24	12	ï
	63.5 mm_wood	0.73E	*	13	44	100		100	12	20	-	100	- 2	-	-	-	W			200			-	305		
	with 25.6 mm		12	72	**		N.	.0	- 4	3		5		31,	,15	35	23	2.7	29	37	31	30	23	25	22	ì
	insulation													710												
	203.4 mas L.W.	0.715	-			Sale				161		100	-	-		10.00		414		24	200	-	30	-210	eguo	
	con tress	MI CAN	- 44	17	14	12	10	- 4	6	5	4	-	3	7	11	14	32	22	25	38	30	30	20	27	25	1
	101 5 mm H-W.]	1.736	1	-	-	OF SE	-			350	35	10	135	1	60		Contract	20	/4 E	-349	E	-	1	27		4
	Concrete with	The state of the s	114	12	100	-	1	-	4	4	8	H	1.	15	T.F	22	25	21	25	30	29	27	25	21	19	
	ALCOHOLD TO VC-10715, ULTOV	(0.6FJ)																è			-					
	25.4 mm [or 50.5		1																							
	mnifelcani (curr	10 100	1	1200					- 3					20013		v = 57								- 17		
ŀ	63.3 mm wees	0.528	12	13	13	11	¥	- 8	40	3	- 25	5	7	10	23	17	71.	24	17	18	23	25	27	23	23	á
	twick insufarion	9000	1/2				1													-		*				
	Ruof ten see	0,602	19	17	15	24	11	11	9	8	7	\$	1	10	12	15	18	20	22	24	25	25	25	24	22	
	Byston																			415				155		9
	152.4 mm H.W.	8:664	18	16	24	17	F1	10	1	2	. 8	3	10	12	15	17	26	22	24	25	25	25	74	11	20	
	concrete with					900			2150					- 1	3	-	HOS	77	50	200	-	~		-		
	25,4 mm. (az 50,8														-				100	71			At-			
	mm) landarion																	120		100			100			
1	101.6 mm wood	0.602	inn	20	12	17	24	14	13	11	(0)			0	70	49	14	200		70		-	-	1		*
	with 25,4 mm (or		177	3 GA			-					100		- 5	75	20	*	24	400	w.	-	13	44	49	14	Q
	30.8 min)	1								63								87				39				Ē
	husbien.		1		12			4		10	or i	ď.,	10.75	- 2	20.7		-	4 .	- 4	· .						
B	AND THE PARTY	All In	125	55 W	ion.	1075	TIP.	1783	79558	MAL	WY:	PATE I	PROFES.	COURT	IPSO	nerty.	See a	aner	District	TENO	Seve	SEL	NO.	-	-	ú
٠	Bisel about with																									
		0.761	11	0	-1	-2	-3	-3	C	5	13	20	20	35	90	13	43	41	33	31	32	15	10	7	5	
	25.4 rem (or 50.8	(67133)	1		2					_ /	8 3		6												*	
	mms] Inquia rimn	* ***	1021	20	000				- 11	000				do			400	32	50							
	25-mm wood	0.653	11	-	6	5	3	2	73	2	4	.7	13	17	22	27	33	33	35	34	32	78	74	20	17	
	with 25.4 mm		100													2		3	(Contract)	141127			*		7	
	insulation													32						33						
	101.6 mm L.W.	0.751	110	8	6	4	1	1	C	C	2	5	10	Lo	31	22	381	34	50	30	39	30	26	21	27	
Ē	COPPOSIG.				_		+				1.4			=3	15			6		14		-	6237	220	100	-
ĺ	50.8 mm H.W.	0,744	115	14	13	11	10	- 45	7	7	- 8	- 20	12	24	17	19	22	90	20	TO F	40	-	-	21	-	ŕ
	monage 25,4	MARKET NA	200	A 100 PM	350	-	-570	1000		1	- 10	-		-		100	-	-	-	200	-48	-	-	ZL	24	
	mon fundacion		1											7												
	35.4 rum setend	8.471	110	11		-		1		-			100		**	-	-	-	20	-	-					Ų
	wish 50.8	100	1	1		110	16			-	4	100	10	*5	12	2.5	21	30	51	37	31	22	16	72	13	
	issulation		1											35									+			
	152.4 mm L.W.	0.619		de.			14	122	134	140	174	00	-	4	-	CLES	4440	1200	125.00	PERM				174.34		
	THE SECRETARY OF THE PARTY OF T	0.014	114	15	13	11	. 4	3	0	- 6	- 4	4		2	12	24	25	24	27	23	39	20	78	26	23	
	CODELEGE	27862	1						*																	
	63.5 mm wood	0.545	19	13	15	16	13	12	10	3	1	. 2		16	12	54	17	15	21	21	24	25	74	23	77	
	with 25.4 mm;					4	-	100	-	90	-	1	-	-	***	100	1	15	**	-	-	-		**	-	
	intulation.				4		2																			
		U.328	27	20	19	14	35	170	27	100	CID.	36	40		-	-	90	20	160	400		-	100	190	1	
		10000	-	-	**	4.0	+2	2.95	AA:	10	9	4	-		- 1	-1	34	78	19	32.1	23	52	15	25	24	
	293,4 mm L.W.		1-4			44	-	-		20	40	-0	133	14.1	-	EGA	1237	38	1215	1	68	1344		63		
	293,4 mm L.W.	0.333		10	3.7	Te	44	12	12	-12	11	11	12	13	12	26	11	13	20	21	28	21	31	20	29	
	293,4 mm L.W. CONTRIBE 193,6 mm ILW.	0.727	17.5	1700					-									. *								
	203.4 mm L.W. Crimbie 103.6 tem II.W.	0.727 (0.511)	122	363																						
	203.4 mm L.W. Contrace 103.6 tem 11.W. Contract with 25.4 mm for \$3.4		12.7													5										
	203.4 mm L.W. CONTINE 103.6 mm 1LW. CONTINE with 25.4 mm for \$3.8 mm) is old for	(0.511)				~~		-								5										
	203.4 mm L.W. Contrace 103.6 tem 11.W. Contract with 25.4 mm for \$3.4					16	14	13	12	11	10	10	10	11	12	14	16	13	19	21	12	25	25	27	22	

Table A-3 Latitude correction factor (LM) for latitude and month applied to walls and roof, north latitudes

La	Month	N	NNE		ENE		ES			5E		Horizoz	
16	Decembe			_	-4.			W 3		W		Roof	
	Jan./Nor				4.000		100		2	5.0	33/25	-5.0	
	Feb./Oct			HIGH.	-3.	10000			.2	4.4	100000	-3.8	
	Mar/Sep				-2.5			.0 1		2.7	3.8	-2.2	
	Apr./Au		0.000		-1.1			5 0.		0.0	0.0	-0.5	
	May/July	2.2	7777		-0.5	-		.5 -1.		-2.7	-3.5	0.0	
	June	3.3			0.0	C 1995		.2 -2.		3.8	-3.8	0.0	
	10000000	3.3	2.2	2.2	0.5	-0.5	-2	2-3,	3 -	4.4	-3.8	0.0	
24	December	-2.7	-3.8	-5.5	100								
	Jan./Nov	-22		-4.4	6,1		111226	7 1.	1 1	5.0	6.6	-9.4	
	Feb./Oct.	-2.2	-2.7	-3.3	-5.0			6-1.		5.0	7.2	-6.1	15
	Mar/Sept.	-1.6	-2.2	-1.6:	F3.3			5 1.0		3.8	5.5	-3.8	
	Apr./Aug	-1,1	-0.5		- TOTAL STATE OF THE PARTY OF T	7.7		5 0.5		1.1	2.2	-1.6	
	May/July		1.1	0.0	-0.5			I -0.5		1.1	-1.6	0.0	
	June.	1.6	1.5	1.1	0.0			5-1.6			-3.3	0.5	
		1 4,0	1.0	1.5	. 0,5	0.0	-1.	5 -2.2	- 75	3.3	-3.3	0.5	
2	December	-2.7	-3.8	-5.5			104-1	20 908					
	Jan./Nov.	-2.7	-3.8	-5.0	-6.1	-1.4	-2.	10001107		5.0	6.6	-9.4	
	Feb./Oct.	-2.2	-3.3		1-6.1	-4.4	-2.5			5.0	6.5	-8,3	
	Mar/Sept.	-1.6	-2.2	-3.8	14.4		-1.1			1.4	6.1	-5.5	
7	Apr./Ang.	-1.1	-1.1	-2.2	-2.2	-1.1	-0.5			2.7	3,8	-2.7	
	May/July	0.5	0.5	-0.5	-1.1	0.0	-0.5			0.1	0.5	-0.5	
-	June	0.5		0.5	0.0	0.0		-0.5		.6	-1.6	0.5	
1		Vij	1.1	1.1	.0,5	0.0	-1,1	-1,1			-2.2	2.1	
1	December	-3.3	-4.4	-5.5		22	275	1					
- 4	Jan./Nov.	-2.7	-3.8	-5.5	-7.2	-5.5		0,0	3	.8	5.5	-11.6	
	Feb./Oct.	-2.7	-3.8		-6.6	-5.0	-3.3		4	.4	6,1	-10.5	
	Mar/Sept.	-2.2			7-5.0	-3,3	-1,5		4	4	6.6	-7.7	
1	Apr./Ang.	-1.1		-2.7	-3.3	-1.6	0.5	0.000	3.	8	5.5	-4.4	
	May/July	0.0	0.0	0.0	-1.1	0.0	0.0	1.1	1.	б	2.2	1.6	
	una	0.5	.0.5		0.0	0.0	0.0	0.0	0.	0	0.5	0.5	
1		0.5		0.5	0.5	0.0	0.5	0,0	0.	0 -	-0.5	1,1	
I	December	-3.3	-4.4	-6.1	177		144	4				100	
J	an./Nov.			-6.1	A 100 M	-7.2	-5.5		1.		3,3	-13.8	
F	eb./Oct.			-5.5	E CANCEL CO.	-6.1	-4.4		2.		4.4	-13.3	
1					and the second		-2.7		4.		5.1	-10.0	
A	THE RESERVE AND ADDRESS OF THE PARTY.	1000			4		-0,5		4.		6.1	-6.1	
	fay/July		-0.5			-0.5	0.0	2.2	3.3	3	3.8	-2.7	
	ine	0.5		0,0	0.0	0.5	0.5	1.5	1.0		2.2	0,0	
-		U.J	0.5	1.1	0,5	1.1	0.5	1.1	1.1		1.6	1.1	

Table A-4 Overall heat transfer coefficient for windows, W/m².℃

	Wind Speed, m/s												
Material Type and		Single Glass		Doub	ım air								
Frames	< 0.5	0.5 - 5.0	> 5.0	< 0.5	0.5 - 5.0	> 5.0							
Wood	3.8	4.3	5.0	2,3	2.5	2.7							
Aluminum	5.0	5.6	6.7	3.0	3.2	3.5							
Steel	5.0	5.6	6.7	3.0	3.2	3.5							
PYC	3.8	4.3	5.0	2.3	2.5	2.7							

Table A-5 solar heat gain factor (SHG) W/m2, for a latitude angle of 32°

Month	Jan.	Feb.	Mar.	Apr	Man	Turn	Test	1	0	- MI UL	474	
N	76	85	101	114	120	700	. 544.	Aug.	acp.	Oct.	Nov.	Dec
NE/NNW	75	85	THE R		120			117	104	88	76	69
	1.7		117	252	350	385	350	249	110	88	76	69
E/NW	91	205	338	461	536	555	527	445	325	199		
ENE/WWW	331	470	577						200	10000	91	59
E/W.	552	647							546	451	325	265
SE/WSW	722	754	716 .					691	678	615	546	511
E/SW		4			628			663	716	738	710	688
	786	782	715 .	590	489	439	473	571	688	754	773	776
SE/SSW :	789	732	615	445	213	262	303	429	596	25		
1	776	697	The same of	266				1.0	11 A	710	775	795
iorizontal	555	625 .			man .		227	O COLOR	540	678	767	795
	_	-	152	933	874	871	861	836	770	672	552	498

Table A-6 Shading coefficient (SC), for single, double and insulting glass without interior shading

Type of Glass	Nominal	Solar	Shading Coefficient, W/ml.K						
	Thickness, mm	Trans.	The second second second second second	k. = 17.0					
Clear	SIN SIN	rle Glass	现在是国际工作中	AND DESCRIPTION OF					
CHEST	3	0.84	1.00	COLUMN SERVICE					
	. 6	0.78	0.94	1.00					
	16	0.72	0.90	0.95					
	1. 12	0.67	0.87	0.92					
lear absorbing	3	- 0.64	. 0.83	0.88					
	5	0.46	0.69	0.85					
4.,	. 10	0.33	0.60	0.73					
•	12	A 62		0.64					
THE RELEASE OF THE	Don	APPLIAL PROPERTY	0,53	0.58					
egular	1	ALCO LOURS		"是有这种人的 "。					
lace	5.1		0.90						
effective			0.83	TT-5					
FORE SAC			0.20-0.40	-					
CILL .	2	ing Glass	THE RESERVE AND ADDRESS OF THE PERSON NAMED IN	Company of the last					
4	3	0.71	. 0.88	0.88					
eat absorbing'	0	0.51	0.81	0.82					
grinite	.6	0.36	0.55	0.58					

Table A-7 Cooling load factors for glass without interior shading, north latitudes

Glass	Building		Solar Time, h													W. C		
Pacing	Construction	1	2	3	4	5	6	7	3	9	°18	11	12	13	14	15	16	17
	3					-1		345	3.0			100						••
70/	М.	0,15	0,13	0.11	0.10	0.09	0.09	0.09	0.10	0.11	0.12	0.13	0.14	0.59	0,29	0,40	0.53	0.56
	H	0.14	0.13	D.T.	0.11	0.10	0.11	0.12	0.13	0.14	0.14	0.15	0.16	0.22	0.30	0.40	0.49	0.54
												-		. 59				
	L										0.12							
WNW	34										0.11							
	H	0.14	0.13	0.12	0.11	0,10	0.11	0,12	213	9.14	0.15	0.16	0.17	0.18	0.25	0.36	0.46	0.53
										-								
	L	0.11	0.09	0.08	0.06	0.05	0.06	0,08	2.10	0.12	0.14	0.16	6.17	0.19	0.23	0.33	0.47	0.59
WW	M	0.14	0.12	0.13	0.99	90.0	0.09	0.10	011	0.13	0.14	0.16	0.17	0.16	0.21	0.30	0.42	0.51
200	, di	0.14	0.12	0.11	0.10	0.10	0.10	0.12	C 13	0.15	0.16	0.18	0.18	0.19	0.22	0.30	0.41	0,50
3	L	0.12	0.09	0.01	0.05	0.05	8,07	0,11	0.14	0.18	0.22	0.25	0.27	0.29	0.30	0,33	0.44	0.57
NNW	M,	0.15	0.13	0.11	0.40	0.09	0.10	0.12	015	0.18	0,21	0.23	0.20	0.27	0.28	0.31	0.39	9,51
Engre	H	0.34	0.13	0.11	0.11	0.10	0.12	0.15	0.17	0.20	0,23	0.23	0.25	0.28	0.28	0.31	0.38	0,43
19			33								1	-		4	2.3			
	L	0.11	0.09	0.07	0.06	0.05	0.07	0.14	0.24	0.16	0.48	0.58	0.60	0.72	0.24	0.73	0.67	0.59
HORIZ.	м.										0.40							
	H	0.17	0.16	0.15	0.14	0.13	0.15	0.20	0.25	0.1	6 0.45	0.57	0.50	0.62	0.5	0.6	0.58	0.51

Fenertration Facing		Solar Time, h														3 1 1 1 1 1 1				
	1	2	3	4	5.	6	7	. 8	9	10	11	. 12	- 13	14	15	16	17			
N	0.08	0.07	.0.05	0.06	0.07	0.73	0.66	0.65	0.73	0.80	0.86	0.89	0.89	08.0	0.82	0.75	0.78			
NNE	0,03	0.03	0.02	0.02	8.63	0.64	0.77	0.62	0.42,	0.37	0.37	0.37	0.36	0.35	0.32	0,28	0.23			
NE	0.03	0.02	0.02	0.02	0.02	8.56	0.76	0.74	155	0.37	12.29	0.27	0.26	0.24	0.22	0.20	2.16			
ENE			0.02																	
E -	0.63	0.02	3.02	0.02	0.02	0.47	0,72	8,80	6.76	0.62	0.41	0.27	0.24	0.72	0.20	0.17	0.14			
ESE	0.03	0.03	0.02	0.02	0.02	0.41	0.67	0:79	LSO	0.72	0.54	0.34	0.27	0.24	8,21	0.19	0.15			
SE	0.03	0.03	0.02	3.02	0.02	0.30	0.57	:0.74	6,81	0.79	0.68	0.49	0.33	9.28	0,25	0,22	0.18			
SSE	0.04	0.03	6.03	0.03	0.02	0.12	0.31	0.54	CJ2	0,81	0:81	0.71	0.54	0.38	0.32	0.27	0.72			
5	0.04	0.04	0.03	0.03	1.03	0.07	0.16	0.23	6.35	0.53	0.75	0.83	0.80	0.63	0.50	0.35	0.27			
SSW	0.05	0.04	0.04	0.03	0.03	0.09	0,14	0.18	1.22	0.27	0.43	0.63	0.78	0.84	0.80	0.66	0.45			
sw	3.05	0.05	0,04	0.04	0.03	0.07	0.11	0.14	0.16	D.19	0.22	0.38	0.59	0.75	0.83	0.81	0.69			
WSW	0.05	0.05	0.04	0.04	1.03	0.07	0.10	0.17	0.14	0.16	0.17	0.23	0.44	0.64	0.78	0.84	0.71			
W	0.05	0.05	0.04	0.04	0.03	0.05	0.09	0.11	0.13	0.15	0.16	0.17	0.31	0.53	0.72	0.82	0.81			
WWW	0.05	0.05	0.04	0.03	1.03	0.07	0.10	0.12	1.14	0.16	0.17	0.18	0.22	0.43	0,65	9.83	0.84			
NW	0.05	0.04	0.04	0.03	3.03	0.07	0,17	0.14	1.17	0.19	0.20	0.21	0.72	0.30	0,52	0.73	2.83			
NNW	0.05		0.04			ALL STATE OF THE PARTY OF THE P				0.30										
HOLIZ.	0.06	0.05	0.04	0.04	0.03	0.12	0.27	0.44	3,59	0.72	0.81	0.85	€.85	0.81	0.71	0.58	0.47			

Table A-8 cooling load temperature differences for glass convection

Solar Time	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	- 27	71	7/
CLTD. 'C	1	0	-1	-1					-	2	_	_	-	_	_	-								

Table A-9 outdoor air requirement for ventilation

Apolloss	Maximum Occupancy Pe	Ventil Requi	ation Air
Application	100 m ²	L/s/Person	
Offices Office space Reception areas	7 60	10.0	2.5-10.0
Telecomm, Centers . Conference rooms	60 -	10.0	_
Public sparer	50	. 10.0	-
Public restrooms	-	-	0.25
	100	25.0	_
Locker and dressing rooms	50	7.5-17.5	5-2.5
Smoking lounge	70	30.0	_
Elevators		7.5	5,00
Laundries:			5100
Commercial laundry	10 .	. 13.0	
Commercial dry cleaner	30	15.0	
Coin-operated laundries	. 20.	8.0	
Coin operated dry cleaner	20	8.0	
Food and beverage services:	1	- 1	
Dining rooms	70	10.0	
Cafeteria	100	10.0	-
Bars	100	21/4 5000000000000000000000000000000000000	-
Kitchens	20	15.0 -	_
Garages, service stations:	20	8.0	_
Enclosed parking garage			
Auto repair rooms	3	L/s/car	7.50
		-	7.50 .

Table A-10 Cooling load factors for lighting

Number of hours after lights are		operation	The second secon	operation
turned On	10	16	10	16
0	0.08	0.19	0.01	0,05
1	0.62	0.72	0.76	0.79
2	0.66	0.75	0.81	0.83
3	0.69	0.77	0.84	0.87
4 .	0.73	0.80	0.88	0.89
5	0.75	0.82	0.90	0.91
5 .	0.78	0.84	0.92	0.93
. 7 .	0.80	0.85	0.93	0.94
8	0.82	0.87	0.95	0.95
9	0.84	0.88	0.96	0.96
10	0.85	0.89	0.97	0.97
1.1	0.32	0.90	0.22	0.98
12	0.29	0.91	0.18	69.0
13	0.26	0.92	0.14	0.58
14	0.23	0.93	0.12	0.99
15	0.21	0.94	0.09	0.99
16	0.19	0.94	0.08	0.99
17	0.17	0.40	0.06	0.24
18	0.15	0.36	0.05	0.20

Table A-11 sensible heat Cooling load factors for people

Hours after each entry into			7	Cutal hor	irs in spa	ce.		
space	2	4	6	8	10	12	14	16
1	0.69	0.49	0.50	0.51	0.53	0.55	0.58	0.62
2	0.58	0.59	0.60	0.61	0.62	0.64	0.66	0.70
3	9.17	0.66	0.67	0,67	0.69	0.70	0.72	0.75
4	0.13	0.71	0.72	0.72	0.74	0.75	0.77	0.79
5	0.10	0.27	0.75	0.76	0.77	0.79	0.80	0.82
6	80.0	0.21	0.79	0.80	0.80	0.81	0.83	0.85
7	0.07	0.16	0.34	0.82	9.83	0.54	0.85	0.87
8 9	0.05	0.14	10.26	0.84	0.85	0.85	0.87	0.88
	0.05	0.11	0.21	0.35	0.87	0.88	0.89	0.90
10	0.04	0.20.	0.18	0.30	0.89	0.89	0.9	0.91
11	0.04	0.08	10.15 .	0,25	0.42	0.91	0.91	0.92
12	0.03	0.07	0.13	0.21	0,34	0.92	0.92	0.93
13	0.03	0.05	0.11	0.18	0.28	0.45	0.93	0.94
14	0.32	0.06	10.10	0.15	0.23	0.36	0.94	0.95
15	0.02	0.03	0.0E	0.13	0.20	9.30	0.47	0.95
16	0,02	0.04	0.07	0.12	0.17	0.25	0.38	0.96
17	0.02	0.04	0.06	0.10	0.15	0.21	0.31	0.49
18	B.01	0.03	0,06	0.09	0.13	0.19	0.25	0.39

Table A-12 Cooling load factors for occupants

Peripheral aras of offices with glazing area of 20%-50% 0.70-0.85 0.70-0.85 Core areas of offices and peripheral areas with less than 0.90-1.00 0.7-0.8 Apartments and hotel bedrooms	Application -		Diversit	Factor
20% glazing 0.90-1.00 0.7-0.8 Aparements and hotel bedrooms 0.30-0.50 0.4-0.0	Peripheral area of a Ferman	Service .	Lights	Prople
Apartments and hotel bedrooms Public rooms in hotels 0.30-0.50 0.4-0.6		50% than		0.7-0.8
	Aparaments and hotel bedrooms Public rooms in hotels	40	The State of the S	0.4-0.6

Table A-13 Cooling load factors for equipment

VETTO ALL DOCUMENTO	Y	ithout He	nd .	With Hood
Appliances	Sensible	Latent	- Total	All Sepsible
. Heir dryers (Blower type)	575	120	795	The same of the sa
Halr dryers (Helmet type)	550	100	653	-
Coffee brewer (electrical)	225	65	290	95
Coffee brower (gas)	490	- 210	700	415
Water heater	1,130	335	1,465	-
Coffee um (electrical)	1,075	350	1,425	440
Coffee ura (gas)	1,460	625	2,085	415.
Deep fat fryer (electrical)	820	1,930	2,750	730
Deep far fryer (gas)	2,080	2,030	4,160	830
Touster	1,055	705	1,760	440
Domestic gas oven	2,430	1260	3,630	
Reasting oven	500	320	820	
Food warmer (gas)	1,550	400	1,950	400
Egg boiler	335	220	555	_
Frying griddle	13,600	7,200	20,800	4,150
Eotplate	1,550	1,060	2,510	780
Neon sign, per meter length	56	_	55	100
Sterillrer	190	350	540	-
Laboratory burner	470	120	590	-
5mali copy machine	1,760	_	1,760	-
Large copy machine	3,515 -	-	3,515	_
Motors:			10.000	0)1
400-2,000 TV	2,100	_	1,100	440
2,000-15,000 W	2,430	-	2,430	

Table A-14 Heat gain from occupants in watt person

Type of Activity	Typical Application	Yotel Heat Dissipation Adult Mole	Total Adjusted Heat Dissipation	Bent	Heat,
Seated at mat	Theater:	-	3		5000
	Matines	111.5	94.0	64.0	30.0
	Evening	121.5	100.0	70.0	50.0
Seared, very light work	Offices, botels, apartments, restaurents	128.5	114.0	70.0	44.0
Moderately	-total and a second	124.5	2130	70.0	44.6
active office	Offices, Borels.				20
work	spartments	135.5	128.5	71.5	57.0
	Department stors, retail				
Standing, light work, walking	store,	157.0	143.0	71.5	71.5
Walleing, seaced	Drug store	157.0	143.0	71.5	71.5
Standing.	Tres onto	10.00	3.55,0	1,2.25	*,*
walking					
slowly -	Bank	157.0	163.0	71.5	71.5
Sedentary work	Restaurant	168.5	157.0	78.5	78.5
Light bench				100000	
reck	Factory	238.0	214.0	78.0	126.0
	Smill-Parts	101			
Moderate work	assembly	257.0	243.0	87.0	186.0
Moderate	-				-
duccing	Dance halls	257.0	241.0	87.6	156.0
Walking at 1.5	Factory	286.0	285.0	107.0	178.0
Bowline	* married J	200.0	*05.0	107.0	170,0
(participant)	Bowling alley	428.5	414.0	166,0	248.0
Heavy work	Factory	428.5	414.0	155.0	248.0

⁽a) Adjusted heat disalpation is based on the percentage of men, women and children for the application.

Table A-15 Overall heat transfer coefficients Uw , for basement walls below grade (W/m^2 . °C).

	U_, W/m ² *C									
Depth Below		Insulation Resistance, m1. C/V								
Grade (m)	Uninsulated	0.715	1.430 2.145							
0.0-0.3	2.328	0.863	0,528 0.380							
0.3-0.6	1.261	0,659	0.449 0.335							
0.6-0.9	0.880	0.534	0.386 0.301							
0.9-1.2	0.676	0.449	0.341 0.273							
1.2-1.5	0.545	0.392	0.301 0.250							
1.5-1.8	0.449	0.341	0.273 0.227							
1.5-2.1	0.392	0.307	0.250 0.210							

Table A-16 overall heat transfer coefficients for typical ceiling constructions, W/m^2 , $^{\circ}C$, for $R_0=0.03~m^2$, C/W

No.	Construction	R _d	Thickness	Layer
	Asphalt Mire	0.028	3.02 in	0
	Concrete	0.029	0.05 m	07
	Insulation '	0.750	0.03 m	O - Lucio - Lu
(1)	Reinforced Concrete	0.034	0.03 m	0-13-10-0
	Coment Block	0.147	3.14 m	0
	Pleater	0.027	2.02m	0
	¥=0.88 .			
	Asphalt Mix .	0.028	0.02 mi	0-
- 43	Concrete	0.029	0.05 m	0-
	Insulation	0.500	0.02 m	
(2)	Reinforced Concrete	0.034	0,06 m	0-12
	Cement Block	0.189	0.18m	0
	Plaster	0.017	0,G2 m	© —
	U=1.08			
	Asphalt Mix	0.028	£.02 m	0
. 1	Concrete	0,329	6.05 m	
(E) 1	Insulation	0.750	0,03 m	(1) - Telephone (1)
1	Reinforced Concrete	0.057	0.10 m	0-1000000000000000000000000000000000000
3	Plaster '	0.017	0.02 m	(i) (ii) (iii) (ii
1	T = 1.00			
				- 4
3	Inside Surface :	0.110	425	Φ.
) 3	Metal Lath	0.083	0.02 m	0 / \
1	Air Gap .	0.164	0.10 m	0 2
M	stal Cuiting Suspension	n — .	1777	0
	crugated Metal Deck			0
(Concrete Slab	0.029	0.05 m .	0
1	nsuktion	0.500	0.02 m	0
1	wilt-up roofing	0.058	0.01 m	0. 1
-	Ontside Surface	0.030	-	D 234 5578
T	7= 1.03			

Table A-17 Air change per hours in residences and commercial application

Type of Room or Bullding	No. of Air Change per Hour
Rooms with no windows or exterior doors	0.5
Rooms with windows or exterior doors on one side only	1.0
Rooms with windows of exterior doors on two sides	1.5
Rooms with windows or exteriors doors on three sides	2.0
Entrance halls	2.0-3.0
Factories, machine shops	1.0-1.5
Recreation rooms, assembly rooms, gymnasium	1.5
Homes, apartments, offices	1.0-2.0
Classrooms, dining rooms, lounges, hospital rooms, bitchess, laundries, ballrooms, ballrooms	2.0
Stores, public buildings	2,0-3.0
Todets, auditorium	3.0

⁽¹⁾ For rooms with weather stripped windows or storm such, use 2/3 of these values.

Table A-18 Overall heat transfer coefficients for wood and steel doors, W/m2,°C

Door Type	Ç	S	Without tom Door	With Wood Storm Door	With Metal Storm Door
25 mm-wood		1	3.6	1.7	2.2
35 mm-wood			3.1	1.6	
40 mm-wood		1	2.8		1.9
45 mm-wood				1.5	1.8
50 mm-wood		140	2,7	1.5	1.8
Aluminum			2.4	1.4	1.7
		1	7.0	- !	_
Steel		24	5.8	_	
Steel withs				*/	
Fiber core			3.3		
Polystyrene core		3	2.7		_
Polyurethane con	e	17	2.3		=

Table A-19 Recommended and maximum air velocities for warm and cool air systems

	Recom	mended Vel	ocity, m/s	Maxi	œum Valoci	ty, m/s
Description	Residence Bulldings	Public Buildings	Industrial . Buildings	Residence Buildings	Public Buildings	Industrial Buildings
Cutzide air	2.5	2,5	2.5	- 4.0	4.5	6.0
intake			-	1		C-4
Heating cells	2.3	2.5	3.0 -	2.5	3.0	3.6
Cooling calls	2.3	2.5	3.0	2.5	3.0	3,5
Fan suction	3.5	4.0	5.0	4.5	5.0	7.0
Fan oudet	5.0-5.0	6.5-10.0	8.0-12.0	8.5	7.5-11.0	1.5-14.0
Main duct	4.0-4.5	5.0-6.5	6.0-9.0	4.0-0.0	5.5-8.0	6.5-11.)
Branch ducts	3.0	3.0-4.5	4.0-5.0	3.5-5.0	4.0-6.5 -	5.0-9.0
Branch risers	2.5	3.0-3.5	4.0	3,5-4,0	4.0-6.0	5.0-8.0

Table A-20 Circular equivalents of rectangular ducts for equal friction and capacity,

	-						1	ingth s	d Kless S	ode of	Restan	gular I	Duct (a)	in many				_	_	
Leth	100	125	150	178	266	225	250	275		350		-			600	650	700	750	Sile	961
Adj.									Circui	ar Du	t Diam	utir, m	int.	11.450	22.000			3.277	-	
100	(199)					-				-			_		_	_	_		_	
123	122	137																		
139	[3]	120	164																	
III C)(IAI	IOI:	172	2191																
200	132	172	189	204	214															
225	163	THE	200	216	232	246														
250	SHO.	3907	23(9)	228	244	259	27.8													
275	176	199.	220	238	256	- 272	287	301												
366	192	267	224	245	200	281	299	314	328											
350	195	255	243	2670	- EK6	305	322	339	354	STATE										
(000	307	235	260	293	209	324	345	361	378	4(9)	457									
450	217	247	274	290	327	143	363	343	400	411	454	492								
500	222	288	28%	313	317	360	STATE OF	401	420	455	488	538	341							
590	236	268	299	3.26	1552	373	398	419	410	1	311	541	573	-166						
600	245	279	510	33%	365	390	414	436	451	495	533	567	200	603	200					
680	253	TAKE	321	331	378	494	6429	432	474	515	881	58V	622	629	656					
2(8)	261	299	331	362	391	418	443	467	490	311	573	610	211	633	706	711	202			
130	200	306	341	373	603	430	457	482	566	-550	5102	630	666	-700	712		765			
500	275	314	350	25%	414	440	470	196	520	367	689	549	867	722		76A	792	W799		
900	289	330	367	482	435	463	494	577	548	597	6-13	686	726		755	187	RIF	947	3875	
1000	301	344	384	420	454	486	517	546	574	1076	674	719	762	763	399	KXX	884	E92	923	984
1100	313.	-358	709	437	472	506	-515	360	516	632	-303	731		802	840	876	911	5944	976	3657
£200	334	370	Att	453	490	131	434	908	620	177	131	THO	795	358	579	916	953	SPER	1022	2096
1300	334	382	426	248	396	343	577	670	642	701	757		H27	102	914	554	993	1036	1066	1123
14/07	145	214	4.19	410	332	MAN	395	628	562	334	(78)	80E		964	948	990	1091	14369	1107	3177
1500	355	404	452	193	336	575	612	648	681	745	805		NAS-	914	3400	(1924)	1995	111/02	1146	2220
10000	362	413	461	3000	331	501	129	665	700		627	560	913	56.5	1011	1167	1100	1143	1163	1266
700	2572	425	475	521	504	605	Y644	682	7863	765	1849	883	939	99)	1041	1988	1133	11.77	1219	1201
1500	379	434	483	533	577	4.19	660	(95	393	804		900	964	1016	111699	HILL	\$164.	1200	1253	1335
1900	SKT	224	496	591	500	661	674	713	751	823	809 800	933	955	10.53	1996	714n	1395	1241	1286	4571
5986	395	453	306	355	602	646	585	728	707	NAD-			M12	1068	1122	1174	1224	1271	1318	\$403
1100	402	462	316	566-	616	0.59	710	743	792	RST.	908	973	標準	100	H	1200	1292	\$30L	1548	5429
2200	\$10	470	525	577	624	621	715	137	797	874	925	963	1035	1112	1172	1226	1274	1329	1375	1470
2300	412:	47K	114	387	636	483	728	571				1011	1076	1117	116	1251	1505	1356	1486	1500
400	424	486	543	507	647	625	740	784	842 926	N797	363	1691	11997	11159	1218	\$2.15	11100	1387	1434	1533
2500	430	294	553	606	65W	700	753	797		1915	9111	1050	3110	1280	1341	1299	1385	5409	1861	1561
1000	4325	500	360	618	668	312	764		840	920	3996	1068	1136	1200	1212	1322	1379	1414	145%	1,5109
190	443	580	380	625	678	雅	775	810	453	935	0012	1083	1154	1220	1251	1341	1800	1450	1513	1612
909	\$50	516	377	634	988	738	79.7	822 834	No.	959	11/25	1102	1173	1240	1364	1,766	1425	1483	153%	1644
700	456	521	355	643	697	739			879	964	1043	1119	1150	1259	1324	1397	1447	1504	1562	E530
	-	-	NI COL	Water St.	THE PARTY	DAM.	:799.	845	805	977	1055	3135	1208	1272	1544	1006	Line	152%	1386	1696

							1	ength (One Ski	e of Re	etangu	dar Du	er tirk r	nem.						
tigth	1000	1100	1200	1300	1,000	1500	pe00	1706	1900	1960	2000	2100	2200	2300	2400	2400	2600	2700	2800	2900
Adj.b									Circub	or Duct	Diame	ter, ma	m	22.73000	FI-SEAT	100		21313	-	
1000	1093											10000		_	_	_			_	
1100	1146	1202																		
1200	1.19%	1250	1312																	
1300	1244	1306	1365	1421																
1400	1289	1354	1416	1473	1530															
1500	1392	1400	1464	1,526	1584	1610														
1600	1373	1444	1311	1574	1035	1093	1749													
1700	1413	1488	1335	1621	1684	1745	1803	1858												
1886	1451	1527	1544	1662	1732	1794	1854	1912	1965											
1900	1488	1566	1640	1710	1778	1841	1904	1964	2021	2077										
2900	1523	1604	1680	1753	1822	1889	1953	2014	2073	2131	2186									
2100	1358	1640	1719	1793	3865	1933	1999	2863	2124	2183	2220	2296								
2200	1391	1676	1756	1833	1906	1977	2014	2110	2177	2233	2292	2350	3405							
2300	1623	1710	1793	1871	8947	2019	2088	2155	2220	2283	2343	2402	2450	2514						
2300	1655	1044	1528	1900	1996	2000	2131	2200	2266	2330	2303	5455	2531	2568	2674					
2500	1685	1776.	1862	1945	2024	2100	2173:	2243	2311	2377	2441	1502	2562	2621	2678	2711				
2600	1715	1808	1895	1980	2661	2140	2213	2263	2355	2422	2492	2551	2612	2672	2730	2767	3842			
27700	1744	1839	1979	2015	2097	21771	2253	3327	2398	2466	2533	2008	2661	5939	2782	1810	3896	2052		
2900	1772	1809	1961	2048	2133	2214	2202	2267	2435	2510	257x	2644	2708	2771	2832	2891	2949	3006	3061	
2900	1800	1898	1992	2081	2107	2250	2329	2406	2480	2552	2621	2689	2755	2819	2681	2941	3001	3059	3115	3170
inte b	sed on t	- 13	KINP C	Sw to del	X28					,					Town Brief V				CVES	9119

Table A-21 Equivalent length L_o, of various fittings.

	L_{i}
Fitting	m
45° Round elboy	1.5
90° Four pieces elbow	3.0
Gradual reduction	6.0
45° Round Tee;	- 1
Main run	1.5
Branch	11.0
90° Round Tee:	
Main run	1.5
Branch	15.0
90° Rectangular elbow	5.0
Abrupt round contraction or	
expansion	11.0

Table A-22 Model 4SNOD four-way throw square diffusers.



NECK SIZE Ak	NECK VELOCITY FPM	200	300	400	500	600	700	800	90
	Total Pressure	.619	.039	.067	.10	.14	19	34	3
6.X6.	Tetal CFM	50	75	100	525	150	175	200	
	CFM such side-a	13	19	25	32	38-	44	50	500
Ak = .15	Throw each side-a	2.3	3.5	4.7	3.9	A.II	7.11	8-15	
9°X9"	Tetal CFM	112	168	224	250	336	392		
	CFM each side-2	28	42	94	-	84	98		
Ak = 28	Threw each side-a	2.3	3.5	4	310	6-12	7-14	Service Control	
12° X 12°	Total CFM	200	300		500	600	BA.		
	CFM each side-a	50	7.5	Total Control	125	150		916	
Ak = 5	Threw each side-a	24	4.7	30	6411	7.11			411
15°X 15°	Total CFM	312	468	601	750	936			
	CFM each side-z	78	117	150	195	235			
Ak = .79	Threw each side-a	3.5	4.8	510	7.13	8-16			
18°X 18°	Total CFM	450	634	300	1125	1350		DNR 1	
	CFM each side-a	113	169	25	281	338			
Ak -1.11	Throw such side-a	3.5	15	A Ja	7.11	9-17			
21° X 21°	Total CFM	10	345	1224	1530		Titlata.		1754
	CFM each side-a	10	139	306	382	191	TOU !	918	
Nr = 1.54	Throw each side-a	14	4	6-11	7-13				
14°X24°	Total CFM	- 00	100	1660	2006				lab
	CFM each side-2	200	300	400	500		-	an I	MB.
Ak-2	Throw each side-a		5.9	6-12	7.14				

Table A-23 Fixed blade Return Air Grille Models 7145H.

Oxe	Ex-4	Area (sq. ft.)	Factor	Neg. SP	.00	1 .00	2 .90	0 .01	0 .0	00 00 16 .00 70 .16	2 .83	1 .04	0 .83	00.
	1014	0.20	0.23	NC.	20	1 22	50			0 12	0 14	0 100	The second second second	
525	10 85	0.28	0.55	CFM	25	50	84	11	2 14	17	-		30	3
	12 x 4 12 x 5	0.20	0.30	100	-	-	-	-	1	Can			252	28
10 x 8	16 x 4	0.25	037	CFM NC	35	70	105	14	9 17	5 210	240	250	the second second	33(
8x8	Hx5	0.38	0.40	CFM	36	76	314	15	19	0 221		364	342	36
12 1 0	18±4	6.42		CFM	42	-84	126	160	1 2H	20	25	29	33	389
	10×0	0.92	0.45	AC.	-		-	1 2	16		294	336	378	421 38
12 X &	24x4	0.58	0.59	CFM NO	58	116	174	232	29	348	400	464	222	580
10 x 10	Ne7 Nx4	0.61	0.62	CFM	01	122	183	288	300		26 427	488	549	516
18 x 0	14x2 30x4	3.22	-	CEM	65	130	-	-	17	and the second	27	32	35	133
1000	28×4	0.65	0.67	NC	-	130	190	200	320	390	450 26	520	565	030
12 x 10	10×8 20×6 24×5	5.74	0.74	CFM	74	148	222	290			518	12 592	000	740
12 x 12	NAME OF A	0.00	0.00	CFM	90	180	270	300	18	23	26	33	32	-49
***	16 x 8 36 x 4 16 x 12 20 x 8	0.90	0.89	NC.	22	1,000	-	900	430	248	23	728	810	900
14 x 14	16 x 12 24 x 8 20 x 10 34 x 6	124	1.22	CFM	124	246	372	490	020	744	808	992	1110	1240
18 # 12	地方科 2818	137	134	CFM	137	274	411	548	19	822	939	34	38	43
-	22 x 10 38 x 8 20 x 12		(101	版		-224	-	15	20	Z	30	1090	1233	1570
24 7 10	30 x 8	152	1.42	NO NO	132	304	450	15	766	912	1864	1210	1368	1320
15 x 16	18 x 14 30 x 8 20 x 12	164		CFM	154	328	492	030	820	984	1148	1312	1476	42
20.00	18 x 10 30 x 10			CFM	722	-	-	16	21	. 26	31	36	39	1048
24 11 12	25x14 35x8	1.85		NC .	185	370	553	740 15	923	1110	1295	1480	1005	1850
18 x 18	24×14 22×10	2.10		CFM	210	420	630	840	1030	1200	1470	36	1890	2100
30 x 12	HXM MXH	242		CFM	232	464	690	16	21	27	32	-37	40	43
CALL S (8.7.	22 16 35 x 10 24 x 18 35 x 14	232	2.23	NC .	2		0.00	925	1100	1392	1024	1806	2058	2325
	24x18 35x14 25x16 35x12	261	248	CFIM	201	522	783	1044	1305	1566	1827	2088	2849	2010
22 x 22	PARE BAR	217	0.00	CFM	317	634	931	1708	1585	78	23	38	41	44
	Nin Bill	3.17	200	NC.	772	-	-	18	23	1902	2219	2536 38	2803	3170
	HXII	154		DEM NE	334	708	1862	1410	1770	2124	2478	2832	3189	3340
14 14 14	西大型 豆木包	3.79		Part	379	738	1137	1515	1895	2274	34	30	42	46
	28 x 20 36 x 16 22 x 20 45 x 14	9/4	- 3	VC O	-	-		15	23	29	2055	3032	3411	3790
PU A 10	40 x 10	427		IC IC	427	854	1281	1708	2133	2562	2989	3416	3843	4270
	28 x 34 45 x 14	447	410 0	FM .	447	894	1341	1788	2235	2082	3129	40 8576	4028	4470
Beat	80 x 20 30 x 20			EFM .	477	024	4.694	10	24	30	35	40	43	47
0 x 24	22 x 22 40 x 16	4.77	100	0	-	934	1431	1905	2383	2862	3339	3818	4293	4770
8 x 28	8x25 80x20 8x22	527			200	1040	120000	2080	2000	3129	3840	4180	4080	5295
5 2 24 3	0x28 44x20		- 0	FM :	574	1148	1722	20	25	31	35	41	44	48
14	0 x 72	534	N	C	-	1136	1144	2290	2670	3444	4018 36	4592	\$100 45	5740
	8x24 8x26	5.99		-	199	1198	1797	-	2995 26	3294	4198	4792	3391	3990

Table A-24 Air Handling Unit.

Inlet Water Temp. 45°F- Coils are of 8 Fins/inch

Model	2	Coll	AFR		4 R	ows			6.R	ows	_		40	ows	_
moder	DB	WB		TCAP	S.CAP	WFE	MPD	TCAF	5.CAS	WER	I WPD	TCAP			_
	19	- ik	SCFM	BTUR	STUR	SPM	FT	eru/H	BTUN	GPM	FT	BTUH	B.CAP BTUH	SPM.	WPE
	71	63		413363	290955	87.0	9.47	485135	355133	112.0	1.61	1	7-1-1-1	-	
AHEITSO	78	65		410000	287900	90.0	10.09	566726	379140	128.0	-	559688	402501	1250	2.17
	60	67	13000	48,5000	303610	97.8	21.61	654756	433336		4.59	001097	438374	1010	6.47
	85	70	1	202000	321180	101.0	12.53	E00109		142.0	2.66	707113	428053	158.0	8.00
	78.	65							470484	168.0	7.68	912115	392507	105.0	10.87
2000	71	65	1	489000	352780	37.0	8.10	055748	475627	149.0	424	T93495	539291	103.0	0.97
AHUQDO	80	07	20000	495000	358-678	99.0	8:42	700163	509429	109.0	5.37	189301	577102	187.0	7.66
	82			202000	354510	101.0	8.74	886249	543271	190.0	0.70	1038191	013350	205.0	9.43
	52	79	_	215060	375930	103.0	9.30	1078248	630175	223.0	9.07	1199000	090150	218.0	12.0
	76	63		210080	415140	102.0	\$1.85	820021	598039	176.0	T.64	960200		-	
Delization .	718	65	25000	515000	408910	123.0	12.10	962024	637022	190.0	5.26	-	#70981	195.0	11.50
1000	60	62	*3000	520000	402480	184.0	12.32	1000000	639000	200.0		985000	683000	197.0	11.27
	85	70	0	525000	429450	195.0	12.54	1020000	664020	Timber Section 1	5.71	1020000	000000	204.0	12.02
	70	60						1400000	664050	254.0	10.86	1000090	784500	212.0	12.91
- 11	78	65		920000	484120	196.0	11.83	950900	723900	190.0	8.27	1020000	779286	204.0	11.54
MEJ 320	80	87	33500	825000	471130	105.0	12.65	995000	724380	199.0	5.12	1050000	773850	218.0	12.17
	85	-		535086	472946	197.0	12.47	1050000	724700	210.0	10.08	1070000	763990	2140	12.60
=	0.0	70		345000	\$11755	139.0	12.01	1070000	769338	214.0	10.44	1550000	808780	210.0	10.04
	70	63		385000	582675	117.0	14.14	975000	820550	125.0	E.37	1050900		_	=
HEARDO .	78	65	40000	600000	079080	120.0	14.81	1000000	615000	200.0	6.77	-	885100	210.0	21.71
	80	67	40000	625000	277580	125.0	13.30	1050000	1000			1076000	875260	2140	12.12
	85	70		800080	631150	130.0	17.12	1005000	815850	211.0	9.80	1090000	664378	218.0	12.54
diam'r.				311111		230 E	11:10	1485500	871785	217.0	10.20	1110000	122746	222.0	12/90

- AFR: Air flow rate (SCFM). SCFM: Sandard value of Air Flow Rate at sea level, where:
- Air Density= 1.2 kg/m² (6.075 lbft²)
- Elevation= Zero (Std.)

- WB: Wet bulb

- T.CAP. Total capacity (MBH)
- WPD: Water pressure drop (Feet of H₂O)

- WB:
- SCAP. Sensible cooling capacity (MBH)
- T.CA
- WB:
- WB:
- T.CA
- WPD

Table A-25 "PAH" Static pressure drop.

No.	Module	1 in Width	th Thick Insul Depth (mm[lnch])	ation Height	Static Pressure Drop inch of water
1	Mixing Box Module+1 inch Flat Filter	1370[53.9]	750[29.5]	1370[53.9]	0.08
2	95% Bag Filter Module+Media	1370[53.9]	750[29.5]	1370[53.9]	0.68
3	Cooling / Heating Module	1370[53.9]	500[19.7]	1370[53.9]	930
4	4 Rows Cooling / Heating Coil			1920[33:9]	0.233
5	Forward Curved Fan Module	1370[53.9]	1450[57.1]	1370[53.9]	0.08
6	Petra 8 Fan		1.0.0[4.03]	-110	0,00
	External Static Pressure				0.5

Pressure Drop Through Coils

3/8 coil pipe

I Fins Per Inch	_			^	Ro	ws Pres	sute Dr	op (Incl	h Of Wa	ter)				
Face Velocity (FPM)	Dry	Wet	Dry	Wet	Dry	Wet	Dry	4 Wet	Dry	Wet	Dry	Wet	Dry	Wet
350	0.024	0.028	0.048	0.057	0.072	0.035	0.096	0.115	0.116	0.149	0.136	8 452	0.492	0.21
400	0.029	0.036	0.060	0.071	0.039	0.108	0.121	0.144	0.146	0.188	0.172	0.205	0.230	PROPERTY
450	0.036	0.043	0.073	0.087	0.110	0.131	0.147	0.176	0.179	0.231	0.211	0.252	0.282	0.27
500	0.644	0.052	0.087	0.104	0.130	0,156	0.175	0.210	0.215	0.277	0.254	non-realizable and	NAME OF TAXABLE PARTY.	0.33
550	0.051	0.061	0.102	0.122	0.154	- Harristonia	0.206	0.246	1,000,00	0.328	0.300	0.303	0.338	0.40
600	0.059	0.071	0.118	0.142	0.178	0.212	0.238	0.285	0.297	0.382	0.349	0.358	0.399	0.47

Table A-26 Chiller RWC Model 530 from Petra company.

Model IOVC	218	1	60	-310		356	390	430	470	Pin	-	(Santage
Pewer Supply Voll/Phase Ti				-		1000		3PH-50Hz	-	530	580	630
Cashe				_	-	11	_		_			
Finishing			-	_	-	FIGURE .	to the same	Galvanion	Esteel			
Compressor		_	-		-		-	Static Peru		II.		
No. of Compressors				_	Ti.	74	imetical	v Salet S	Ilon			
Grade OFOIL			-	_	_		100 tt 20	-	3		4	
Off Charge ILin	104	1 1	10	A 50	II a	25633	BOOK IN	l benivale	-	-		
Coder	1000	100	20.]	.0.00	12	23000	-	3.25	6.66	3.80	1.258.1.3	0.50
No. Of Confers			_		_		Shell	& Tabe				
Retriggesur			-	_	_	_	-	1				
Control		_	-	_	-	_		-22				
Refrigeration Circuits		- 7		_	1	-	Expans	ing Valra		,		
Condenser			-	_		-	-	-4	3		4	
Flus Per Inch		_	-	_	_	Copp	or Tubes	Aluminum	Fins			
Rows	1	_	-	_	-	_		12				
Face Area [Pi	28.00	1 30	w. II	33.00	11	5.00	14.00	4	-			
Condenser Fan	-	1	-11	10000	15	53,007	45.00	Harris Co.	45.00	60.00	60.00	6400
No. Of Fans		_	-		_	_	130	peller				1241
Air Flow Rate [CFN	10816	252	1 1	36340	1 3	901E	2903s	II South	H mosts			3
Operation Weight (Approximately) [Kg]	695	77		107		man and	The same of	28931	29038	21370	3(320	41100
[142]	477			N/A		HILE	1015	709	1109	1389	1389	1547

Note:

Electrical Data Table.

MODEL	POWER SUPPLY	CO	MPRES	SOR		CFM		MC	Man	
	[Volt:Ph/Hz]	NO	RLA	LRA	No.	KW	FLA	SICA	MOP	MIDS
25	380-420/3/50	4	20	130	2	1.1	3	-91	110	100
RWC 430	230/3/69	4	41	237	2	2.2	9.5	193	225	250
	380/3/60	4	24	160	2	2.2	5.5	113	125	125
2/1	380-420/3/50	3	28	155	2	1.7	3	97	125	125
RWC 470	230/3/60	3	58	380	2	2.2	9.5	208	250	250
	380/3/60	3.	35	235	2	2.2	5.5	125	150	160
The Control of the Co	380-420/3/50	4	24	145	2	1.1	3	108	125	125
RWC 530	230/3/60	4	50	255	2	2.2	9.5	212	250	315
	380/3/60	4	32	155	2	2.2	5.5	147	150	160

KW: Nominal Output Power (in Kilo Watt)

RLA: Rated Load Ampere. FLA: Full Load Ampere.

MOP: Maximum Overcurrent Protection. MDS: Non-Fused Main Disconnect Switch.

LRA: Locked Rotor Ampere. MCA: Minimum Circuit Ampacity. CFM: Condenser Fan Motor.

^{*} Data Above Are Based On Water IN/OUT: 55/45 °F / F

^{**} For Power Supply Voltage Refer To Electrical Data Tables

Table A-27 Heat pump performance data cooling part load WRA-420.

	Source			L	and		Capacity	Heat of	Miner	Source
EWT	GPM	WPD	EWT	GPM	LWT	WPD	Btu/h	Rejection Btuh	Watts	LWT
			50	7.5	40.0	16.7	371,290	410,056	13,061	51.5
			44	95	41.6	23.2	376,802	415,498	13,105	51.7
	75.0	9.6	55	75	44.3	16.7	399,720	438,132	13,293	52.3
	1000	370	1775	90	45,9	23.2	405,919	444,252	13.344	52.5
			60	75	48.5	16.7	429,362	467,432	13,541	53.2
40			0.000	90	50.3	23.2	436,301	474,297	13.600	53.3
			50	75	40.0	16.7	387,750	433,753	13,768	49.6
				90	47.6	23.2	393,548	439,552	13,813	49.8
	90.0	13.3	55	75	44.2	16.7	417,559	463.575	14,004	50.3
	100000	50%	1000	90	45.9	23.2	424,085	470,107	14,056	50.4
			60	75	48.4	16.7	448,656	494,714	14,257	51.0
			-	90	50.2	23.2	455,968	502.042	14,317	51.1
			55	75	40.7	16.7	380,340	450,013	15,183	60.9
			30	90	42.2	23.2	385.822	455,762	15,230	61.1
	75.0	9.6	55	75	45.0	16.7	409,340	480,302	15,433	61.6
	Thomas .	77.	200	90	46.6	23.2	415,502	486,735	15,487	61.8
			60	75	49.3	16.7	439,573	511,873	15,700	62.4
50			77.5	90	50.9	23.2	446,459	519,078	15,762	62.6
			50	75	40.7	16.7	377,271	434.244	15,423	59.1
			24	90	42.1	23.2	382,749	439.804	15,459	59.2
	90.0	13.3	55	75	45.0	16.7	406,150	463,562	15,668	50.7
	00000	2332		90	46.5	23.2	412,314	469,822	15,720	59.0
			60	75	49.2	16.7	436:274	494,168	15,929	50.4
			00	90	50.9	23.2	443,177	501.186	15,990	60.5
			50	75	41.5	16.7	335.475	383.304	18,694	80.4
		- 1	30	90	42.8	23.2	340,029	387,721	18,740	80.5
	75.0	9.6	58	75	45.9	16.7	361,037	408,104	18.954	81.1
	1,000		-00	90	47.3	23.2	366,152	413,068	19.007	81.2
			60	75	50.2	16.7	387,672	433,960	19.229	81.8
70			90	90	51.7	23.2	393,394	439,517	19,289	81.0
			50	75	41.5	16.7	355,032	430,739	19.255	78.7
			20	90	42.8	23.2	359,890	435,745	19,300	78.6
	90.0	113	55	75	45,8	16.7	382,183	458.725	19.509	79.2
	-	1	***	90	47.3	23.2	387,645	464,355	19.561	79.4
			60	75	50.2	16.7	410,492	487.919	19,779	79.8
			60	90	51.7	23.2	416,606	494,228	19,838	80.0

Table A-28 Heat pump performance data heating part load WRA-420 and correction factor.

50	urce		t.	nad .		Capacity	Heat of		Source
EWT	GPM	EWI	GPM	LWT	WPD	Stuth	Absorbaces Stuft	Watts	LWT
-			75	103.0	16.7	500,597	305,626	AN 192	
		90	90	100.9	23.2	501,420	395,062	27,176	59.6
	Massa	300		112.8	16.7	493,212	374,220	30,342	59.6
	75.0	100	75 90	110.7	23.2	493,988	376,295	29,984	60.1
		222		122.6	16.7	486,284	354,408	man-to-the delication	
70		110	75 90	120.5	23.2	486,989	356,550	33,895 33,499	60.5
			75	103.1	16.7	498,374	411,879	27,324	60.6
		90	95	101.0	23.2	499,242	414,011	26,995	61.2
	1	444	75	112.9	16.7	490,678	391,948	30,505	61.7
	90.0	100	90	1198	23.2	493,495	394,163	30,141	
		440	75	122.8	16.7	483,460	371,042	34,076	616
		110	90	120.6	23.2	484,232	373.335	33.679	62.1
			75	105.5	16.7	581,123	475,857	25,819	
		90	75 90	103.0	23.2	582.563	478.645	26,449	72.1
	75.0	100		1153	16.7	570.523	454.074	29,888	72.7
	75.0	100	75	112.7	23.2	571,848	456,916	29.472	72.6
		110	75	125.0	16.7	560,738	431,539	33,380	73.3
85		110	90	122.5	23.2	561,924	434,419	32,916	73.3
		200	75	165.7	16.7	593,522	504.747	27,308	74.1
		90	90	103.2	23.2	\$95,076	507,780	26,927	74.0
	99.0	100	75	115.4	16.7	582,234	481,390	30,424	74.6
	-99.0	100	75 90	112.9	23.2	583,663	484,473	29,996	74.5
		446		125.2	16.7	571,808	457.274	33.974	75.1
		510	75 90	122.7	23.2	573,087	460,389	33,497	75.1

- 1. Heating Data in BOLD * Freeze protection of the source loop is required.
 2. All data is based on 100% water as the heat transfer fluid.
 3. Apply capacity correction fluidors based on the percent and freeze mixture.
 4. Do not select units above 120°F leaving water temperature for the load in the heating mode or below 40°F for the load in the cooling mode.
 5. Capacity Bruh produced by the load loop.
 6. Load water loop serving the air handler or terminal device.
 7. Soorce heat rejection water loop, geothermal or bollentower loop.

EWT = Entering water temperature, "F GPM = Gallons per minute flow

WPD - Water pressure drop, ft. of water Bluth - Blu per hour of heat transfer LWT - Leaving water temperature, "F

Cooling EER	C_{fc}	Heating COP	C_{fh}
11	1.31	3.0	0.75
13	1.26	3.5	0.77
15	1.23	4.0	0.8
17	1.2	4.5	0.82

Table A-29 Long-Term change in ground filed Temperature.

Equivalent Full Load Hours Heating/Cooling	Bore Separation, m	Temperature Penalty, K	Base Bore Length, m/kW (refrigeration)
1000/500	4.6	Negligible	16.6
1000 1000	4.6	2.6	19.5
	6.1	1.3	17.8
500/1000	4.6	4.2	22.5
	6.1	2.2	19.7
	4.6	7.1	29.9
500/1500	6.1	3.7	22.0
	7.6	1.9	19.4
	4.6	Not a	dvisable
0/2000	6.1	5.8	27.4
	7.6	3.1	21.8
Cor	rection Factors	for Other Grid Pa	ifterns
1 × 10 grid	2 × 10 grid	5 × 5 grid	20 × 20 grid
$C_f = 0.36$	$C_f = 0.45$	$C_f = 0.75$	C _f =1.14

Table A-30 High density polyethylene pressure drops."1 1/4 in "

	Flow		Velo	city		Pressure	Denn	
(m²/s)	(Men's)	(US gpm)	(mis)	(fiva)	(Fartioom)	(mmHyO/100m)		(RH 20/100H)
1.3E-4	0.13	2.1	0 135	0.44	1041	106	0.046	
1.4E-4	0.14	2.2	0.145	0.46	1178	120	0.052	0.106
1.55-4	0.15	2.4	0.166	0.51	1317	134	0.068	0.12
1.6E-4	0.16	2.6	0.186	0.55	1459	149	0.064	0.134
1.7E-4	0.17	27	0.177	0.58	1647	188	0.004	0.149
1.8E-4	0.16	2.9	0.187	0.61	1797	163		0.168
1.8E-4	0.19	3.0	0.197	0.65	2002	204	0.079	0.183
2.0E-4	0.2	3.2	0.21	0.68	2157	220	0.088	0.2
3.0E-4	0.3	4.8	0.31	1.02	4437	452	0.095	0.22
4.0E-4	0.4	6.3	0.42	1 38	7395	764	D.196	0.45
5 DE-4	0.5	7.9	0.62	1.7	10785		0.33	0.75
6.0E-4	0.6	9.5	0.62	2.0	14975	1100	0.48	1.1
7.0E-4	0.7	11.1	0.73	2.4	19628	1527	0.65	1.53
8.0E-4	0.8	127	0.83	2.7	24651	2001	0.87	2.0
9.0E-4	0.9	14.3	0.94	3.1	31199	2514	1.09	2.5
0.0010	1.0	15.9	1.04	3.4	36976	3161	1.38	3.2
0.0011	1.1	17.4	1.14	3.8		3770	1.63	3.6
0.0012	1.2	19.0	1.25		44741	4562	1.90	4.6
0.0013	1.3	21	1.35	4.1	51027	5203	23	5.2
0.0014	1.4	22	1.45	4.4	69886	6107	2.6	6.1
0.0015	1.5	24		4.8	69454	7082	3.1	7.1
0.0016	1.6	25	1.56	5.1	76263	7777	3.4	7.8
0 0017	1.7	27	1,68	5.5	86771	8648	3.8	8.9
0.0018			1.77	5.8	97958	9989	4.3	10.0
0.0019	1.8	29	1.87	6.1	109819	11196	4.9	11.2
0.0020	1.9	30	1.97	6.5	115/99	11910	5.2	11.9
0050	2.0	32	2.1	6,8	129417	13197	5.7	13.2

Figure A-31 F0 vs. G for a cylindrical heat source,

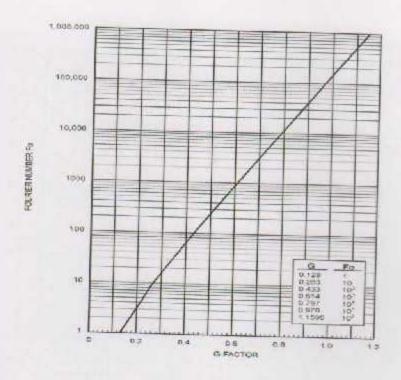


Figure Λ-32 Performance curves for TPE Series 1000 Grundfoss pump.

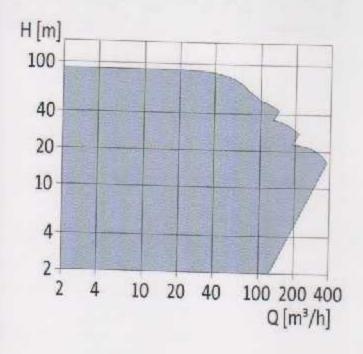
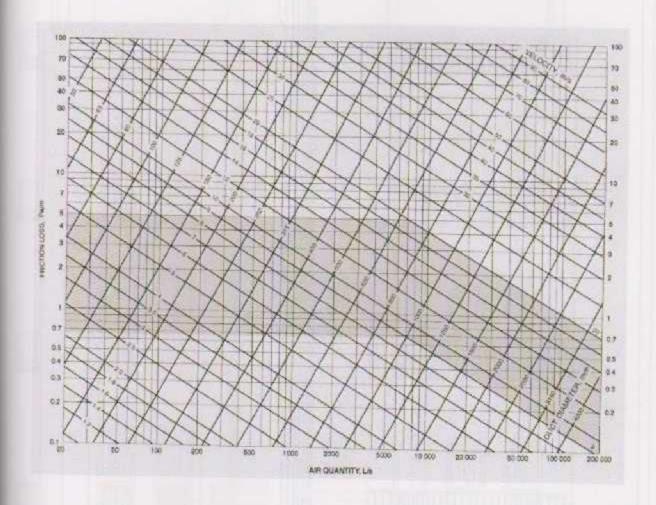
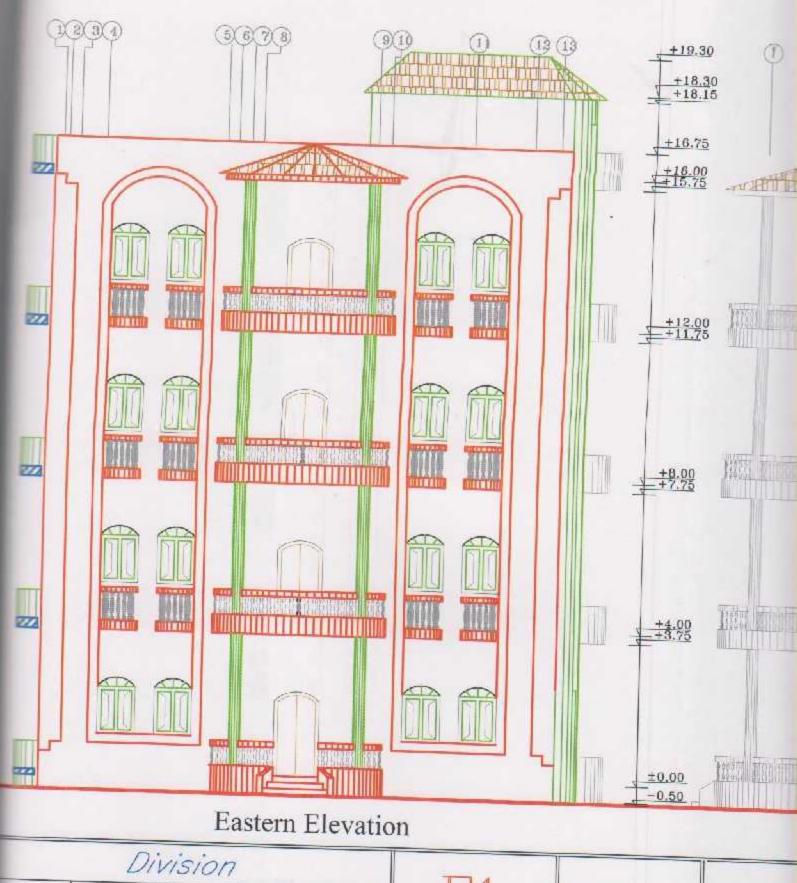
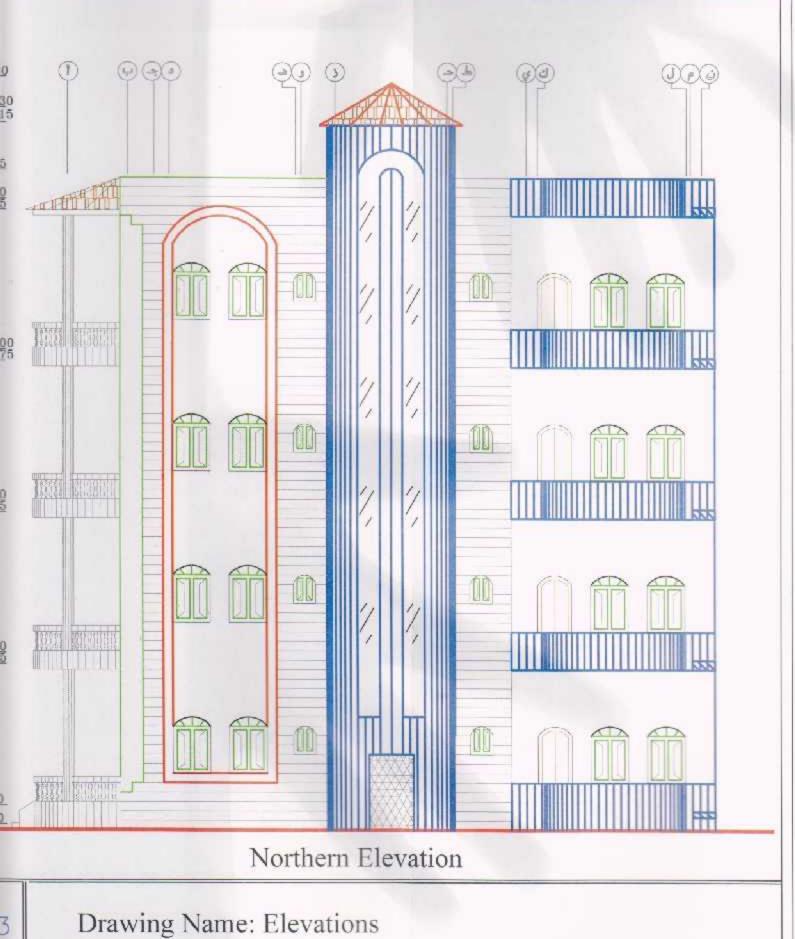


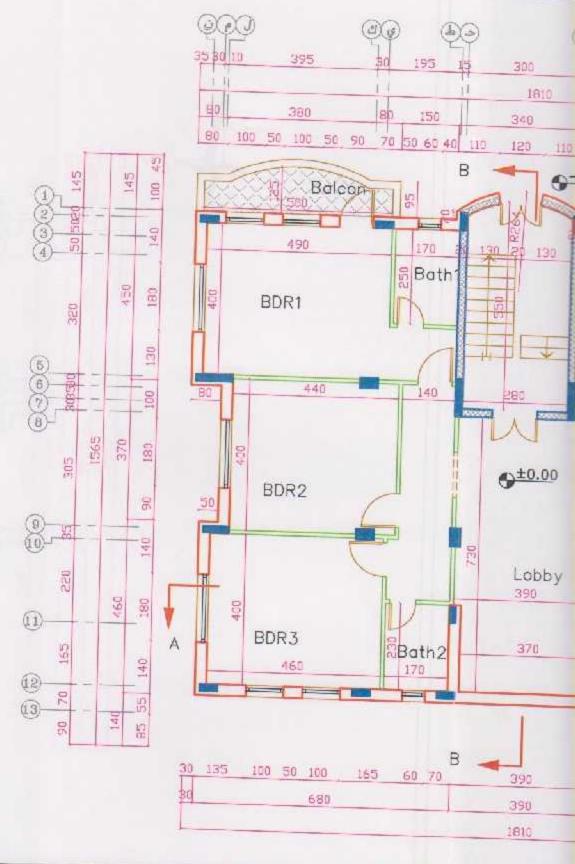
Figure A-33 Pressure drop (Δ P/EL), for air in galvanized steel ducts, based on round duct diameter.



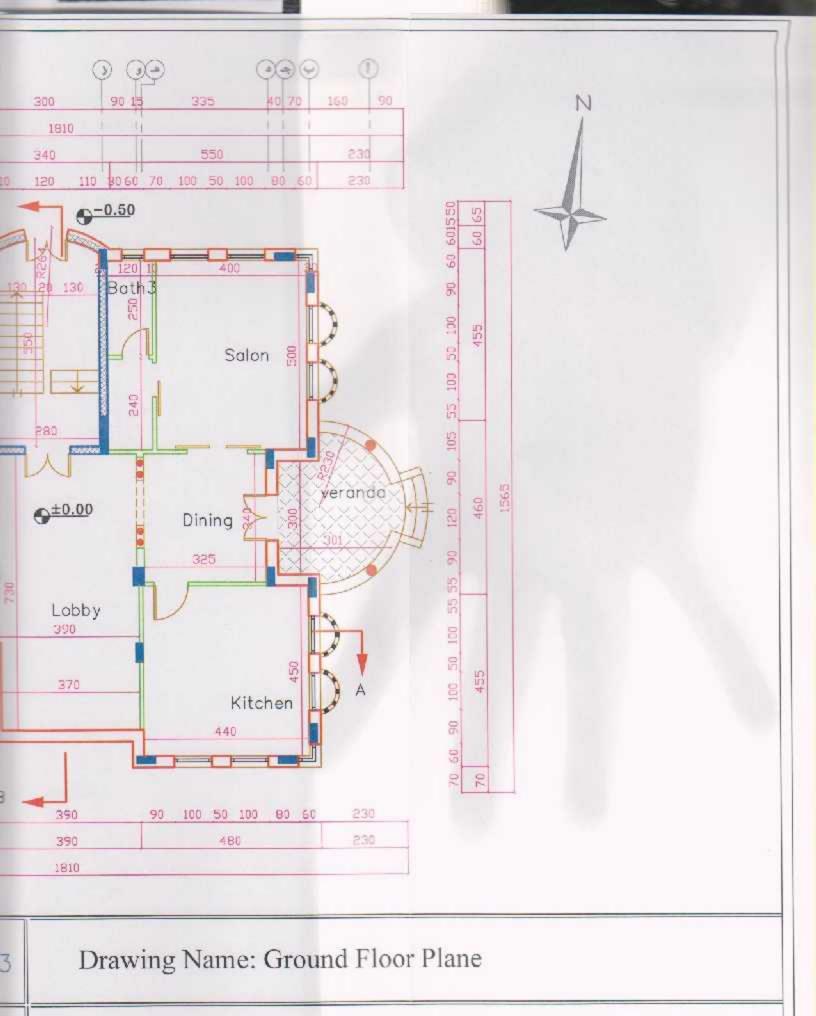


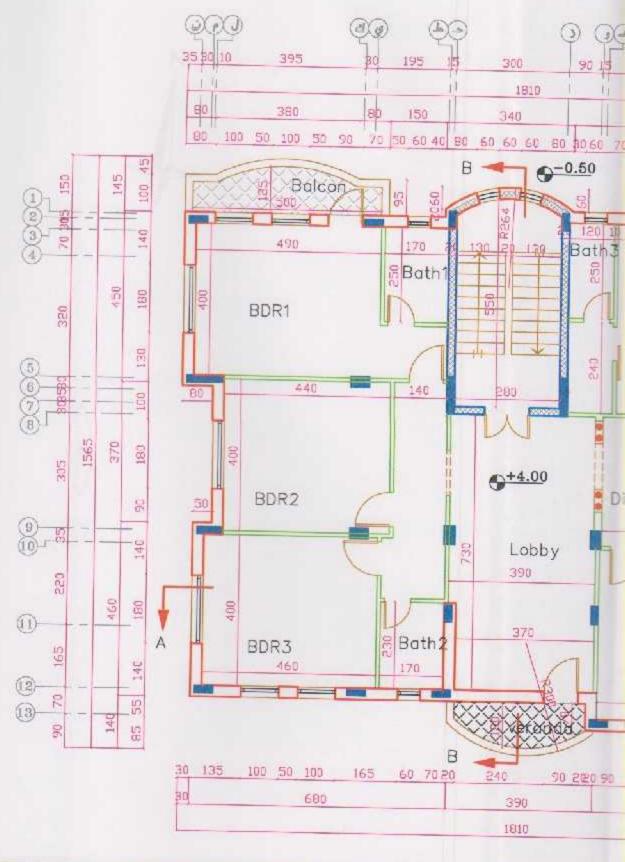
	Division					
Name:	IBRAHIM&HANI&MOHAMMAD	SCALE:	F'1	21.5.2013	Dra	
pervisor	Eng.Mohammad Awad	1/100	Graduation			
F	igure A-34	Sign	Project	HEBRON	Pale	



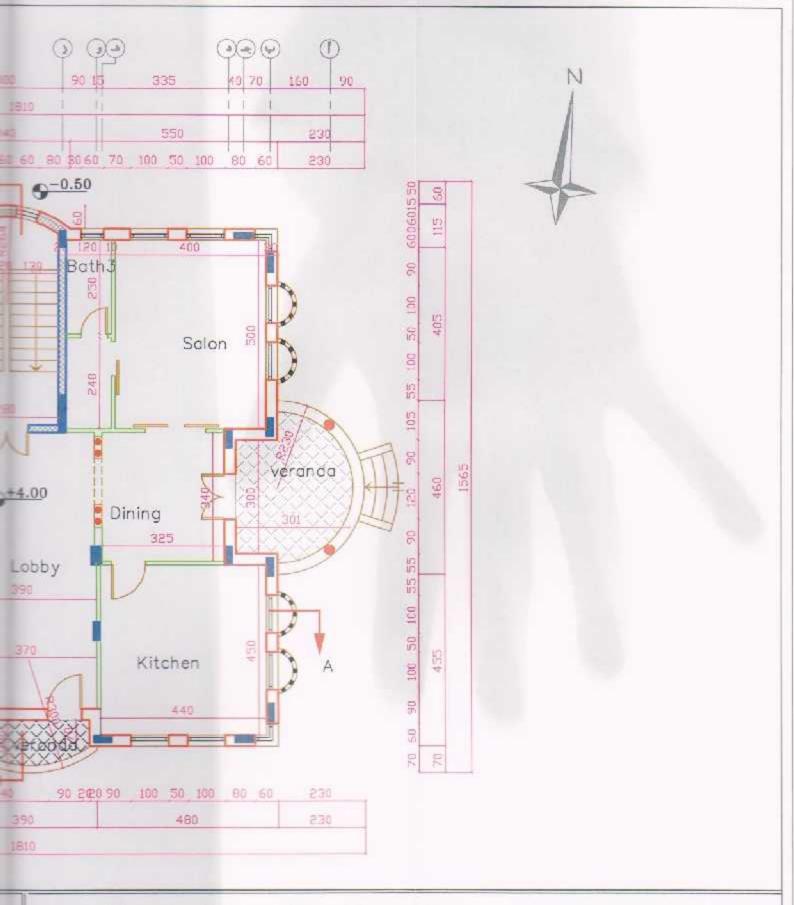


Division		TIC			
Name:	IBRAHIM&HANI&MOHAMMAD	SCALE:	F'2	21.5.2013	Dra
upervisor	Eng.Mohammad Awad	1/100	Graduation		
F	igure A-35	Sign	Project	HEBRON	Pale

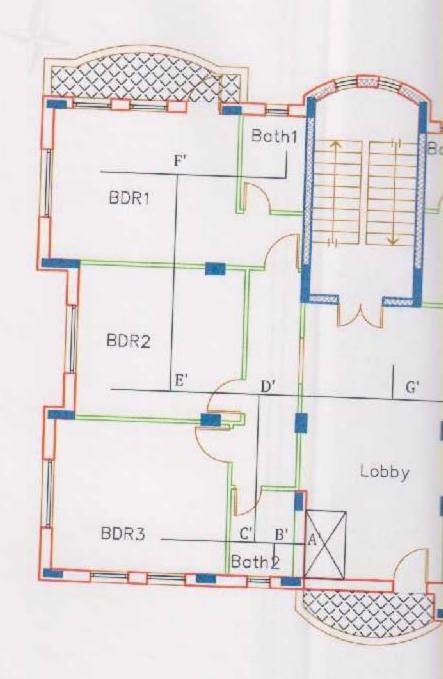




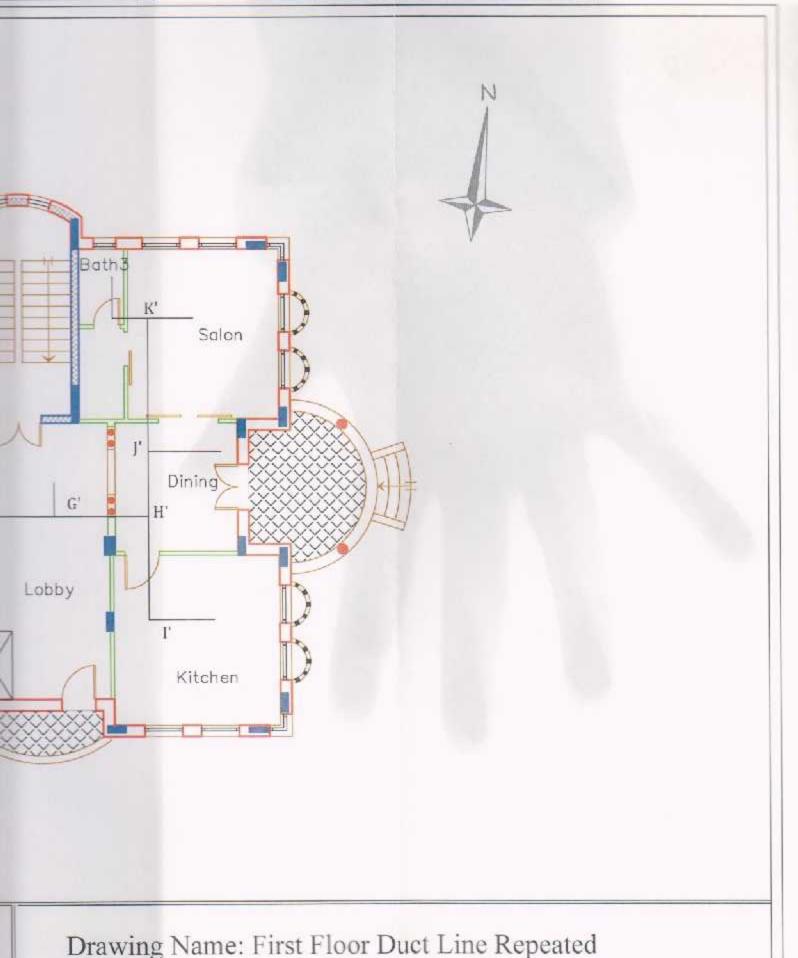
Division			Do		Dr
Name:	IBRAHIM&HANI&MOHAMMAD	SCALE:	F'3	21.5.2013	Re
upervisor	Eng.Mohammad Awad	1/100	Graduation		
F	igure A-36	Sign	Project	HEBRON	Pales



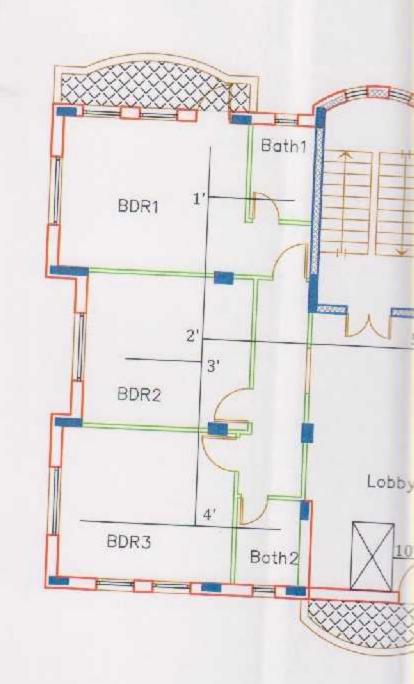
Drawing Name: First Floor Plane Repeated



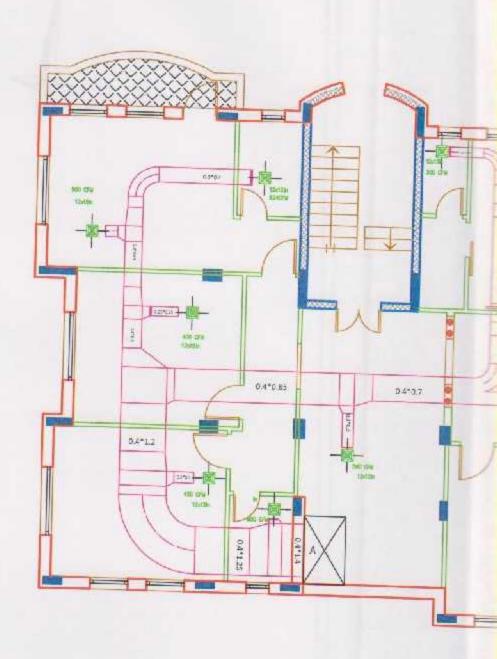
	Division				
Vame:	IBRAHIM&HANI&MOHAMMAD	SCALE:	F'4	21.5.2013	Drav
pervisor	Eng.Mohammad Awad	1/100	Graduation		
F	igure A-37	Sign	Graduation Project	HEBRON	Pales



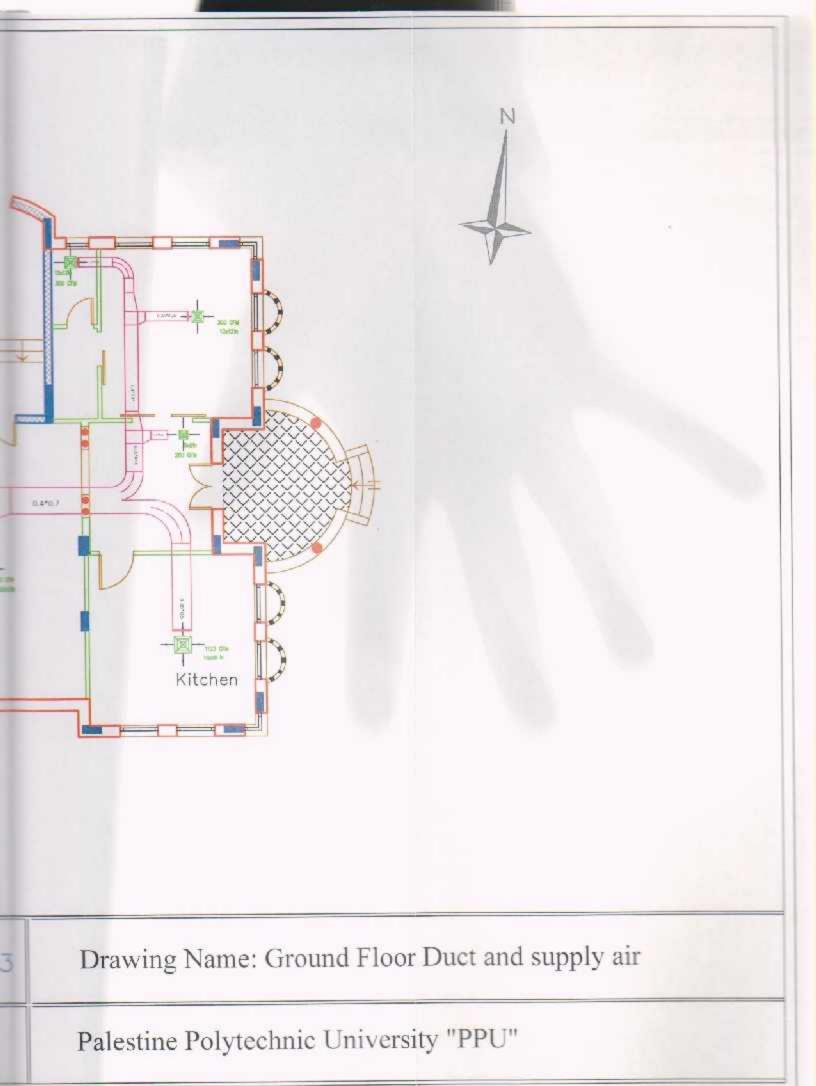
Drawing Name: First Floor Duct Line Repeated

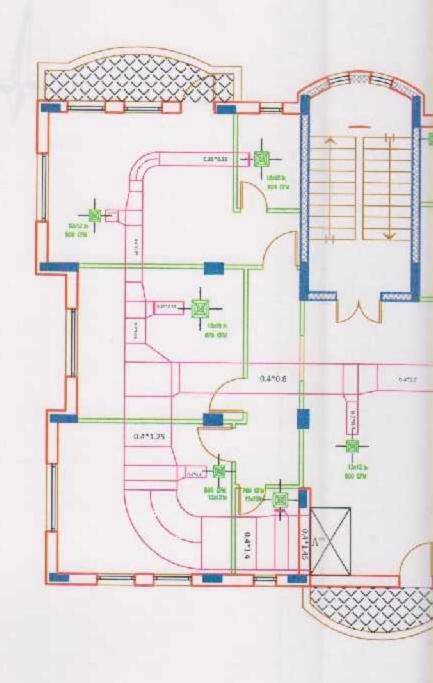


	Division				
lame:	IBRAHIM&HANI&MOHAMMAD	SCALE:	F5	21.5.2013	Dra
pervisor	Eng.Mohammad Awad	1/100	C 1 .		
F	igure A-38	Sign	Graduation Project	HEBRON	Palesti

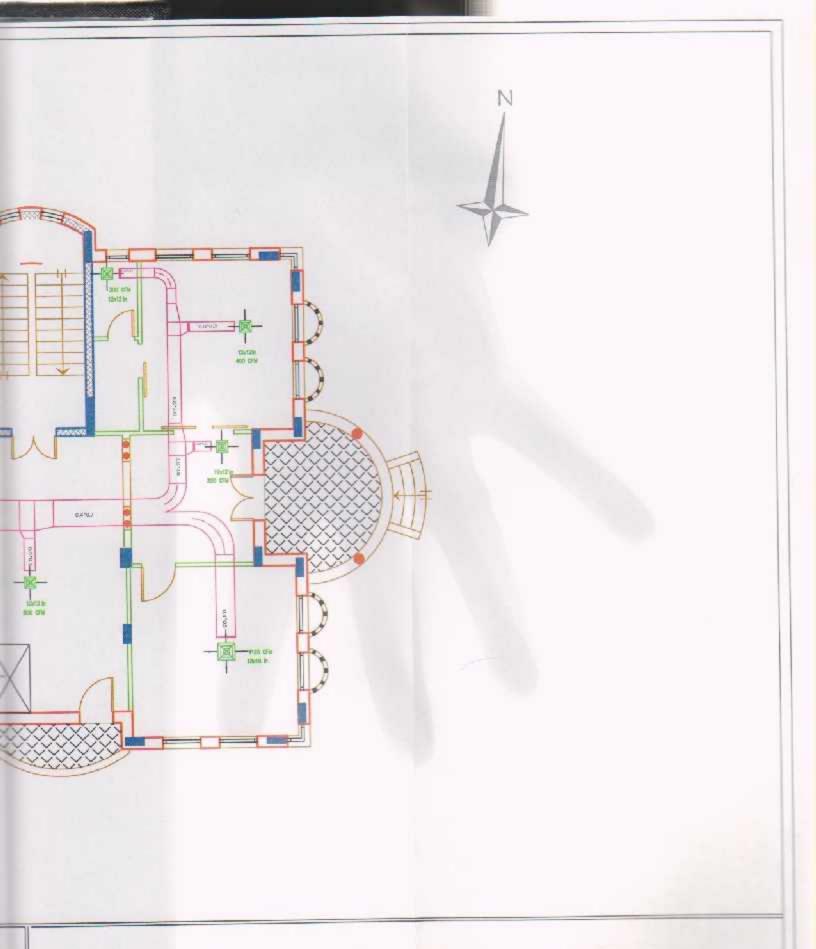


Division		T 6			
ame:	IBRAHIM&HANI&MOHAMMAD	SCALE:	F'6	21.5.2013	Drawi
pervisor	Eng.Mohammad Awad	1/100	Graduation		
F	igure A-39	Sign	Project	HEBRON	Palesti

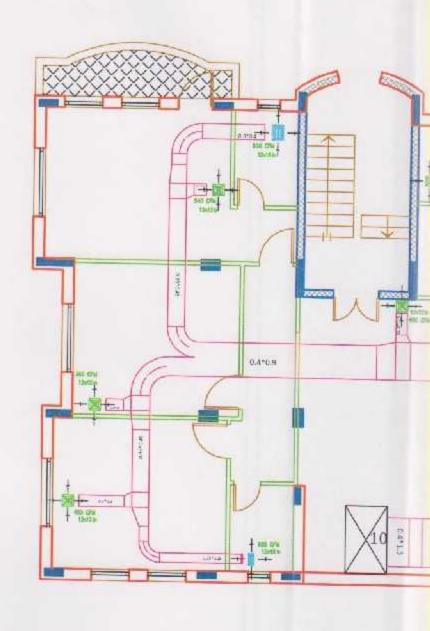




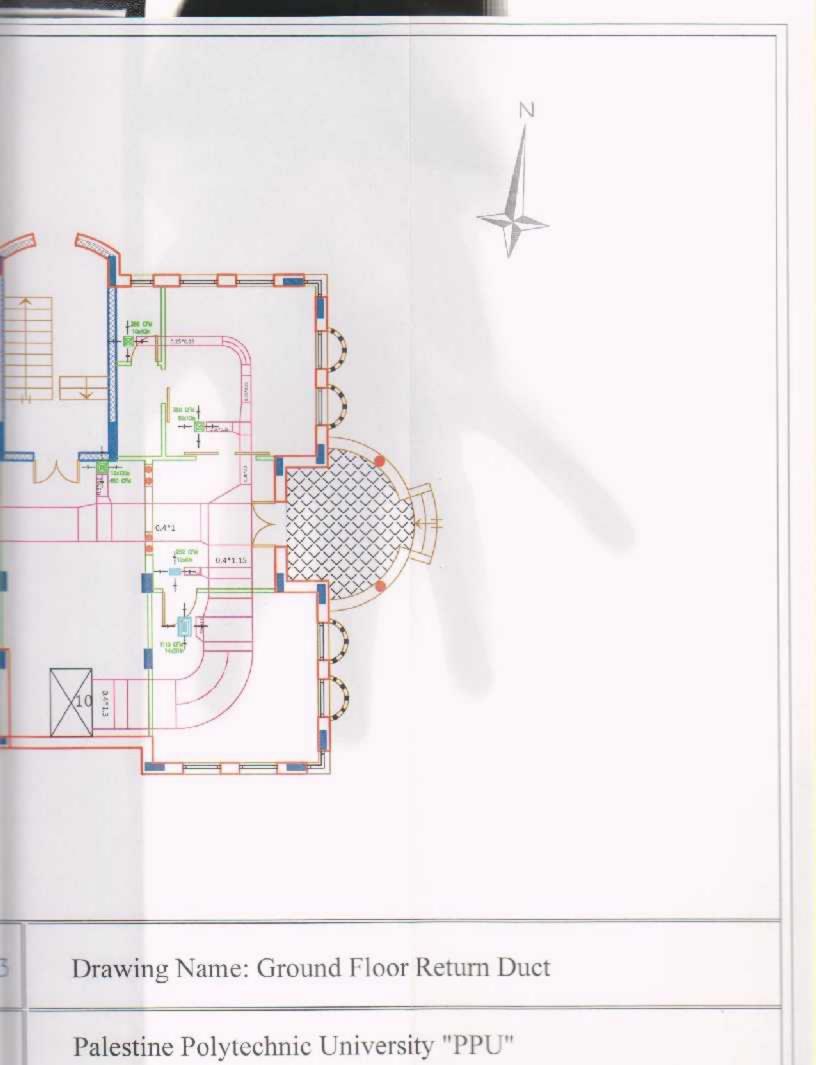
Division			TIM		
Name:	IBRAHIM&HANI&MOHAMMAD	SCALE:	F'7	21.5.2013	Dra
Supervisor	Eng.Mohammad Awad	1/100	Graduation	HEDDON	D 1
F	Figure A-40		Project	HEBRON	Pale

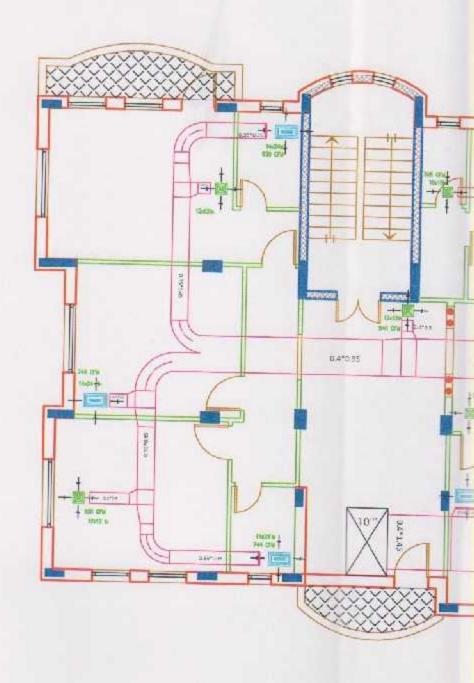


Drawing Name: Third Floor Duct and supply air

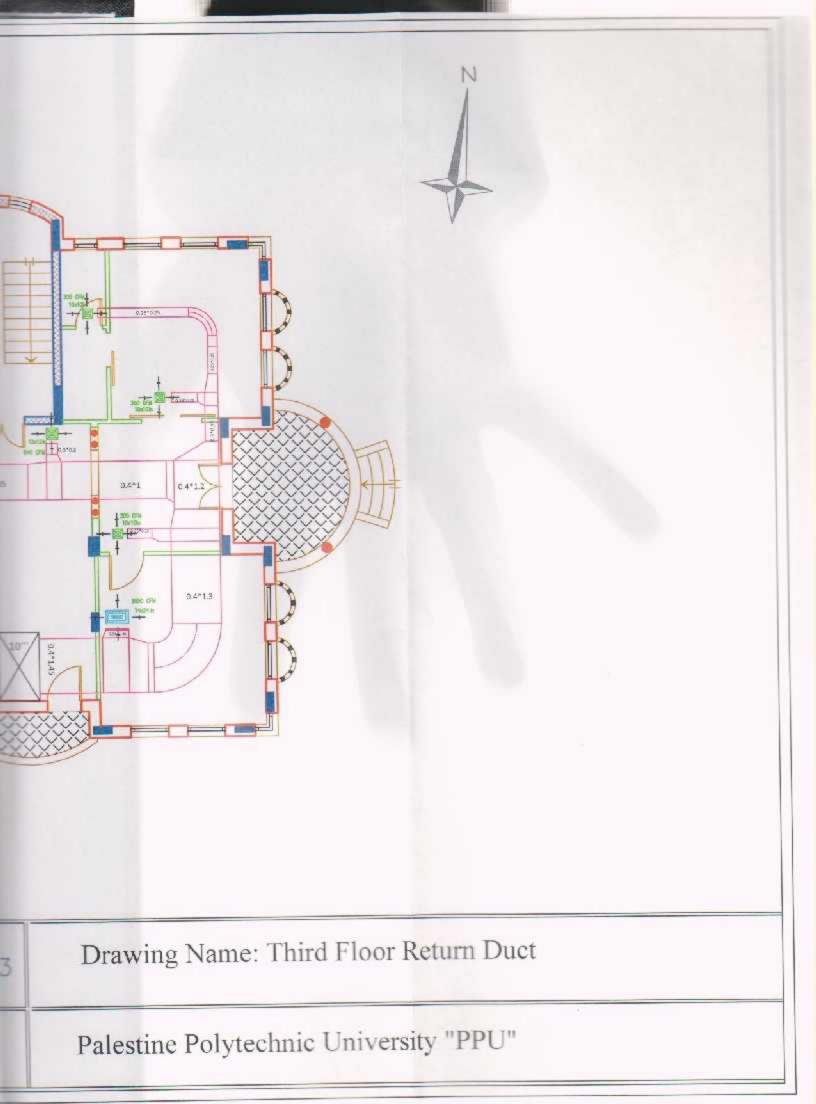


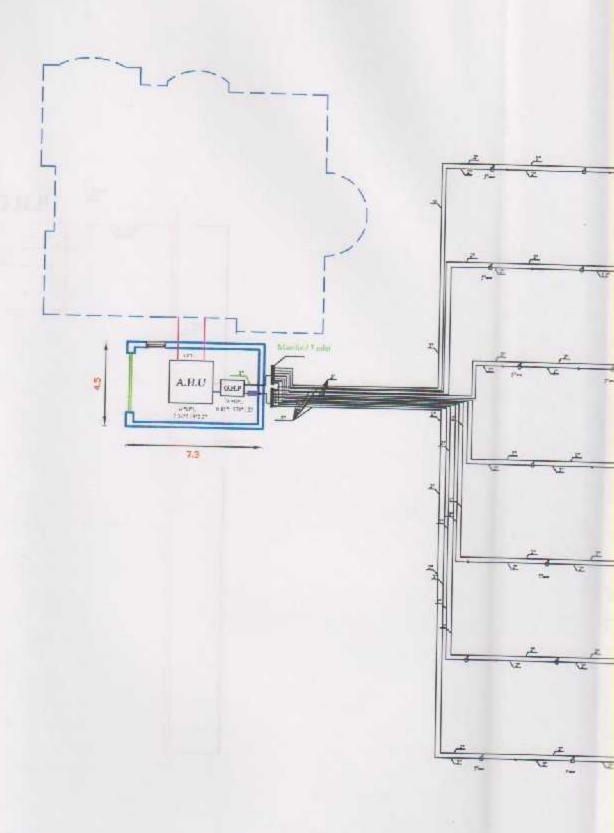
Division		TIO			
lame:	IBRAHIM&HANI&MOHAMMAD	SCALE:	FB	21.5.2013	Drawi
pervisor	Eng.Mohammad Awad	1/100	Graduation		
F	igure A-41	Sign	Project	HEBRON	Palest



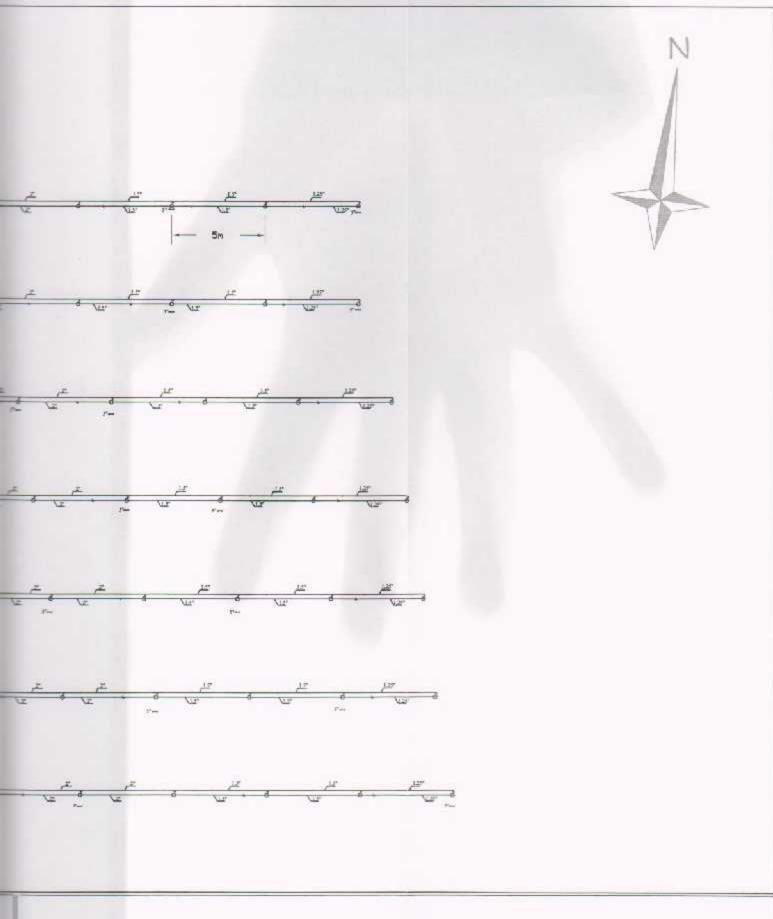


Division					
Name:	IBRAHIM&HANI&MOHAMMAD	SCALE:	F9	21.5.2013	Draw
upervisor	Eng.Mohammad Awad	1/100	Graduation		
F	igure A-42	Sign	Project	HEBRON	Pales

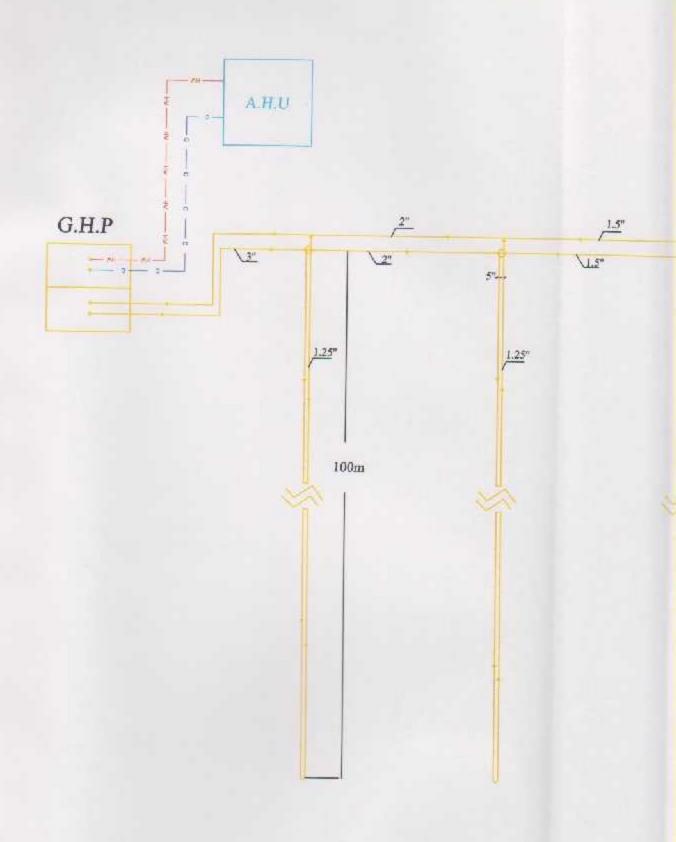




Division			TI4 O		
Name:	IBRAHIM&HANI&MOHAMMAD	SCALE:	F10	21.5.2013	Draw
upervisor	Eng.Mohammad Awad	1/200	Graduation		
Figure A-43		Sign	Project	HEBRON	Pales



Drawing Name: Ground Floor Plane & GHP Lines



Division			Data		0-2
Name:	IBRAHIM&HANI&MOHAMMAD	SCALE:	F11	21.5.2013	Drav
Supervisor	Eng.Mohammad Awad	1/100 =	Graduation		
Figure A-44		Sign	Project	HEBRON	Pales

